

**OKLAHOMA DEPARTMENT OF ENVIRONMENTAL QUALITY
AIR QUALITY DIVISION**

MEMORANDUM

May 13, 2019

TO: Phillip Fielder, P.E., Chief Engineer

THROUGH: Phil Martin, P.E., Manager, Existing Source Permits Section

THROUGH: Peer Review

FROM: David Schutz, P.E., New Source Permits Section

SUBJECT: Evaluation of Permit Application No. **2016-1295-C (M-5)(PSD)**
Koch Fertilizer Enid LLC (Formerly “Koch Nitrogen”)
Enid Nitrogen Plant
Enid, Garfield County, Oklahoma
1619 South 78th
Sec. 17 – T22N – R5W
Five Miles East of Enid on Highway 64, One Mile South on County Road
Latitude 36.37700°N, Longitude 97.76500°W

SECTION I. INTRODUCTION

Koch Fertilizer Enid LLC (Koch) operates an ammonia products and nitrogen fertilizer plant (SIC 2873) located approximately five (5) miles east of Enid, Oklahoma. The facility is currently operating as authorized by Permit No. 2016-1295-TVR2 (M-2) issued on October 8, 2018. The facility was also issued three construction permits: an expansion to the urea production operations is currently being conducted under Permit No. 99-092-C (M-3)(PSD) issued October 12, 2009; the reformers are being upgraded under Permit No. 99-092-C (M-5) issued August 3, 2010; and a major expansion to the facility was authorized under Permit No. 2011-441-C (M-9)(PSD) issued September 18, 2016.

The facility has requested a minor change to Permit No. 2011-441-C (M-9)(PSD):

- EUG 21, the No. 2 Urea Plant Synthesis Vent, currently has the following requirement:
 - A. Compliance Demonstration: Compliance with these limits is demonstrated by Urea production of 2,425 TPD (monthly average) or less.

The operator is requesting that the production limit be increased to 2,900 TPD from the current 2,425 TPD. The applicable emissions limits for the unit (for CO, VOC, and PM), which were derived from BACT requirements for the PSD permit, will not be changed, nor will any monitoring, reporting, or recordkeeping requirement. No effect is anticipated on upstream units; ammonia and CO₂ production will be the same, but more of the ammonia will go to urea production. Downstream loading operations emissions were based on higher hourly rates (141 TPH based on equipment capacity compared to the proposed 121 TPH), and are fugitive (no emissions limits are stated); fugitive PM emissions will remain below the levels which were modeled. The requested change qualifies as a “minor” modification. Tier I processing is allowed.

EPA’s policy for modified PSD permits is stated in a document, “PSD Permit Modifications: Policy Statement on Changes to a Source, a Permit Application, or an Issued Permit and on Extensions to Construction Schedules” dated 6/85. That guidance divides changes into “fundamental,” “significant,” “minor,” and “administrative” changes. The change category is based on emissions changes for the facility rather than unit capacities. The emissions rates from the initial PSD permit are unchanged.

Since the facility emits more than 100 TPY of a regulated pollutant, it is subject to Title V permitting requirements. Emission units (EUs) have been arranged into Emission Unit Groups (EUGs) in Section III.

SECTION II. OVERALL PROJECT DESCRIPTION

The construction project which was permitted under Permit No. 2011-441-C (M-3)(PSD) will accomplish the following:

- The two existing ammonia plants will be modified, increasing capacities from the current value of 1,600 TPD each to approximately 1,700 TPD for Plant No. 1 and 1,900 TPD for Plant No. 2.
- A second urea plant (to be designated “No. 2 Urea Plant”) with a capacity of 2,900 TPD will be added. (That capacity is being revised in this permit from 2,425 TPD.)
- A liquid-based urea production unit will be added.
- A 450 MMBTUH gas-fired boiler will be installed. The unit will have Low-NO_x burner technology.
- A cooling tower will be constructed serving the No. 2 Urea Plant. Maximum water circulation is 50,700 GPM. Drift eliminators will be installed to achieve 0.0005% or less drift.

- A new urea storage building, urea handling equipment, and truck and railcar loading operations will be constructed.
- Connections will be installed between the existing No. 1 Urea Plant and the new No. 2 Urea Plant which will result in enhanced production from the No. 1 Urea Plant by better removal of water from urea product and better granulation. This project may be considered to constitute “debottlenecking” of the unit.

The facility manufactures ammonia (NH_3), urea ($\text{CO}(\text{NH}_2)_2$), carbon dioxide (CO_2), and urea-ammonium nitrate blend (UAN). The market for each product varies considerably month-to-month and year-to-year. The fundamental business purpose of the facility is to use natural gas and nitrogen feedstocks to manufacture ammonia, urea, UAN, and CO_2 , and the facility must have the flexibility to operate in the various production configurations to respond to changing market conditions for these products.

The proposed project is subject to Prevention of Significant Deterioration (PSD) review for added emissions of greenhouse gases (GHG), carbon monoxide (CO), and particulate matter (PM_{10} / $\text{PM}_{2.5}$). Nitrogen oxide (NO_x) emissions increases will exceed PSD significance levels, but the project will “net out” from full PSD review. Sulfur dioxide (SO_2) and volatile organic compound (VOC) emissions will be below PSD levels of significance. Full PSD review consists of:

- A. determination of best available control technology (BACT)
- B. evaluation of existing air quality and determination of monitoring requirements
- C. evaluation of PSD increment consumption
- D. analysis of compliance with National Ambient Air Quality Standards (NAAQS)
- E. ambient air monitoring
- F. evaluation of source-related impacts on growth, soils, vegetation, visibility
- G. evaluation of Class I area impacts.

SECTION III. FACILITY DESCRIPTION

Construction of the plant began in 1973. The operations at the site are currently split into seven distinct “plants:” the two (2) ammonia plants (each currently 1,600 TPD capacity), the two (2) urea plants, the urea ammonium nitrate (UAN) plant, the vapor CO_2 plant, and the hydrogen recovery unit (HRU) plant. The CO_2 plant is operated by KFE, but owned by another entity. Additionally, a contractor owns, operates and maintains a portable ammonium polyphosphate process unit that is also used on-site on a seasonal basis. The primary raw materials for the process are methane and nitrogen, producing ammonia, urea, nitric acid, and urea-ammonium nitrate. The facility operates process units that conduct the following operations:

- Natural Gas Desulfurization: Raw materials used for the production of ammonia are natural gas, water and air. After natural gas enters the plant, the natural gas stream is split. A portion of the stream is used to fuel various combustion sources. The remainder of the stream is directed to the desulfurization unit. The desulfurization unit uses a cobalt-molybdenum or nickel-molybdenum catalyst followed by a zinc catalyst to "sweeten" or remove sulfur compounds from the natural gas. These sulfur compounds would otherwise poison subsequent catalysts.
- Catalytic Steam Reforming: Steam reforming is the process by which hydrogen gas is produced and nitrogen is added. Steam reforming takes place in two steps: primary reforming and secondary reforming. In the Primary Reformer, steam (H_2O) is reacted with methane (CH_4) to form carbon monoxide (CO), carbon dioxide (CO_2), and hydrogen (H_2) in the presence of a nickel-based reforming catalyst. H_2 will be used later to react with N_2 to produce ammonia (NH_3). A gas-fired boiler (EU-2202UB) rated at 144 MMBTUH is used to generate supplemental steam for both units. In the Secondary Reformer, air is added to the process stream, which provides nitrogen (N_2) and oxygen (O_2). The ratio of air is carefully controlled to provide the correct mixture of N_2 and H_2 to obtain the optimum yield from the reaction. The stream leaving the Secondary Reformer is cooled in a waste heat boiler as it exits the reformer. The emission units within this part of the process represent the combustion emissions from Primary Reformers and Auxiliary Boilers, and are identified as Emission Unit Group (EUG) EUG-2.
- Carbon Monoxide Shift: The shift converter consists of two converter systems: high temperature shift (HTS) and low temperature shift (LTS). The objective of the shift converters is to "shift" as much CO to CO_2 as possible. In the shift converters, CO is reacted with H_2O to form CO_2 and H_2 . The unreacted water vapor is then condensed and removed from the process gas stream. The stream is now referred to as "synthesis gas." The raw synthesis gas passes into the CO_2 Absorber for the initial synthesis gas purification step. The LTS catalyst produces a small amount of methanol, as a byproduct, which contributes to potential methanol emissions at the Plant. KFE, however, utilizes a low methanol producing catalyst designed to minimize methanol formation.
- Carbon Dioxide Removal: In the CO_2 Absorber, the synthesis gas stream flows upward and passes through packed beds, which promote close contact of the synthesis gas with a down flowing unsaturated (lean and partially unsaturated (semi-lean)) solution of potassium carbonate and potassium bicarbonate (Benfield solution). The Benfield solution absorbs the CO_2 from the synthesis gas stream to form potassium bicarbonate. The Benfield solution is regenerated by flashing into the CO_2 Stripper Towers (EU-1102E1 and EU-1102E2). The absorber overhead flows to the CO_2 Absorber knock out drum for removal of any entrained Benfield solution. The synthesis gas leaving the knock out drum then passes through heat exchangers to be preheated before flowing to the inlet of the Methanator. The stripped CO_2 leaves the top of the stripper and is sent to the urea and urea ammonium nitrate plants or is sold as product to various customers. Linde, an independent company not related to KFE, purchases some of the CO_2 from this point in the process. Their facility is on adjoining property and they receive the CO_2 via pipeline and use it for food grade CO_2 production. Merit, an independent company not related to KFE, purchases some of the CO_2 from this point and it is processed in their on-site Carbon Dioxide Plant. Any remaining CO_2 not used or sold as product is vented to the atmosphere.

- Methanation: At this point in the process, the synthesis gas contains mostly H₂ and N₂ with residual amounts of CO and CO₂. The Methanator catalyst reacts the remaining carbon oxides with hydrogen to form methane and water. Methanation is required to remove the remaining CO and CO₂, which could poison the ammonia synthesis catalyst.
- Ammonia Synthesis ($3\text{H}_2 + \text{N}_2 \rightarrow 2\text{NH}_3$): The stream from the Methanator is cooled in a series of steps and is then compressed. Compression of the purified synthesis gas is the first step in the liquid ammonia production phase of the process. Prior to the final compression stage, a stream of recycled synthesis gas, containing ammonia, is combined with the stream. The high-pressure synthesis gas leaves the after-coolers of the compressors and is cooled further in two parallel streams. Ammonia from the recycle stream condenses out in the chillers and is sent to storage. The synthesis gas continues on to the inlet of the Ammonia Converter. In the Converter, N₂ reacts with H₂ to form ammonia (NH₃).

The Converter effluent purge gas is sent to the Hydrogen Recovery Unit for ammonia removal. In the event of unanticipated outages, the ammonia-laden purge gas is sent to the flare. Liquid ammonia from the purge separator is routed to the refrigeration system for recovery. Each Converter is equipped with a natural gas fired start-up heater (EUG 4) rated at 33 MMBTUH. The start-up heater is used to heat the Converter up to reaction temperature during start-up.

The plant operates two (2) atmospheric cold storage tanks and two (2) pressurized bullet tanks for ammonia storage. Some of the ammonia is loaded into trucks and railcars (EU-AMH) or transported to consumers via pipeline. The flare (EU-2220U) is used to combust ammonia or hydrocarbons during loading, unloading and maintenance/startup/shutdown operations and to combust process gas (containing ammonia, hydrocarbons, hydrogen, etc.) from various relief valves throughout the plant.

- Hydrogen Recovery Unit (HRU): The HRU plant processes the High Pressure and Low Pressure Purge streams that are removed from the Ammonia processes to prevent the accumulation of non-reacting compounds such as methane and argon. After scrubbing with water to remove ammonia, a Prism Membrane unit removes hydrogen from the High Pressure Purge Gas streams. The recovered hydrogen is recycled back to the compressors in the Ammonia Synthesis section. The scrubbed Low Pressure Purge streams and the Prism unit reject stream are combined and sent to the Purge Gas fuel header.
- No. 1 Urea Synthesis (No. 1 Urea Plant): The urea plant receives CO₂ directly from the ammonia plants, and ammonia from the pressurized ammonia storage tanks. The CO₂ feed is compressed to synthesis pressure using a steam driven compressor and the ammonia is pumped to the synthesis pressure, and both are fed into the urea synthesis section (EUG 7). Condensate from the compression of CO₂ is sent to the Process Condensate Stripper (EU-308E). The reactants form ammonium carbamate, which dehydrates to urea. Excess water from the urea synthesis process is sent to the No. 1 Urea Plant Wastewater Concentrator (EUG 8).

- No. 1 Urea Evaporation: Target urea concentration is accomplished through the use of the evaporation section in two (2) steps. Before going through the evaporation section a portion of the liquid urea solution may be diverted for sale as a urea solution or may be used in the urea ammonium nitrate (UAN) product. The urea solution flows through the First Stage Evaporator where it is heated and system pressure is lowered resulting in an increased urea purity/concentration. The urea solution then passes through the Second Stage Evaporator where the urea concentration is further increased. The solution is now referred to as the “urea melt.” The urea melt is delivered to the granulation step for additional processing. A portion of the urea melt may be transferred to No. 2 Urea Plant for granulation. The evaporation process requires heat, which is provided by steam from two (2) natural gas fired boilers (EU-403A and EU-403B) rated at 84 MMBTUH each. The steam they produce is used in the synthesis step, in the evaporation step, and in the CO₂ compressor. The heat is also required to keep the refined urea in a molten state for the next step in the process.
- No. 1 Urea Granulation: A conditioning agent is added by direct injection to the urea melt to form methylenediurea. The conditioning agent is stored in the conditioning agent storage tank (EU-D202) prior to use. The conditioning agent reacts with the urea to reduce caking during storage and to reduce dust formation during material handling. Granulation currently takes place in three (3) rotating drums. The hot urea melt is sprayed into rotating drums (urea granulators) filled with solid urea granules. The urea spray coats the smaller granules in the drum. Cool air is used in a counter flow to the spray to cool and solidify the urea granules. The urea granulators (EU-K201A, EU-K201B, EU-K201C) each utilize a wet scrubber for the recovery of product and reduction of PM emissions. The solid urea is screened for size and sent to product storage via an enclosed belt conveyor. The material is transported in bulk via trucks or railcars. KFE occasionally produces granular products with additional additives for specialized product properties. The additives are incorporated into the urea melt upstream of the granulators and do not significantly change the quantity of PM emissions.
- No. 2 Urea Synthesis (No. 2 Urea Plant): The urea plant receives CO₂ directly from the ammonia plants, and ammonia from the pressurized ammonia storage tanks. The CO₂ feed is compressed to synthesis pressure using a steam driven compressor and the ammonia is pumped to the synthesis pressure, and both are fed into the urea synthesis section (EUG 21). The reactants form ammonium carbamate, which dehydrates to urea. Process water is collected and sent to a desorber and hydrolyzer system for recovery.
- No. 2 Urea Evaporation: Target urea concentration is accomplished through the use of the evaporation section in two (2) steps. Before going through the evaporation section a portion of the liquid urea solution may be diverted for sale as a DEF grade urea solution product. The urea solution flows through the First Stage Evaporator where it is heated and system pressure is lowered resulting in an increased urea purity/concentration. The urea solution then passes through the Second Stage Evaporator where the urea concentration is further increased. The solution is now referred to as the “urea melt.” The urea melt is delivered to the granulation step for additional processing. The evaporation process requires heat, which is provided by steam from a natural gas fired boiler (EUG-23) rated at 450 MMBTUH. The steam produced is used in the synthesis step, in the evaporation

step, and in the CO₂ compressor. The heat is also required to keep the refined urea in a molten state for the next step in the process.

- No. 2 Urea Granulation: A conditioning agent is added by direct injection to the urea melt to form methylenediurea. The conditioning agent is stored in the conditioning agent storage tank prior to use. The conditioning agent reacts with the urea to reduce caking during storage and to reduce dust formation during material handling. Granulation takes place in a fluidized bed. The hot urea melt is sprayed into the bed containing small seed particles. The urea spray coats the smaller particles and they increase in size. Cool air is used to cool and solidify the granules. The granulator utilizes a wet scrubber for the recovery of product and reduction of PM emissions (EUG 23). The solid urea is screened for size and sent to product storage via an enclosed belt conveyor. The material is loaded for transport in bulk via trucks or railcars (EUG 26). A portion of the granular product may be transferred to No. 1 Urea Plant for processing.
- Urea Synthesis (UAN Plant): Ammonia from the ammonia pressurized storage (bullets) and CO₂ from the ammonia plants are reacted in a once-through urea production unit at high pressure to form ammonium carbamate (NH₂CO₂NH₄), which then forms urea (CO(NH₂)₂). The CO₂ is compressed to reaction pressure using an electric driven reciprocating compressor. At the outlet of the urea synthesis reactor, the reaction mixture's pressure is dropped, which causes the unreacted ammonium carbamate to decompose back to gaseous ammonia and carbon dioxide, which is referred to as "off-gas." The off-gas stream is split and sent as ammonia feed to the nitric acid section of the UAN plant and to the ammonium nitrate section of the UAN plant.
- Nitric Acid Synthesis (UAN Plant): Nitric acid is produced in three steps: ammonia oxidation to form nitrogen oxide (NO) and H₂O; NO oxidation to form nitrogen dioxide (NO₂); and, absorption of NO₂ in water to form nitric acid (HNO₃). In the first step, compressed air and off gas from the urea section of the UAN plant are reacted in a converter over a platinum gauze catalyst to produce nitrogen oxide (NO) and water. The nitric oxide is further oxidized to form NO₂. The NO₂ is absorbed by water in a absorption column to form nitric acid. A bleaching section uses a secondary stream of air to strip some of the dissolved gases (mainly NO and NO₂) from the nitric acid prior to storage. Unreacted nitrogen oxides in the tail gases are mixed with hydrogen rich synthesis/purge gas and directed to the nonselective catalytic reduction (NSCR) abatement system for NO_x control. Nitric acid is stored in a storage tank, which is vented to the process condensate overhead condenser. It should be noted that the nitric acid plant was originally constructed in Kennewick, Washington in 1968. It was relocated to the current site in 1990.
- Ammonium Nitrate Synthesis (UAN Plant): Ammonia rich off gas from the urea section of the UAN plant is neutralized with nitric acid to form ammonium nitrate (AN). The synthesis process pH is carefully controlled for safety reasons such that no free ammonia remains. Process equipment for ammonium nitrate production includes two (2) distinct vessels (neutralizer and process condensate tank), each equipped with a scrubber. These scrubbers are inherent to the process and cannot be shutdown or bypassed during the production process. The process cannot function as designed and the AN product cannot be made without the scrubber section of each vessel operating.

- Urea Ammonium Nitrate (UAN) Solution: The final step in the production of UAN is combining the urea with the ammonium nitrate to produce the UAN solution. The UAN solution contains a product specific percentage of ammonium nitrate and urea. The remainder of the solution is water. The product is stored in a storage tank prior to being bulk shipped by truck or rail. The plant operates one (1) UAN day tank and two (2) UAN storage tanks.
- Carbon Dioxide Plant: The Merit CO₂ Plant receives CO₂ produced in the ammonia plants and prepares it for transportation via pipeline. The CO₂ passes through three (3) stages of compression and cooling, then a final dehydration polish by contacting the gas with a circulating solution of triethylene glycol (TEG). The TEG is continuously circulated back to a glycol dehydrator where the water is driven off by heating with one (1) natural gas-fired glycol dehydrator reboiler (EU-R2401) rated at 1.5 MMBTUH. After dehydration, the CO₂ is further compressed to approximately 1,700 psig for injection into the pipeline owned and operated by Merit Energy Company who transports it for enhanced oil recovery (EOR).

Plant operations are 24 hrs/day, every day of the year.

SECTION IV. INDIVIDUAL PROJECT DESCRIPTIONS

The proposed modifications to the facility may be grouped in Ammonia Plant changes, No. 1 Urea Plant changes, and No. 2 Urea Plant (new).

Ammonia Plant Changes

The following changes will increase the capacity of the No. 1 and No.2 Ammonia Plants from approximately 3,200 TPD to approximately 3,600 TPD.

- The two ammonia plant primary reformers currently have permitted firing rates of 909.6 MMBTUH and 931.4 MMBTUH, respectively, for the No. 1 and No. 2 plants. Selective Catalytic Reduction (SCR) will be retrofitted on the No. 2 Primary Reformer to reduce NO_x emissions. The firing rates will be increased to 965 MMBTUH and 990 MMBTUH, respectively, annual average (1,076 MMBTUH and 1,350 MMBTUH, respectively, short-term capacities.)
- “Feed gas saturation” (injection of water into a hot process stream) will be added to improve energy efficiency.
- Additional reformer burners and tubes will be added to the No. 2 Ammonia Plant to improve heat distribution.

- Existing burners and fans in the No. 1 and No. 2 Ammonia Plants will be replaced as necessary to improve operability and emissions performance of the Reformer.
- The No. 2 Ammonia Plant air preheater will be replaced to achieve a higher heat transfer rate.
- The mixed feed preheat coils in the heat recovery sections of both reformers will be upgraded to improve energy efficiency.
- The capacity of the process air compressors will be increased on both ammonia plants.
- The No. 2 Ammonia Plant high-temperature shift converter vessel will be altered to achieve a lower pressure drop.
- A new low-temperature shift converter will be added in each ammonia plant to reduce pressure drop and extend catalyst life.
- CO₂ Absorption Tower absorption solution and tower packing will be changed on both ammonia plants.
- The synthesis gas compressors on both ammonia plants will have a mixer/separator section added to dehydrate synthesis gas.
- One of the interstage coolers in the No. 2 Ammonia Plant will be replaced with a larger heat exchanger.
- A recycle cooler will be added to each compressor.
- The ammonia recovery operation will be modified to achieve higher production rates and energy efficiency.
- A new ammonia converter will be added to the No. 2 Ammonia Plant in series with the existing converter.
- The heat recovery exchanger on the No. 2 Ammonia Plant will be replaced with a larger unit.
- The primary shift heat effluent waste heat exchanger in the No. 2 Ammonia Plant will be changed to steam superheater service.
- An additional cooling tower cell will be added to the No. 2 Ammonia Plant.
- The cooling tower fill material in the No. 1 Ammonia Plant will be upgraded to improve capacity.
- The steam turbines powering the refrigeration compressors on both ammonia plants will be altered to provide increased refrigeration capacity.
- Other changes in the Ammonia Plants required to achieve the proposed production and emission rates.

No. 1 Urea Plant Changes

Proposed changes will allow the No. 1 Urea Plant to perform up to its permitted design capacity

- Connections will be installed from the existing No. 1 Urea Plant to the proposed new No. 2 Urea Plant so that urea solution may be transferred for concentration by evaporation and granulation.
- Connections will be installed to transfer process condensate from the No. 1 Urea Plant to the proposed No. 2 Urea Plant.
- There will be equipment installed to transfer granulated urea from the proposed No. 2 plant to the No. 1 Urea Plant materials handling, storage, and loading units.
- There will be additional steam demands on the two existing 84 MMBTUH boilers in the No. 1 Urea Plant although these units will not be physically modified.
- There will be additional loading on the existing No. 1 Urea Plant cooling tower but this unit will not be physically modified.

No. 2 Urea Plant

- The capacity of the proposed No. 2 Urea Plant will be 2,900 TPD (dry-basis), reacting CO₂ and ammonia to form urea. Urea solution is either converted to a solid granular product or sold as “diesel exhaust fluid” (DEF).
- A new 450 MMBTUH gas-fired boiler will be installed to provide necessary heat. The unit will have Low-NOx burner technology.
- A new cooling tower will be installed on the No. 2 Urea Plant. Maximum circulation rate is 50,700 GPM with a drift of 0.0005%.
- The No. 2 Urea Plant evaporators and granulator will be sized for 3,390 TPD throughput, which includes the capacity of the proposed plant plus any urea solution transferred from the existing No. 1 Urea plant.
- The process water recovery section will handle process water from the No. 1 Urea Plant.
- Granular urea product will be stored in a new enclosed barn for shipment by truck and/or rail.
- The DEF product will be blended to desired urea strength for shipment to customers via truck.
- A 70,000-gallon tank will be constructed for a formaldehyde-based liquid additive used to condition urea for better granulation and reduced dusting.
- Conveyors will be constructed to transfer granulated urea from the No. 2 Urea Plant to a new bulk urea storage building. Conveyors and transfer towers will be completely enclosed.

- There will be truck and railcar loading stations for the urea product.
- Haul roads will be paved to minimize fugitive dust from vehicle traffic.

SECTION V. EQUIPMENT

A. New Equipment

EUG 17 No. 2 Urea Conditioning Agent Storage Tank

EU ID	Point ID	Capacity	Construction Date
UR2FBATK	24-9166	70,000 Gallons	Est. 2014-2017

EUG 21 No. 2 Urea Plant Synthesis Vent

EU ID	Point ID	EU Name/Model	Capacity	Construction/Modification Date
UR2SYN	21-9163	No. 2 Urea Synthesis Vent	2,900 TPD	Est. 2014-2017

EUG 22 No. 2 Urea Plant Granulators

EU ID	Point ID	EU Name/Model	Capacity	Construction/Modification Date
UR2GRAN	22-9164	No. 2 Urea Granulator	3,390 TPD	Est. 2014-2017

EUG 23 No. 2 Urea Plant Boiler

EU ID	Point ID	EU Name/Model	Heat Input	Constr. Date
UR2BLR	23-9165	No. 2 Urea Plant Boiler	450 MMBTUH	Est. 2014-2017

EUG 25 No. 2 Urea Plant Cooling Tower

EU ID	Point ID	EU Name	Capacity
UR2CTWR	25-9167	No. 2 Urea Plant Cooling Tower	50,700 GPM

EUG 26 No. 2 Urea Plant Fugitive PM

EU ID	Point ID	EU Name
UR2MSTG	26-9168	No. 2 Urea Materials Storage
UR2MTRFR	26-9169	No. 2 Urea Materials Transfer
UR2MLD	26-9170	No. 2 Urea Materials Loading

EUG 27 New Haul Roads

EU ID	Point ID	EU Name
HAULRD	---	No. 2 Urea Plant Vehicle Traffic

B. Physically Modified Equipment**EUG 2 Ammonia Plant Primary Reformers**

Location	EU ID	Point ID	Heat Input*	Manufacturer	Construction Date
Ammonia Plant #1	101B1	2-9095	1076 MMBTUH hourly 965 MMBTUH annual	Kellogg	1973
Ammonia Plant #2	101B2	2-9097	1350MMBTUH hourly 990 MMBTUH annual	Kellogg	1975

*Post-modification heat inputs.

EUG 9 No. 2 Ammonia Plant Cooling Tower

EU ID	Point ID	EU Name	Capacity
22014B	9-9159	No. 2 Ammonia Plant Cooling Tower	65,700 GPM

EUG 10 CO₂ Stripping Towers

Location	EU ID	Point ID	EU Name/Model	Manufacturer	Construction Date
Ammonia Plant #1	1102E1	10-9120	CO ₂ Stripping Tower 1 (PV30-1)	Kellogg	1973
Ammonia Plant #2	1102E2	10-9121	CO ₂ Stripping Tower 2 (PV30-2)	Kellogg	1975

C. Units with Increased Utilization**EUG 1 Plant-wide**

This EUG is established to address requirements that apply to the entire plant, including open burning restrictions, visible emissions, fugitive dust control. The plant is requesting to operate under a state and federally enforceable plant-wide cap for methanol, which is classified as a hazardous air pollutant (HAP). The process condensate stripper, the primary source of methanol emissions from this type of plant, is refluxed to the process rather than vented to the atmosphere.

EUG 7 No. 1 Urea Plant Synthesis Vents

EU ID	Point ID	EU Name/Model	Manufacturer	Capacity	Construction/Modification Date
HIC135	7-9111	High Pressure Vent	Foster Wheeler	1,550 TPD	1980 / 2007
D119	7-9110	Low Pressure Vent	Foster Wheeler	1,550 TPD	1980 / 2007

EUG 3 Boilers/Heaters > 50 MMBTUH

EU ID	Point ID	EU Name/Model	Heat Input	Manufacturer	Constr. Date
2202UB	3-9099	Ammonia Unit Startup Boiler	144 MMBTUH	Zurn Industries	1975
403A	3-9100	No. 1 Urea Boiler No. 1	84 MMBTUH	Zurn Industries	1980
403B	3-9101	No. 1 Urea Boiler No. 2	84 MMBTUH	Zurn Industries	1980

EUG 16 No. 1 Urea Plant Cooling Tower

EU ID	Point ID	EU Name
22014E	22014E	No. 1 Urea Plant Cooling Tower No. 2

Unaffected Existing Units**EUG 4 Boilers/Heaters < 50 MMBTUH**

Location	EU ID	Point ID	EU Name/Model	Heat Input	Manufacturer	Construction Date
Ammonia Plant #1	102B1	4-9102	Ammonia Unit Startup Heater No. 1	33 MMBTUH	Kellogg	1973
Ammonia Plant #2	102B2	4-9103	Ammonia Unit Startup Heater No. 2	33 MMBTUH	Kellogg	1975

EUG 5 No. 1 Urea Plant Conditioning Agent Storage Tank

EU ID	Point ID	Capacity	Construction Date
D202	5-9107	54,319 Gallons	1980

EUG 6 No. 1 Urea Plant Granulators

EU ID	Point ID	EU Name/Model	Manufacturer	Capacity	Construction/Modification Date
K201A	6-9104	No. 1 Urea Granulator No. 1	Foster Wheeler	517 TPD	1980 / 2007
K201B	6-9105	No. 1 Urea Granulator No. 2	Foster Wheeler	517 TPD	1980 / 2007
K201C	6-9106	No. 1 Urea Granulator No. 3	Foster Wheeler	517 TPD	1980 / 2007

EUG 11 Nitric Acid Plant

EU ID	Point ID	Manufacturer	Capacity (as 100% HNO ₃)	Construction Date
M221	12-9115	Weatherly	118 TPD	1968 / 1990 *

* This unit was originally constructed in 1968 and relocated to Enid in 1990 from Kennewick, Washington.

EUG 12 Ammonium Nitrate Plant

EU ID	Point ID	Manufacturer	Capacity (as 75.5% AN)	Construction Date
T311	12-9116	Weatherly	176 TPD	1968 / 1990 *

* This unit was constructed in a different location and relocated to Enid in 1990.

EUG 13 Flare

EU ID	Point ID	Heat Input *	Construction Date
222OU	13-9118	1,350 SCFH	1993

*Heat input refers to natural gas and/or purge gas to maintain flare pilot.

EUG 14 Fugitives

Location	EU ID	Point ID	EU Name
Ammonia Plants	AMH	14-9119	Ammonia Plant Material Handling –Materials Loading
No. 1 Urea Plant	UMH	14-9120	No. 1 Urea Plant Material Handling/Loading Fugitives

EUG 14A No. 1 Urea Plant Fugitives

EU ID	Point ID	EU Name
UMS	UMS	No. 1 Urea Materials Storage
UMH	UMH	No. 1 Urea Materials Handling
UML	UML	No. 1 Urea Materials Loading

EUG 15 Startup/Shutdown Vents

Location	EU ID	Point ID	EU Name	Construction Date
Ammonia Plant #2	308E	15-9109	Process Condensate Stripper	1980
Ammonia Plant #1	SP73-1	15-9151	Startup/Shutdown Vent 1 (PV-102 & PV-5)	1973
Ammonia Plant #1	SP74-1	15-9152	Startup/Shutdown Vent 2 (102F-RV Mute)	1973
Ammonia Plant #1	SP75-1	15-9153	Startup/Shutdown Vent 3 (PV-4)	1973
Ammonia Plant #2	SP73-2	15-9154	Startup/Shutdown Vent 1 (PV-102 & PV-5)	1975
Ammonia Plant #2	SP74-2	15-9155	Startup/Shutdown Vent 2 (102F-RV Mute)	1975
Ammonia Plant #2	SP75-2	15-9156	Startup/Shutdown Vent 3 (PV-4)	1975
Ammonia Plant #1	1102E1	15-9120	CO ₂ Stripping Tower 1 (PV-30)	1973
Ammonia Plant #2	1102E2	15-9121	CO ₂ Stripping Tower 2 (PV-30)	1975

EUG 17 Insignificant Activities

Unit ID	Description
R-2401	Glycol dehydration reboiler (1.5 MMBTUH)
APP-IC	475-hp Portable mixer engine *
APP-Portable Unit	APP Portable 10-34-0 processing unit*
Diesel	Diesel storage tanks (3)
UAN TANKS	UAN tanks (2)
LIME	Lime silos (2)
#1 Plant 108-D Vent	No. 1 Ammonia Plant 108-D vent (TV-50)
#1 PIC-14 Vent	No. 1 Ammonia Plant PIC-14 fuel vent
#1 PIC-33 Vent	No. 1 Ammonia Plant PIC-33 fuel vent
#1 Catalyst Warm-ups	No. 1 Ammonia Plant catalyst warm-up vent (SP-73)
#1 Low Shift Vent	No. 1 Ammonia Plant Low-Shift Reductions vent (SP-73)
#1 LTS Catalyst Cooling	No. 1 Ammonia Plant LTS Catalyst Cooling vent (SP-73)
#1 HTS Catalyst Cooling	No. 1 Ammonia Plant HTS Catalyst Cooling vent (SP-73)
#1 Methanator Unit Catalyst Cooling	No. 1 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)
#2 Plant 108-D Vent	No. 2 Ammonia Plant 108-D vent (TV-50)
#2 PIC-14 Vent	No. 2 Ammonia Plant PIC-14 fuel vent
#2 PIC-33 Vent	No. 2 Ammonia Plant PIC-33 fuel vent

Unit ID	Description
#2 Catalyst Warm-ups	No. 2 Ammonia Plant catalyst warm-up vent (SP-73)
#2 Low Shift Vent	No. 2 Ammonia Plant Low-Shift Reductions vent (SP-73)
#2 LTS Catalyst Cooling	No. 2 Ammonia Plant LTS Catalyst Cooling vent (SP-73)
#2 HTS Catalyst Cooling	No. 2 Ammonia Plant HTS Catalyst Cooling vent (SP-73)
#2 Methanator Unit Catalyst Cooling	No. 2 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)
Lab Vents	Laboratory fume hoods and vents
UR2FBATK	No. 2 Urea Plant conditioning agent tank

* Equipment owned, operated, and maintained by a contractor.

EUG 18. Emergency Engines Subject to NSPS Subpart JJJJ

Point ID#	Capacity (hp)	Make/Model	Installed Date
GEN2	147	Generac 6.8GN	2010
GEN3	40	Olympian G25LTA	2011

EUG 19. Diesel Engines Subject to NESHAP Subpart ZZZZ

Point ID#	Capacity (hp)	Make/Model	Serial Number	Installed Date
GEN	460	Cummins KT-1150-G	100P1432	1976
PUMP	145	Clarke VMFPT6HT	91B-02093	2002

EUG 20. Gasoline Tank

Unit ID	Point	EU Description	Capacity	Construction Date
Gasoline	Gasoline	Vehicle gasoline tank	1,128 gal	>2003

SECTION VI. EMISSIONS

Emissions calculations are shown for the new units and physically-modified units. In determining PSD applicability, the facility used the option of determining Projected Actual Emissions (PAE) from each modified unit to be the Potential-to-Emit from each unit. Potential emissions from each emissions unit have been calculated using the particular configuration that results in the maximum emissions from that unit on a pollutant-by-pollutant basis. This approach allows for permit conditions that reflect the PTE for the full range of potential operational configurations, which are in turn based on the fundamental business purpose of the source.

Emission factors are derived from several sources including AP-42, other published emission estimation methodologies, stack tests, laboratory data, permitted limits, mass balance equations, and process knowledge. As indicated, some factors have been adjusted by a safety factor to account for process variability.

KOCH quantified emissions of hazardous air pollutants (HAPs) from processes facility-wide. For the combustion processes, emission factors from AP-42 (7/98), Section 1.4 and Section 1.11 and from other published information are used as a means of estimating emissions, some of which were derived from limited test data. For HAP estimates from non-combustion processes, methodology is discussed in this section for individual emission unit groups. Ammonia emissions are no longer shown due to the revocation of OAC 252:100-41.

A. New Units

EUG 17: No. 2 Urea Plant Conditioning Agent Storage Tank

VOC / formaldehyde / methanol emissions from the storage tank were based on a mass balance (since the tank will be maintained at approximately 150°F, no breathing losses were calculated). An annual maximum throughput of 1,123,000 gallons, molecular weight of 30, and vapor pressure of 0.33 psia were used.

Vapor Pressure, psia	Throughput, gallons	Molecular Weight	VOC Emissions, TPY
0.33	1,123,000	30	0.14

EUG 21: No. 2 Urea Plant Synthesis Vent

The new No. 2 Urea Plant has a design capacity of 2,546 TPD, with a maximum short-term production rate of 2,900 TPD (106.1 TPH). PM₁₀ / PM_{2.5} emissions are based on vendor guarantees, while CO emissions are based on June 2006 analytical testing (where sampling of the CO content in the CO₂ stream sent to urea plants) data plus a 300% safety factor.

Unit Throughput, TPH	Pollutant	Emission Factor	Emissions	
			lb/hr	TPY
106.1 (initial design)	PM ₁₀ / PM _{2.5}	0.046 lb/hr	0.05	0.20
120.83 (new limit)	CO	0.029 lb/ton	3.08	12.83

NOTE: limits based on initial design capacity are unchanged.

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
21-9163	No. 2 Urea Plant Vent	0.05	0.20	--	--	--	--	--	--	3.08	12.83

EUG 22: No. 2 Urea Plant Granulator

The new No. 2 Urea Plant granulator will have a design capacity of 3,390 TPD (141.25 TPH). The listed PM emission factor, 0.043 lb/ton, was derived from vendor guarantees for PM emissions of 5 mg / dry m³. Controlled formaldehyde emissions were taken from EPA's "Locating and Estimating Air Emissions from Sources of Formaldehyde" (March 1991). Methanol emissions were based on 0.1% in the granulation additive, annual usage of 1,123,000 gallons, and 11.0 lb/gal density. VOC is the sum of methanol plus formaldehyde.

Unit Throughput, TPH	Pollutant	Emission Factor	Emissions	
			lb/hr	TPY
141.25	PM ₁₀ / PM _{2.5}	0.043 lb/ton	6.04	26.45
	VOC	0.029 lb/ton	2.39	8.44
	Formaldehyde	0.0054 lb/ton	0.76	3.34
	Methanol	Mass balance	1.41	4.34

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
22-9164	No. 2 Urea Plant Granulator	6.04	26.45	--	--	--	--	2.39	8.44	--	--

EUG 23: No. 2 Urea Plant Boiler

Emissions from the new boiler were based on a unit capacity of 450 MMBTUH. NO_x and CO emission are taken from manufacturer data, but a 25% safety factor was added to NO_x emissions. SO₂, VOC, and PM emissions were based on AP-42 (1/95), Section 1.4. GHG emission factors are based on 40 CFR 98, Subpart C for natural gas combustion.

Unit Capacity	Pollutant	Emission Factor, lb/MMBTU	Emissions	
			lb/hr	TPY
450 MMBTUH	CO	0.037	16.65	72.93
	NO _x	0.045	20.25	88.70
	SO ₂	0.0006	0.26	1.16
	VOC	0.0055	2.43	10.63
	PM ₁₀ / PM _{2.5}	0.0076	3.35	14.69
	GHG	117	52,652	230,614

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
23-9165	No. 2 Urea Plant Boiler	3.35	14.69	0.26	1.16	20.25	88.70	2.43	10.63	16.65	72.93

EUG 25: No. 2 Urea Plant Cooling Tower

PM emissions from the No. 2 Urea Plant Cooling Tower were calculated using a drift factor of 0.0005%, water circulation rate of 50,700 GPM, and total dissolved solids content of 3,300 ppm. PM₁₀ / PM_{2.5} emissions were calculated from methodology in "Calculating Realistic PM₁₀ Emissions from Cooling Towers" (Joel Reisman and Gordon Frisbie).

Circulation Rate, GPM	Drift Factor	TDS, ppm	Emission Factor	Pollutant	Emissions	
					lb/hr	TPY
50,700	0.0005%	3,300	Mass balance	PM	0.42	1.83
			47.1% of PM	PM ₁₀	0.20	0.86
			0.2% of PM	PM _{2.5}	0.01	0.01

Point ID	Emission Unit	PM ₁₀		PM _{2.5}		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
25-9167	No. 2 Urea Plant Cooling Tower	0.20	0.86	0.01	0.01	--	--	--	--	--	--

EUG 26: No. 2 Urea Plant Fugitive PM (Loading, Storage, and Transfer)

Calculation of loading PM was based on a production capacity of 3,390 TPD urea (141.3 TPH). An uncontrolled emission factor of 0.017 was obtained from EPA's WEBFIRE database. Three control efficiencies were determined for the control methods:

1. 85% for partial enclosures per TCEQ "Technical Guidance for Rock Crushing Plants;"
2. 90% for product conditioning which results in stronger granules which resist crushing to dust; and
3. 75% for loading using telescopic chutes per EPA's "Stationary Source Control Techniques for Fine Particulate Matter" (D-98-026, 1998).

PM_{2.5} was stated at 69% of PM₁₀ per "Emissions from Industrial Plants – Results from Measurement Programmes in Germany" (December 2006).

The following emissions will be discharged from each of movement from the No. 2 Urea Plant to storage, loading from storage onto transfer conveyors, and loading from transfer conveyors into trucks or railcars.

Operation	Process Rate	Pollutant	Emission Factor	Control Efficiency 1	Control Efficiency 2	Control Efficiency 3	Emissions, TPY
Loading	141.3 TPH	PM ₁₀	0.017 lb/ton	85%	90%	75%	0.04
		PM _{2.5}	69% of PM ₁₀	--	--	--	0.03
Storage	141.3 TPH	PM ₁₀	0.017 lb/ton	85%	--	--	0.12
		PM _{2.5}	69% of PM ₁₀	--	--	--	0.08
Transfer	141.3 TPH	PM ₁₀	0.017 lb/ton	85%	--	--	0.12
		PM _{2.5}	69% of PM ₁₀	--	--	--	0.08

EUG 27: New Haul Roads

Fugitive dust emissions were calculated using the method of AP-42 (1/2011), Section 13.2.1:

$$EF \text{ (lb/VMT)} = k * (sl)^{0.91} * W^{1.02} * (1 - p / 4N) * (1 - CE)$$

Where $k = 0.0022$ for PM_{10} and 0.00054 for $PM_{2.5}$
 sl = silt loading, 0.6 g/m^2
 W = average vehicle weight, 27 tons
 p = number of days in a year with at least 0.01 inch rain, default = 80
 N = number of days in a year, 365
 CE = control efficiency, 82.9% for water flushing and sweeping

The facility anticipates loading 27 tons per truck:

- 109 trucks per day hauling urea 0.303 mile each way (66 miles/day, 24,100 miles/yr)
- 40 trucks per day hauling DEF 0.18 mile each way (29 miles/day, 10,500 miles/yr)

EPA guidance, “Control of Open Fugitive Dust Sources” (EPA-450/3-88-008), Table 2-4, lists a control efficiency for “Water flushing followed by sweeping” as “96% - $0.263 * V$,” where V is the number of vehicles which traverse a road following the control measure, here shown as 100, or approximately the anticipated number of vehicles per day.

Based on the emission calculations for the road segments and summing all segments, PM_{10} emissions will be 0.377 TPY and $PM_{2.5}$ emissions will be 0.092 TPY.

B. Physically Modified Equipment

EUG 1: Plant-wide Emissions

The process CO_2 generated in the No. 1 Ammonia Plant and No. 2 Ammonia Plant can be emitted from vents located in the No. 1 Ammonia Plant, No. 2 Ammonia Plant, No. 1 Urea Plant, No. 2 Urea Plant and other locations/vents throughout the facility. The total CO_2 generation is based on ammonia production capacity and the 40 CFR 98, Subpart G calculation methodology. The potential annual process CO_2 emissions are based on a maximum expected process CO_2 emission rate of 1.26 tons of CO_2 per ton of ammonia generated.

Unit	Feedstock MMscf/yr	Carbon Content	Potential Process CO_2 Generation TPY	CO_2 Potential to Emit ¹ TPY
No. 1 Ammonia Plant	13,297	0.74	781,829	--
No. 2 Ammonia Plant	14,861	0.74	873,809	--
TOTALS			1,655,639	1,260,000

1 – Based on emission rate of 1.26 tons CO_2 / ton ammonia where the potential to emit is limited by permit condition.

EUG 2: Ammonia Plant Primary Reformer Heaters

Post-project emission factors for CO and PM₁₀ / PM_{2.5} are from AP-42, Section 1.4 (7/98) using a fuel heat content of 1,020 BTU/SCF. For SO₂, a 50% safety factor was added to the AP-42 factors, and for VOC, a 50% safety factor was added to the AP-42 values to account for process variability. No. 1 and No. 2 Reformer post-project short-term NO_x emissions were based on 0.2 lb/MMBTU to cover all operational circumstances; the annual NO_x emissions were based on the stack test results of 0.1185 lb/MMBTU for the No. 1 Reformer and 0.04 lb/MMBTU for the No. 2 reformer. GHG emission factors are based on 40 CFR 98, Subpart C for natural gas combustion.

Unit	Pollutant	Emission Factor, lb/MMBTU	Emissions	
			lb/hr	TPY
101B1, No. 1 Ammonia Plant Reformer (1,076 MMBTUH hourly rate, 965 MMBTUH annual rate)	CO	0.084	88.61	348.08
	NO _x	0.2 / 0.1185	215.20	500.86
	SO ₂	0.0009	0.95	3.73
	VOC	0.0069	8.70	28.49
	PM ₁₀ / PM _{2.5}	0.0076	8.02	31.49
	GHG	117	125,892	494,565
101B2, No. 2 Ammonia Plant Reformer (1,350MMBTUH hourly rate, 990 MMBTUH annual rate)	CO	0.084	111.18	357.10
	NO _x	0.20 / 0.040	270.00	173.45
	SO ₂	0.0009	1.19	3.83
	VOC	0.0069	9.10	29.23
	PM ₁₀ / PM _{2.5}	0.0076	10.06	32.31
	GHG	117	156,558	507,378

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
2-9095 (No. 1 Reformer)	101B1	8.02	31.49	0.95	3.73	215.20	500.86	8.70	28.49	88.61	348.08
2-9097 (No. 2 Reformer)	101B2	9.97	32.31	1.18	3.83	267.60	173.45	9.02	29.23	110.19	357.10
TOTALS		17.99	63.80	2.13	7.56	482.89	674.31	17.72	57.72	198.80	705.18

EUG 9: No. 2 Ammonia Plant Cooling Tower

PM emissions from the No. 2 Ammonia Plant Cooling Tower added cell were calculated using a drift factor of 0.0005%, water circulation rate of 12,700 GPM, and total dissolved solids content of 3,300 ppm. PM₁₀ / PM_{2.5} emissions were calculated from methodology in “Calculating Realistic PM₁₀ Emissions from Cooling Towers” (Joel Reisman and Gordon Frisbie). Emissions from the existing cooling tower cells were based on a circulation rate of 53,000 GPM and a drift factor of 0.001% using the Reisman and Frisbie methodology.

Circulation Rate, GPM	Drift Factor	TDS, ppm	Emission Factor	Pollutant	Emissions	
					lb/hr	TPY
53,000	0.001%	3,300	Mass balance	PM	0.88	3.83
			47.1% of PM	PM ₁₀	0.41	1.80
			0.2% of PM	PM _{2.5}	0.01	0.01
12,700	0.0005%	3,300	Mass balance	PM	0.10	0.46
			47.1% of PM	PM ₁₀	0.05	0.22
			0.2% of PM	PM _{2.5}	0.001	0.005
65,700	0.001%	3,300	Mass balance	PM	0.98	4.29
			47.1% of PM	PM ₁₀	0.46	2.02
			0.2% of PM	PM _{2.5}	0.01	0.01

Point ID	Emission Unit	PM ₁₀		PM _{2.5}		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
9-9159	No. 2 Ammonia Plant Cooling Tower	0.46	2.02	0.002	0.009	--	--	--	--	--	--

EUG 10: CO₂ Stripping Towers

Added emissions from these units are GHG only; CO emissions are not affected. Added GHG are part of the plant-wide emissions shown for EUG-1.

C. Units with Increased Utilization

EUG 7: No. 1 Urea Plant Synthesis Vents

CO emissions were derived from stack testing in 2006 as test results plus 300%, assuming equal CO between high-pressure and low-pressure vents. PM₁₀ / PM_{2.5} emissions were based on AP-42 (7/93), assuming 75% from the high pressure vent and 25% from the low-pressure vent. Hourly emissions assume a short-term production rate of 1,600 TPD, while annual emissions assume production of 1,550 TPD.

Unit	Process Rate, TPH	Pollutant	Emission Factor, lb/ton	Emissions	
				lb/hr	TPY
No. 1 High-Pressure Vent	66.7	PM ₁₀ / PM _{2.5}	0.021	1.40	5.94
		CO	0.029	1.93	8.20
No. 1 Low-Pressure Vent	66.7	PM ₁₀ / PM _{2.5}	0.007	0.47	1.98
		CO	0.029	1.93	8.20

EUG 3 Boilers/Heaters > 50 MMBTUH

Post-project emission factors for CO, VOC, SO₂, and PM₁₀ / PM_{2.5} are from AP-42, Section 1.4 (7/98) using a fuel heat content of 1,020 BTU/SCF, and a 50% safety factor was added to the AP-42 factors to account for process variability. NO_x emissions were based on the limitation of OAC 252:100-33 of 0.20 lb/MMBTU. GHG emission factors are based on 40 CFR 98, Subpart C for natural gas combustion.

Unit	Pollutant	Emission Factor, lb/MMBTU	Emissions	
			lb/hr	TPY
403A, No. 1 Urea Plant Boiler No. 1 (84 MMBTUH)	CO	0.126	10.38	45.45
	NO _x	0.20	16.80	73.58
	SO ₂	0.0009	0.07	0.32
	VOC	0.00825	0.68	2.98
	PM ₁₀ / PM _{2.5}	0.0114	0.94	4.11
	GHG	117	9,828	43,050
403B, No. 1 Urea Plant Boiler No. 2 (84 MMBTUH)	CO	0.126	10.38	45.45
	NO _x	0.20	16.80	73.58
	SO ₂	0.0009	0.07	0.32
	VOC	0.00825	0.68	2.98
	PM ₁₀ / PM _{2.5}	0.0114	0.94	4.11
	GHG	117	9,828	43,050

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO		GHG	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
403A	No. 1 Urea Plant Boiler 1	0.94	4.11	0.07	0.32	16.80	73.58	0.68	2.98	10.38	45.45	9,828	43,050
403B	No. 1 Urea Plant Boiler 2	0.94	4.11	0.07	0.32	16.80	73.58	0.68	2.98	10.38	45.45	9,828	43,050
TOTALS		1.88	8.22	0.14	0.64	33.60	147.16	1.36	5.96	20.76	90.90	19,656	86,100

D. Unaffected Existing Units
EUG 3 Boilers/Heaters > 50 MMBTUH

Emission factors for CO, PM₁₀, SO₂, and VOC are from AP-42, Section 1.4 (7/98), and a fuel heating content of 1,020 BTU/SCF. A 150% safety factor was applied to the AP-42 factors to account for process variability. The emission factor for NO_x is based on OAC 252:100-33 limit of 0.2 lb/MMBTU. The annual emission rates for 2202UB are based on 4,380 hours per year operation.

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
3-9099	2202UB	1.6	3.5	0.1	0.2	28.8	63.0	1.2	2.6	17.8	39.0

EUG 4 Boilers/Heaters < 50 MMBTUH

Emission factors for CO, NO_x, PM₁₀, SO₂, and VOC are from AP-42, Section 1.4 (7/98), and a fuel heating content of 1,020 BTU/SCF. A 150% safety factor was applied to the AP-42 factors to account for process variability.

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
4-9102	102B1	0.4	1.6	0.03	0.1	4.9	21.3	0.3	1.2	4.1	17.9
4-9103	102B2	0.4	1.6	0.03	0.1	4.9	21.3	0.3	1.2	4.1	17.9
TOTALS		0.8	3.2	0.06	0.2	9.8	42.6	0.6	2.4	8.1	35.8

EUG 5 No. 1 Urea Plant Conditioning Agent Storage Tank

Maximum emission estimates of formaldehyde from the No. 1 Urea Plant conditioning agent storage tank (EU-D202) are based on a maximum annual loading rate, maximum hourly loading rate, and upper-bound free formaldehyde concentration in the conditioning agent (30% by weight). The emission factor for formaldehyde was derived from the ideal gas law using the partial pressure of a 30% aqueous formaldehyde solution at a maximum anticipated storage temperature.

Point ID	Tank No.	Formaldehyde Emissions	
		lb/hr	TPY
5-9107	D202	1.7	0.10

Methanol emissions from this source are included in EUG 6 as it was conservatively assumed that the methanol contained in the conditioning agent would all be emitted during the granulation process.

EUG 6 No. 1 Urea Plant Granulators

The emission factor for PM is the controlled factor derived from recent stack testing, 0.307 lb/ton from drum granulators, plus a 13% safety factor. It was assumed that PM is equal to PM₁₀.

Formaldehyde factors are from an EPA document, "Locating and Estimating Air Emissions from Sources of Formaldehyde (Revised)", dated March 1991. The EPA document provides a controlled emission factor of 0.0054 lb formaldehyde/ton urea.

Methanol emissions are present in the granulators from the methanol in the conditioning agent. Vendor specifications are "0.1% - 0.3%" methanol, but the concentrations are routinely less than 0.1%. Short-term emission rates were calculated using the maximum stated (0.3%) while annual emissions were estimated using a conservative 0.15%.

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		Formaldehyde		Methanol	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
6-9104	No. 1 Urea Granulator 1	6.60	28.92	0.12	0.51	1.01	2.21
6-9105	No. 1 Urea Granulator 2	6.60	28.92	0.12	0.51	1.01	2.21
6-9106	No. 1 Urea Granulator 3	6.60	28.92	0.12	0.51	1.01	2.21
TOTALS		19.80	86.76	0.36	1.53	3.03	6.62

EUG 10 CO₂ Stripping Towers

Based on process knowledge, a small amount of CO may be present in the CO₂ stream vented from the CO₂ stripper during startup, shutdown, or malfunction events. The emission factor for CO is derived from testing performed in June 2006 for the CO₂ Stripping Tower #1 scaled up to the maximum CO₂ production rate and a safety factor of 300% to account for process variability. Note that CO emissions are only vented from this source during startup, shutdown, or malfunction events; however, for PTE calculations, 8,760 hours/year of venting was assumed.

Point ID	Emission Unit	CO	
		lb/hr	TPY
10-9120	CO ₂ Stripping Tower 1	5.8	25.4
10-9121	CO ₂ Stripping Tower 2	5.8	25.4
TOTALS		11.6	50.8

This EUG also has the potential to emit methanol during periods of startup, shutdown, or malfunction of the ammonia plants. Startup/shutdown emissions are included in EUG 15.

EUG 11 Nitric Acid Plant

Potential emissions of NO_x from this source are based on previously established permit limits from Permit No. 90-140-O. NO_x emissions were calculated based on a permitted concentration of 79 ppmdv and a design exhaust flow rate of 8,817 SCFM. This unit is equipped with a non-selective catalytic reduction system (NSCR) to reduce NO_x emissions.

Start-up and shutdown emissions have been based on 750 ppm, 3 hours per event, 50 events per year.

Point ID	Emission Unit	NO _x	
		lb/hr	TPY
12-9115	Nitric Acid Plant – Normal Operations	5.0	21.9
	Nitric Acid Plant – Start-up and Shutdown	47.5	3.6
TOTALS		47.5	25.5

EUG 12 UAN Plant

The emission factor for PM is a controlled factor from AP-42 Section 8.3. AP-42 provides a wide range of controlled factors for PM, which is based on the type of controls used at the UAN Plant. The maximum PM factor was adjusted to account for the type of controls used at the Enid Plant. It was assumed that PM is equal to PM₁₀. A small amount of CO is present in the CO₂ feed from the urea section of the UAN Plant. A mass balance equation was used to quantify CO emissions.

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		CO	
		lb/hr	TPY	lb/hr	TPY
12-9116	UAN Plant	2.6	11.0	0.1	0.5

EUG 13 Flare

The flare pilot consumes 1,350 SCF/hr natural gas and the flare combusts a maximum 60,000 lb/hr of ammonia. The flare is designed to meet a 98% destruction efficiency. For the combustion of natural gas and ammonia plant purge gas, the emission factors for CO and NO_x are from AP-42 Section 13.5 (dated 9/91, reformatted 1/95). VOC emissions were calculated using a mass balance and based on 98% destruction efficiency. The emission factor for SO₂ is from AP-42 Section 1.4 (dated 7/98). KOCH estimated NO_x emissions from ammonia flaring using emission estimating methodologies from the "Air Permit and Technical Guidance for Chemical Sources: Flares and Oxidizers", Texas Natural Resource Conservation Commission (TNRCC), Air Permits Division, October 2000 (RG-109 Draft).

Point ID	Emission Unit	SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
13-9118	Flare	0.05	0.01	339.3	15.8	80.1	2.3	30.4	3.0

EUG 14 Plant Fugitives

The main source of particulate matter fugitive emissions at the plant consists of urea fugitives from granular urea storage, transfer, and loading (EU UMH). These operations should generate negligible PM₁₀ due to the organic, non-brittle, sticky nature of the material. In addition, the plant adds a conditioning agent that further reduces dust formation.

Point ID	Emission Unit	PM		PM ₁₀	
		lb/hr	TPY	lb/hr	TPY
UMH	No. 1 Urea Handling/ Loading	1.68	2.38	--	--

EUG 14A No. 1 Urea Plant Fugitives

Fugitive emissions associated with the storage, handling, and loading of the urea product are considered negligible due to the characteristics of the material. Urea is a non-brittle, organic, and sticky material that is not likely to generate significant amounts of dust or particulate emissions during material handling. A sieve analysis of urea product showed no measurable PM₁₀. Using the methods of AP-42 (1/95) for batch drop operations will greatly overstate emissions.

Point ID	Emission Unit	PM		PM ₁₀	
		lb/hr	TPY	lb/hr	TPY
UMS	No. 1 Urea Materials Storage	0.04	0.20	--	--
UMH	No. 1 Urea Materials Handling	0.35	0.25	--	--
UML	No. 1 Urea Materials Loading	7.04	5.14	--	--
TOTALS		7.41	5.49	--	--

EUG 15 Startup/Shutdown Vents

The ammonia plant startup and shutdown vents (EUs SP73-1 and SP73-2) have the potential to emit large quantities of CO for a short period of time from pressure control valves located within each plant. A total of 63 hours/year was assumed. Potential emission rates are based on process flow rates and stream composition data.

Potential methanol emissions from the CO₂ stripping towers (EU 1102E1 and 1102E2) were estimated based on the data from the June 2006 test for the #1 CO₂ stripping tower. The test results were scaled up to the maximum CO₂ production rate. It was assumed that methanol emissions from the #2 CO₂ stripping tower are equivalent to the #1 CO₂ stripping tower. A total of 36 hours/year from each vent was assumed PTE calculation purposes. Note that the potential methanol emissions are estimates only and are not intended to be used as individual emission unit limits in the permit since methanol emissions have been included in the Plant-wide cap.

The Process Condensate Stripper (EU 308E) has the potential to emit methanol only during unanticipated, unforeseen emergencies. Typically, this source does not vent to the atmosphere due to the process condensate recycle system. Potential methanol emissions from EU 308E have been estimated based on the maximum anticipated condensate flow rate and maximum anticipated methanol content. For annual emissions it was conservatively estimated that the plant would experience 36 hours per year of unforeseen releases. During plant maintenance, process condensate may be routed to the zero discharge pond. From the zero discharge pond, the water is sent to the wastewater concentrator. During these events, the methanol in the condensate may be evaporated from the wastewater concentrator; however, methanol emissions have been accounted for under the plant-wide cap as if they were emitted from the vent rather than the wastewater concentrator.

Point ID	Emission Unit	CO		Methanol	
		lb/hr	TPY	lb/hr	TPY*
15-9151	Ammonia Plant 1 SU/SD Vent No.1 (PV-102 & PV-5)	10,962.8	345.3	--	--
15-9154	Ammonia Plant 2 SU/SD Vent No.1 (PV-102 & PV-5)	10,962.8	345.3	--	--
15-9120	CO ₂ Stripping Tower 1 (PV30-1)	--	--	35.8	0.6
15-9121	CO ₂ Stripping Tower 2 (PV30-2)	--	--	35.8	0.6
15-9109	Process Condensate Stripper (308E)	--	--	131.9	2.4
TOTALS		21925.6	690.6	203.5	3.6

*Annual emissions of methanol have been included in the EUG-1 plant-wide cap, and any one source may emit up to 9.9 TPY so long as all sources combined emit less than 9.9 TPY.

Note that the potential methanol emissions are estimates only and are not intended to be used as individual emission unit limits in the permit since methanol emissions have been included in the plant-wide cap.

EUG 16 No. 1 Urea Plant Cooling Tower No. 2

PM₁₀ emissions from No. 1 Urea Cooling Tower No. 2 were calculated based on a maximum water circulation rate of 12,000 GPM, total dissolved solids of 3,500 ppm by weight, and a drift factor of 0.002%.

Point ID	Emission Unit	PM ₁₀	
		lb/hr	TPY
22014E	No. 1 Urea Plant Cooling Tower	0.42	1.84

EUG 17 Insignificant Activities

Emissions estimates from the portable fertilizer mixing unit, which is owned, operated, and maintained by a contractor, are based on 350 hours/year anticipated operation and manufacturer's data.

Emission Unit	PM ₁₀		SO ₂		NO _x		VOC		CO	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Glycol dehydration reboiler	0.01	0.05	0.01	0.01	0.2	0.6	0.01	0.04	0.1	0.5
475-hp Portable mixer engine	0.01	0.05	0.01	0.03	0.3	1.5	0.01	0.06	0.1	0.03
APP Portable 10-34-0 processing unit	--	--	--	--	--	--	--	--	--	--
Diesel storage tanks (3)	--	--	--	--	--	--	--	0.1	--	--
UAN tanks (2)	--	--	--	--	--	--	--	--	--	--
Lime silos (2)	0.2	0.7	--	--	--	--	--	--	--	--

Emission Unit	PM ₁₀		SO ₂		NO _x		VOC		CO	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
No. 1 Ammonia Plant TV-50 vent	--	--	--	--	--	--	104.3	4.9	--	--
No. 1 Ammonia Plant PIC-14 fuel vent	--	--	--	--	--	--	10.4	0.6	--	--
No. 1 Ammonia Plant PIC-33 fuel vent	--	--	--	--	--	--	10.4	0.6	--	--
No. 1 Ammonia Plant catalyst warm-up vent (SP-73)	--	--	--	--	--	--	104.3	1.9	--	--
No. 1 Ammonia Plant Low-Shift Reductions vent(SP-73)	--	--	--	--	--	--	291.4	4.1	--	--
No. 1 Ammonia Plant LTS Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
No. 1 Ammonia Plant HTS Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
No. 1 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
No. 2 Ammonia Plant TV-50 vent	--	--	--	--	--	--	104.3	4.9	--	--
No. 2 Ammonia Plant PIC-14 fuel vent	--	--	--	--	--	--	10.4	0.6	--	--
No. 2 Ammonia Plant PIC-33 fuel vent	--	--	--	--	--	--	10.4	0.6	--	--
No. 2 Ammonia Plant catalyst warm-up vent (SP-73)	--	--	--	--	--	--	104.3	1.9	--	--
No. 2 Ammonia Plant Low-Shift Reductions vent (SP-73)	--	--	--	--	--	--	291.4	4.1	--	--
No. 2 Ammonia Plant LTS Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
No. 2 Ammonia Plant HTS Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
No. 2 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)	--	--	--	--	--	--	208.7	0.4	--	--
Laboratory Vents	--	--	--	--	--	--	--	<5	--	--
No. 2 Urea Plant Conditioning Agent Tank	--	--	--	--	--	--	--	0.14		
TOTALS	0.22	0.8	0.01	0.04	0.5	2.1	2293.8	26.7	0.2	0.53

EUG 18. Emergency Engines Subject to NSPS Subpart JJJJ

Emissions factors for NO_x, CO, and VOC are NSPS Subpart JJJJ limits. Emissions of PM and SO₂ are taken from AP-42 (7/00), Section 3.2. Since PM is from natural gas combustion, PM_{2.5} is assumed equal to PM. 500 hours per year operations were used.

Rated Horsepower	Pollutant	Emission Factor	Emissions	
			lb/hr	TPY
GEN2 : 147-hp (1.24 MMBTUH)	NO _x	2.0 g/hp-hr	0.65	0.16
	CO	4.0 g/hp-hr	1.30	0.32
	VOC	1.0 g/hp-hr	0.32	0.08
	SO ₂	0.0006 lb/MMBTU	0.01	0.01
	PM ₁₀ / PM _{2.5}	0.0194 lb/MMBTU	0.02	0.01
GEN3 :40-hp (0.38 MMBTUH)	NO _x	10 g/hp-hr	0.88	0.22
	CO	387 g/hp-hr	34.13	8.53
	VOC	0.0296 lb/MMBTU	0.01	0.01
	SO ₂	0.0006 lb/MMBTU	0.01	0.01
	PM ₁₀ / PM _{2.5}	0.0194 lb/MMBTU	0.01	0.01

EUG 19. Diesel Engines Subject to NESHAP Subpart ZZZZ

Estimates of emissions from the emergency generator and the fire water pump are based on 500 hours of operations per year, with emission factors from Table 3.3-1 of AP-42 (10/96).

Emission Unit	PM ₁₀		SO ₂		NO _x		VOC		CO	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
GEN : 460-hp Generator	1.1	0.3	0.9	0.2	14.3	3.6	1.2	0.3	3.1	0.8
PUMP: 145-hp Fire Pump	0.3	0.1	0.3	0.1	4.5	1.1	0.4	0.1	1.0	0.2
TOTALS	1.4	0.4	1.2	0.3	18.8	4.7	1.6	0.4	4.1	1.0

EUG 20. Gasoline Tank

VOC emissions are based on an annual throughput of 6,430 gallons, vapor pressure of 6.6 psia, and molecular weight of 66.

NET EMISSIONS CHANGES

The initial step in the process of determining net emissions changes was summing the post-project potential emissions for each new unit, each modified unit, and each unit with increased utilization. These totals exceeded the PSD levels of significance for NO_x, CO, VOC, PM_{2.5}/PM₁₀, and GHG (but not SO₂), requiring determination of net emissions changes.

Net emissions changes for the project were calculated by using the post-project potential emissions for each new unit, each modified unit, and each unit with increased utilization compared to the Baseline Actual Emissions (BAE) for each. The Projected Actual Emissions (PAE) for each modified and increase-utilization unit were taken as PTE.

The BAE period for all pollutants other than NO_x was the 24-month period from September 2010 to August 2012; for NO_x, the BAE period was March 2009 to February 2011.

The only contemporaneous projects were a modification to the two primary reformers and a upgrade to the UAN plant. The reformer project is accounted for in the emissions changes of those two reformers, and the UAN DCS upgrade project (19 TPY NO_x addition) has been accounted for as a contemporaneous change.

Pre-Project Baseline Actual Emissions from Affected Units

Unit	CO TPY	NO_x TPY	PM₁₀ TPY	PM_{2.5} TPY	VOC TPY	SO₂ TPY	GHG TPY
No. 1 Ammonia Plant Primary Reformer	0.68	332.81	28.38	28.38	20.54	2.24	445,682
No. 2 Ammonia Plant Primary Reformer	31.61	411.80	26.17	26.17	18.94	2.07	410,922
Ammonia Plant Process CO ₂ Emissions	--	--	--	--	--	--	486,234
No. 1 Urea Plant Boiler No. 1	28.74	72.63	2.60	2.60	1.88	0.21	40,839
No. 1 Urea Plant Boiler No. 2	28.74	72.73	2.60	2.60	1.88	0.21	40,839
No. 1 Urea Plant Synthesis Vents	8.83	--	4.26	4.26	--	--	--
No. 2 Ammonia Plant Cooling Tower	--	--	1.59	0.01	--	--	--
TOTALS	98.60	889.97	65.60	64.02	43.24	4.73	1,424,516

Post-Project Potential Emissions

Unit	CO TPY	NO _x TPY	PM ₁₀ TPY	PM _{2.5} TPY	VOC TPY	SO ₂ TPY	GHG TPY
No. 1 Ammonia Plant Primary Reformer	348.08	500.86	31.49	31.49	28.49	3.73	494,565
No. 2 Ammonia Plant Primary Reformer	357.10	173.45	32.31	32.31	29.23	3.83	507,378
Ammonia Plant Process CO ₂ Emissions	--	--	--	--	--	--	1,260,000
No. 1 Urea Plant Boiler No. 1	45.45	73.58	4.11	4.11	2.98	0.32	43,050
No. 1 Urea Plant Boiler No. 2	45.45	73.58	4.11	4.11	2.98	0.32	43,050
No. 1 Urea Plant HP Synthesis Vent	8.20	--	5.94	--	--	--	--
No. 1 Urea Plant LP Synthesis Vent	8.20	--	1.98	--	--	--	--
No. 2 Urea Plant Synthesis Vent	12.83	--	0.20	0.20	--	--	--
No. 2 Urea Plant Granulator	--	--	26.45	26.45	8.44	--	--
No. 2 Urea Plant Boiler	72.93	88.70	14.69	14.69	10.63	1.16	230,626
No. 2 Urea Plant Cooling Tower	--	--	0.86	0.01	--	--	--
No. 2 Ammonia Plant Added Cooling Tower	--	--	2.02	0.01	--	--	--
No. 2 Urea Plant Conditioning Agent Tank	--	--	--	--	0.14	--	--
New Haul Roads	--	--	0.38	0.09	--	--	--
No. 2 Urea Plant Loading	--	--	0.04	0.03	--	--	--
No. 2 Urea Plant Storage	--	--	0.12	0.08	--	--	--
No. 2 Urea Plant Transfer	--	--	0.11	0.07	--	--	--
UAN Plant Upgrade Project Contemporaneous Emission Change (Permit No. 99-092-C (M-5))	--	19	--	--	--	--	--
TOTALS	898.24	929.17	124.81	113.65	82.89	9.36	2,578,669
PRE-PROJECT BAE	98.60	889.97	65.60	64.02	43.24	4.73	1,424,516
NET CHANGES	799.65	39.2	59.21	49.63	39.65	4.63	1,154,153
PSD LEVELS OF SIGNIFICANCE	100	40	15	10	40	40	75,000
SUBJECT TO PSD?	Yes	No	Yes	Yes	No	No	Yes

FACILITY-WIDE CRITERIA POLLUTANT EMISSION SUMMARY (PTE)

EUG	Description	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
EUG 2A	Ammonia Plant #1	8.02	31.49	0.95	3.73	215.20	500.86	8.70	28.49	88.61	348.08
EUG 2B	Ammonia Plant #2	10.06	32.31	1.19	3.83	270.00	173.45	5.5	29.23	111.18	357.10
EUG 3	Heaters/Boilers > 50 MMBTUH	3.48	11.72	0.24	0.84	62.40	210.16	2.56	8.56	38.56	129.90
EUG 4	Heaters/Boilers < 50 MMBTUH	0.8	3.2	0.06	0.2	9.8	42.6	0.6	2.4	8.2	35.8
EUG 5	No. 1 Urea Conditioning Agent Storage Tank	--	--	--	--	--	--	1.7	0.1	--	--
EUG 6	No. 1 Urea Granulators	19.80	86.76	--	--	--	--	3.69	8.15	--	--
EUG 7	No. 1 Urea Synthesis Vents	1.87	7.92	--	--	--	--	--	--	3.87	16.41
EUG 9	No. 2 Ammonia Cooling Tower	0.46	2.02	--	--	--	--	--	--	--	--
EUG 10	CO ₂ Stripping Towers	--	--	--	--	--	--	--	--	11.6	50.8
EUG 11	Nitric Acid Plant	--	--	--	--	47.4	25.5	--	--	--	--
EUG 12	UAN Plant	2.6	11.0	--	--	--	--	--	--	0.1	0.5
EUG 13	Flare	--	--	0.05	0.01	339.3	15.8	80.1	2.3	30.4	3.0
EUG 14	No. 1 Urea Plant Fugitives	--	--	--	--	--	--	--	--	--	--
EUG 14A	No. 1 Urea Fugitives	--	--	--	--	--	--	--	--	--	--
EUG 15	Start-up/Shutdown Vents	--	--	--	--	--	--	203.5	--	21,925.6	690.6
EUG 16	No. 1 Urea Cooling Tower No. 2	0.42	1.84	--	--	--	--	--	--	--	--
EUG 17	Insignificant Activities	0.2	0.8	0.01	0.01	0.5	2.1	2293.8	26.84	0.2	0.6
EUG 18	Emergency Engines	0.03	0.02	0.02	0.02	1.53	0.38	0.33	0.1	35.43	8.85
EUG 19	Diesel Engines	1.4	0.4	1.2	0.3	18.8	4.7	1.6	0.4	4.1	1.0
EUG 20	Vehicle Fueling	--	--	--	--	--	--	--	0.14	--	--
EUG 21	No. 2 Urea Plant	0.05	0.20	--	--	--	--	--	--	3.08	12.83
EUG 22	No. 2 Urea Granulator	6.04	26.45	--	--	--	--	2.39	8.44	--	--
EUG 23	No. 2 Urea Plant Boiler	3.35	14.69	0.26	1.16	20.25	88.70	2.43	10.63	16.65	72.93
EUG 25	No. 2 Urea Plant Cooling Tower	0.20	0.86	--	--	--	--	--	--	--	--
EUG 26	No. 2 Urea Plant Loading, Transfer, Storage	0.17	0.26	--	--	--	--	--	--	--	--
EUG 27	No. 2 Urea Plant Haul Roads	0.20	0.38	--	--	--	--	--	--	--	--
	TOTALS	59.15	232.32	3.98	10.10	985.18	1064.25	2606.9	125.78	22277.6	1728.4

FACILITY-WIDE HAP EMISSIONS SUMMARY (PTE)

Emission Unit Group	Formaldehyde		Methanol*	
	lb/hr	TPY	lb/hr	TPY
EUG 1 – Plant-wide	--	--	--	*
EUG 2A – Ammonia Reformers	0.07	0.3	--	--
EUG 2B – Ammonia Reformers	0.07	0.3	--	--
EUG 3 – Heaters > 50 MMBTUH	0.06	0.1	--	--
EUG 4 – Heaters < 50 MMBTUH	0.006	0.02	--	--
EUG 5 – No. 1 Urea Conditioning Agent Storage Tank	1.7	0.1	--	--
EUG 6 – No. 1 Urea Plant Granulators	0.4	1.5	3.0	*
EUG 15 – Start-up/Shutdown Vents	--	--	203.5	*
EUG-22 – No. 2 Urea Plant Granulator	0.76	3.34	1.41	*
EUG-17 – No. 2 Urea Conditioning Agent Storage Tank	1.7	0.14	*	*
EUG 23 – No. 2 Urea Plant Boiler	0.03	0.13	--	--
TOTALS	4.8	5.93	207.9	9.9

* Methanol emissions are included in the plant-wide cap, which allows any one source to emit up to 9.9 TPY so long as all sources combined emit less than 9.9 TPY. The cap is addressed in the Specific Conditions for EUG 1.

POTENTIAL GREENHOUSE GAS EMISSIONS

Activity	CO₂-Equivalent Emissions, TPY
No. 1 Ammonia Plant Reformer	551,453
No. 2 Ammonia Plant Reformer	691,879
No. 1 and No. 2 Ammonia Plant Process CO ₂	1,260,000
#1 Nitric Acid Plant	1,142
Ammonia Unit Start-up Boiler	36,898
Urea Boiler No. 1	43,050
Urea Boiler No. 2	43,050
Ammonia Unit Start-up Heater No. 1	16,912
Ammonia Unit Start-up Heater No. 2	16,912
Diesel-fired Emergency Engines	172
Gas-fired Emergency Engines	49
No. 2 Urea Plant Boiler	230,626
TOTALS	2,892,143

*The emissions above were estimated using the methodologies under 40 CFR 98. The 1,655,639 tons per year is for unlimited production. The permit will limit the process CO₂ emissions to 1,260,000 tons per year.

SECTION VII. BACT REVIEW

OAC 252:100-8-31 states that BACT “*means an emissions limitation (including a visible emissions standard) based on the maximum degree of reduction for each regulated NSR pollutant which would be emitted from any proposed major stationary source or major modification which the Director, on a case-by-case basis, taking into account energy, environmental, and economic impacts or other costs, determines is achievable for such source or modification....*” A BACT analysis is required to assess the appropriate level of control for each new or physically modified emissions unit for each pollutant that exceeds the applicable PSD Significant Emissions Rate (SER).

The U.S. EPA has stated its preference for a “top-down” approach for determining BACT and that is the methodology used for this permit review. After determining whether any New Source Performance Standard (NSPS) is applicable, the first step in this approach is to determine, for the emission unit in question, the available control technologies, including the most stringent control technology, for a similar or identical source or source category. If the proposed BACT is equivalent to the most stringent emission limit, no further analysis is necessary.

If the most stringent emission limit is not selected, further analyses are required. Once the most stringent emission control technology has been identified, its technical feasibility must be determined; this leads to the reason for the term “available” in Best Available Control Technology. A technology that is available and is applicable to the source under review is considered technically feasible. A control technology is considered available if it has reached the licensing and commercial sales stage of development. In general, a control option is considered applicable if it has been, or is soon to be, developed on the same or similar source type. If the control technology is feasible, that control is considered to be BACT unless economic, energy, or environmental impacts preclude its use. This process defines the “best” term in Best Available Control Technology. If any of the control technologies are technically infeasible for the emission unit in question, that control technology is eliminated from consideration.

The remaining control technologies are then ranked by effectiveness and evaluated based on energy, environmental, and economic impacts beginning with the most stringent remaining technology. If it can be shown that this level of control should not be selected based on energy, environmental, or economic impacts, then the next most stringent level of control is evaluated. This process continues until the BACT level under consideration cannot be eliminated by any energy, environmental, or economic concerns.

The following resources were utilized in the BACT analysis:

- EPA’s RACT/BACT/LAER (RBLC) Clearinghouse.
- Federal / state / local new source review permits, permit applications, and associated inspection and testing reports.
- Technical journals, newsletters, and reports, including the “Report of the Interagency Task Force on Carbon Capture and Storage” (August 2010).
- Information from air quality control technology suppliers.
- Engineering designs on related projects.

- “PSD and Title V Permitting Guidance for Greenhouse Gases” (EPA-457/B-11-001, March 2011).
- “New Source Review Workshop Manual” (Draft, October 1990).

The five basic steps of a top-down BACT review are summarized as follows:

- Step 1. Identify Available Control Technologies
- Step 2. Eliminate Technically Infeasible Options
- Step 3. Rank Remaining Control Technologies by Control Effectiveness
- Step 4. Evaluate Most Effective Controls Based on Energy, Environmental, and Economic impacts
- Step 5. Select BACT and Document the Selection as BACT

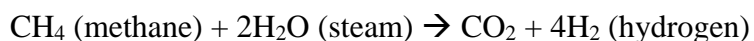
The following table summarizes the new and modified units subject to BACT review:

Unit	Pollutants Subject to BACT
Existing No. 1 Ammonia Plant Primary Reformer	PM, CO, GHG
Existing No. 2 Ammonia Plant Primary Reformer	PM, CO, GHG
Added Cooling Tower Cell at Ammonia Plant	PM
Existing CO ₂ Process Venting	GHG
Existing No. 1 Urea Plant Synthesis Vents	PM, CO
New No. 2 Urea Plant Cooling Tower	PM
New No. 2 Urea Plant Synthesis Vents	PM, CO
New No. 2 Urea Plant Granulators	PM
New No. 2 Urea Plant Boiler	PM, CO, GHG
New No. 2 Urea Plant Conveying, Storage, and Loading	PM
New Haul Roads	PM

A. Greenhouse Gases

For the purpose of this analysis, GHG is assumed to be composed primarily of CO₂, with much smaller quantities of CH₄ and N₂O. Under EPA’s new guidelines for GHG BACT, the typical top-down analysis approach is to be followed. Since CO₂ is not typically feasible to control, the available control options focus on potential improved process efficiency, leading to improved fuel efficiency, rather than end-of-stack types of control systems.

The majority of the CO₂ emitted is generated from combustion, but some is generated from the steam reforming reaction, which creates hydrogen for production of ammonia:



That concentrated CO₂ can be used for urea synthesis and for food or enhanced oil recovery purposes, depending on markets. When the markets are good, the plant uses CO₂ as a marketable product; but when markets are not good, the plant can only use CO₂ to the limits of usage in urea synthesis, and the excess must be vented.

The BACT analysis looks at combustion sources and process sources separately.

i. Combustion Sources

Step 1. Identify Available Control Technologies

Potentially-applicable control technologies include add-on controls, inherently lower-emitting processes, practices, and designs, and combinations of the two. Since CO₂ is created as an unavoidable product of both natural gas combustion and the steam reforming reaction, identification of available controls will focus on lower-emitting processes, practices, and designs. Although many alternatives will be eliminated in following steps, Step 1 should include all potential and relevant options. The following references were consulted in identifying potential control measures:

The following potential GHG controls were identified:

- Carbon capture and sequestration (CCS)
- Combined heat and power cogenerations (CHP)
- Operational energy efficiency measures
- Design energy efficiency measures
- Alternative fuels

Natural gas has the lowest carbon content of any conventional fuel. Hydrogen as fuel has no carbon, but it must first be generated by reaction with carbon-containing fuels, normally methane; in this plant, unused hydrogen from ammonia synthesis is used as fuel. Biofuels may result in no net CO₂ emissions when such fuels are available.

Energy efficiency measures minimize the amount of fuels needed. The following design energy efficiency measures were identified:

- Insulation of heat exchange components, minimizing heat loss.
- A damper in the reformer stack to minimize heat loss during shutdown.
- Optimal heat exchanger design.
- Improvements to radiant and convective heat exchange areas in the reformers.
- Combustion air pre-heating.
- A feed stream saturator injects water into reformer feed, making steam in-situ from available heat.

Operational efficiency measures identified included:

- Periodic maintenance and tuning to maintain/restore optimal efficiency.
- Instrumentation and controls, allowing monitoring of process operations and directing of fuel and air flows for maximum effect.
- Minimizing heat exchange surface fouling to retain efficiency.
- Reduced steam losses from a program of locating and repairing steam leaks.

Combined heat and power cogeneration (CHP) uses hot exhaust gases for generation of steam for process needs and in turning mechanical equipment. The process relies on there being significant temperature and oxygen concentrations in the exhausts. CHP is used at the Enid facility.

Carbon capture and sequestration (CCS) is a “tailpipe” control process in which CO₂ is injected into deep aquifers, depleted oil and gas reservoirs, un-mineable coal seals, or existing oil fields (as an enhanced oil recovery process). The process may be conducted either by using an amine unit to separate out CO₂ from the remainder of flue gases, or the entire stream may be injected. There is an experimental process being developed for coal-fired power plants that conducts firing with high-purity oxygen rather than air, yielding an exhaust stream that is mostly CO₂ and water. The overall system requires capture of adequate efficiency, available transportation (pipelines or trucks), and an end destination; without any one of these, the process does not function.

The following table shows the results of a search of EPA’s RBLC for BACT for sources of greenhouse gas emissions.

Natural Gas Fired Boilers > 250 MMBTUH – Greenhouse Gases

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Good combustion practices, 117 lb/MMBTU CO ₂
FL-0330	Port Dolphin Energy	Florida	12/01/11	Tuning, optimization, instrumentation and controls, insulation, 117 lb/MMBTU CO ₂
IA-0106	CF Industries	Iowa	7/12/13	Proper operation, natural gas, 117 lb/MMBTU CO ₂
LA-0254	Ninemile Point Generating	Louisiana	8/16/11	Proper operation and good combustion, 117 lb/MMBTU CO ₂
NE-0054	Cargill, Inc.	Nebraska	3/01/13	Good combustion practices

Natural Gas Fired Primary Reformers – Greenhouse Gases

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Good combustion practices, 117 lb/MMBTU CO ₂

The prevailing limitation is 117 lb/MMBTU, which is equal to the emission factor from 40 CFR Part 98.

Step 2. Eliminate Technically Infeasible Options

The list of potential control technologies identified in Step 1 are evaluated for technical feasibility. EPA considers technologies to be technically feasible if:

- They have been demonstrated and operated successfully at a similar source, and
- They are available and applicable to the source under review.

Technologies in the pilot or R&D phases are not considered to be “available.”

CCS: For carbon capture and sequestration (CCS) to be technically feasible, each of three distinct activities must be feasible: CO₂ capture, transport and storage.

- ***Carbon Capture.*** Carbon capture has not been installed and operated successfully on combustion sources similar to Enid’s primary reformers and natural gas-fired boilers and therefore has not been demonstrated. Scrubbing has not been shown feasible, in part because an amine or caustic solution would have to be used to strip up to 90% of CO₂, requiring large amounts of steam which would, in turn, create additional GHGs and criteria pollutant emissions; oxy combustion has not been demonstrated for natural gas combustion; and membrane absorption has not been demonstrated for natural gas fuel. Accordingly, carbon capture is not “applicable” to the combustion sources that are part of the Project.

Carbon capture is also not “applicable” to the combustion sources because the physical and chemical characteristics of the pollutant-bearing gas stream are different from other gas streams for which carbon capture technologies have been tested. EPA’s recently proposed NSPS for GHGs from electric generating units supports these conclusions, as does the National Energy Technology Laboratory, and several PSD permits identified in the RBLC.

- ***Carbon Storage.*** Currently-available forms of EOR are not technically feasible as permanent geologic sequestration of CO₂. According to EPA’s recently proposed NSPS for GHGs from EGUs, EOR is only technically feasible if it is compliant with 40 CFR Part 98, Subpart RR. (“If the captured CO₂ is sent offsite, then the facility injecting the CO₂ underground must report under 40 CFR Part 98 subpart RR.”). EOR facilities that are not subject to and compliant with Subpart RR are therefore insufficient to satisfy the permanence requirement for geologic sequestration and cannot qualify as BACT. Based on Part 98 reported data available as of this date, there is no current EOR operation that is compliant with Subpart RR. Accordingly, sequestration at Subpart RR EOR facilities is not “demonstrated” for the purposes of BACT. The EOR field to which KOCH’s customer, Merit Energy Company, currently sells the CO₂ product, is not—according to EPA’s Part 98 data—a Subpart RR EOR facility.

Permanent geological sequestration of CO₂ is not a demonstrated technology. The active and planned sequestration projects in the United States and Canada are not demonstrated. The NETL's 2012 Carbon Utilization and Storage Atlas identifies three active large-scale CO₂ injection projects in the United States and Canada, only one of which is a non-EOR sequestration project (Illinois Basin—Mt. Simon Sandstone, near Decatur, Illinois). For planned projects, only the Kevin Dome project in Montana is a non-EOR storage project. None of the active or planned projects has demonstrated the capability to accept 1,318,600 tons per year of CO₂ from Enid. The largest active injection site (SECARB's Cranfield EOR Field) has a *total* capacity of only 3.4 million metric tons. Further, NETL describes these sites as being evaluated to "validate" the hypothesis that carbon capture, use, and sequestration can be conducted at a commercial scale.

Because of the injection volume limitations of these projects, along with the uncertainty associated with the fate of injected CO₂, long-term geologic sequestration has not been successfully applied to the type of source under review. For these reasons, permanent geologic sequestration is not a demonstrated technology for purposes of the Project.

Permanent geological sequestration of CO₂ is not an available technology. The large-scale CO₂ storage projects identified by NETL have not yet reached the licensing and commercial stage of development. These projects are public-private partnerships, with significant government financial support. The stated purpose of the projects is to "validate that CCS can be conducted at a commercial scale." The relatively small storage capacities of these projects (the largest of which is only 3.4 million metric tons) supports that they are pilot scale. Technologies in the pilot scale testing stages of development are not considered "available" technologies. Because these pilot scale projects have not yet reached the licensing and commercial stage of development, permanent geological sequestration of CO₂ is not an available technology.

Permanent geological sequestration of CO₂ is not an applicable technology. The large-scale CO₂ storage projects identified by NETL cannot accept the quantity of CO₂ that would be produced over the life of the project. NETL itself is assessing whether these projects have the capacity to reliably store CO₂ long-term without adverse human health or environmental impacts, and so these projects cannot reliably provide permanent CO₂ sequestration for the Project.

- ***Carbon Transportation*** CO₂ transportation to permanent geological sequestration sites is not a demonstrated technology. There is no CO₂ pipeline that has been installed and operated successfully connecting an anthropogenic CO₂ source like the project to a permanent geologic sequestration site with sufficient capacity to accept such volumes long term.

CO₂ transportation to permanent geological sequestration sites is not an applicable technology. Because there are no technically feasible, large-capacity, reliable, permanent geological sequestration sites, any CO₂ pipeline from the Project would be a pipeline to an indeterminate location. Even if one of the large-scale carbon sequestration projects in NETL's 2012 Atlas were hypothetically capable of serving the project, the logistical hurdles of constructing, owning, and operating a high-capacity CO₂ pipeline to one of those sites are high. For example, the closest non-EOR sequestration site noted by NETL would be the Archer Daniels Midland sequestration demonstration project near Decatur, Illinois, approximately 535 miles away from the project. Issues such as obtaining contracts for offsite land acquisition (including the availability of land) and the timing of when the new pipeline would be available relative to the startup of the proposed project would be extraordinarily difficult to overcome.

CO₂ transportation to Subpart RR-compliant EOR facilities is neither demonstrated, nor applicable. The existing CO₂ compressor and pipeline system at the facility is owned and operated by Merit Energy Company, an independent company, and is used to transport a portion of the current CO₂ production off site for use in EOR. As the compressor and pipeline system are owned and operated by Merit, KOCH does not control use or maintenance and therefore cannot assure the availability or the reliability of this equipment as a transport system for any particular future needs for purposes of a CO₂ control strategy. In addition, because the existing pipeline leads to an EOR field that is not Subpart RR compliant, for the reasons stated above CO₂ transportation through this pipeline is neither demonstrated nor applicable and is currently technically infeasible. Since a sequestration site cannot be identified that meets the required availability criteria or assure longevity or viability, the use of an EOR pipeline as part of a CO₂ reduction strategy cannot be assured for the life of the Project, and geologic sequestration is not considered an applicable technology.

In summary, because each of the three components of CCS, namely capture, transport and long-term permanent storage is technically infeasible for the life of the project, CCS as a whole is technically infeasible as BACT for the proposed Project.

Alternative Fuels: Natural gas is the lowest GHG emitting fuel and is a feedstock for the reformer process. Alternative fuels would have to be gasified prior to introduction into the process. They are, therefore, infeasible.

The remaining three options (combined heat and power cogeneration, operational energy efficiency measures, and design energy efficiency measures) are currently being conducted at the Enid facility, therefore are both demonstrated and available.

Step 3 Rank Remaining Control Technologies by Control Effectiveness

The following table shows the remaining controls:

Control Technology Option	Estimated GHG Emission Reduction	Estimated Energy Efficiency Increase	Reference
Maintenance and Fouling Control	1-10% of process heater emissions	3-6%	October 2010 EPA GHG BACT Guidance & Energy Star Guide (LBNL-56183, February 2005)
Combustion Air and Feed/Steam Preheat	5% compared to typical reformer	5% compared to typical reformer	October 2010 EPA GHG BACT Guidance
Combustion Air Controls	1-3% of heater emissions	1-3%	October 2010 EPA GHG BACT Guidance
Combined Heat and Power Generation	No data available	No data	--

Step 4. Evaluate Most Effective Controls Based on Energy, Environmental, and Economic Impacts

Under the top-down approach, the highest ranking option is considered first and is evaluated on the basis of cost and collateral environmental impact. Since the highest ranking three options are incorporated in the proposed boiler and modified reformer heaters, along with several other options, costs have not been evaluated.

Though CCS has been found not to be technically feasible under Step 2, and therefore need not be ranked under Step 3 nor evaluated under Step 4, KOCH voluntarily provided an analysis of economic feasibility and of the energy and environmental impacts of CCS in its application. KOCH concluded that the capital costs associated with implementing CCS for the reformer and boilers, comprised of a CO₂ scrubber, compressor and pipeline (from Enid, OK to Decatur, IL), would be approximately \$841,000,000 to \$903,000,000. Based on recent economic infeasibility analyses by EPA Region VI in support of BACT decisions for GHG PSD permits, these capital cost analyses are reasonable estimates, and if they were necessary for the BACT analysis we would conclude that the use of CCS in the proposed project would make the project economically infeasible. The energy and environmental impacts analysis set forth in the permit application further support the conclusion that CCS is not BACT.

Step 5. Select BACT and Document the Selection as BACT

The following combination of energy efficiency techniques is selected as BACT:

- Combined heat and power cogenerations (CHP)
- Operational energy efficiency measures
- Design energy efficiency measures

A limit of 117 lb/MMBTU CO₂ will be established for new and modified combustion sources.

ii. Process Sources

Step 1. Identify Available Control Technologies

The application identified the following potential control technologies:

- Carbon capture and sequestration (CCS)
- Good design practices
- Good operating practices

The category, “Good design practices,” includes the following items:

- Improved CO₂ removal
- Small catalyst in ammonia converters
- Hydrogen recovery from purge gas.

These items focus both on optimal recovery of CO₂ and minimizing generation of CO₂ in reforming; the more hydrogen is recovered and recycled, the less that must be generated. The “small catalyst” refers to a configuration with reduced pressure drop, which reduces energy consumption in pushing reactants through the catalyst.

The category, “Good operating practices,” includes the following items:

- Maintenance of pressure balance between ammonia and urea plants, minimizing venting of CO₂

CO₂ is a feed for urea formation. The more efficiently it is supplied (not oversupplied) to the urea reactor, the less is vented from the urea reactor.

The following table shows the results of a search of EPA’s RBLC for BACT for sources of greenhouse gas emissions: process sources.

Carbon Dioxide Regenerators – Greenhouse Gases

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Not stated
IA-0106	CF Industries	Iowa	7/12/13	Not stated

Step 2. Eliminate Technically Infeasible Options

Similarly to combustion units, carbon capture and sequestration is not a demonstrated technology. The technology necessary to recover process CO₂ from the ammonia synthesis process has been demonstrated and operated successfully, and is available and applicable, and therefore the capture of process CO₂ from this source is technically feasible. However, the transportation and permanent storage of process CO₂ generated at this facility that is not sold as a product are both technically infeasible, based on the same conclusions set forth above. Since two of the three components of CCS are technically infeasible, CCS is considered technically infeasible as a control technology. All other controls mentioned in Step 1 are either currently in use or are being designed into the system.

Step 3. Rank Remaining Control Technologies by Control Effectiveness

Data are not yet available to complete such a ranking since most ammonia process systems, including this facility, are designed and operated with all remaining controls in place, therefore it is not possible to evaluate the effects of individual measures.

Step 4. Evaluate Most Effective Controls Based on Energy, Environmental, and Economic Impacts

As stated above in the Combustion CO₂ step 4 evaluation, an economic evaluation was completed for CCS. CCS as a control strategy for process CO₂ emissions is not economically feasible. The most effective feasible controls are being designed into the proposed project.

Step 5. Select BACT and Document the Selection as BACT

The following combination of energy efficiency techniques is selected as BACT:

- Good design practices
- Good operating practices

The facility is proposing a limit of CO₂ emissions of 1,260,000 tons per year, 12-month rolling total.

B. CO BACT Review

Carbon monoxide is formed primarily as a result of incomplete combustion of fuel, and to a lesser degree, from incomplete reaction in steam reforming; over 98% of CO emitted is from combustion units. For combustion units, control of CO is accomplished by providing adequate fuel residence time and high temperature in the combustion zone to ensure complete combustion; for reforming, having a complete “CO shift” reaction is necessary to minimize CO. These control factors also tend to result in high NO_x and GHG emissions. Since efficient operation of reformers is part of GHG BACT, and 98% of CO is emitted from combustion units, the BACT analysis for CO will focus on combustion units: the two modified reformers and the proposed new No. 2 Urea Plant boiler.

CO emissions from combustion units are a function of oxygen availability (excess air), flame temperature, residence time at flame temperature, combustion zone design, and turbulence.

Alternative CO control methods include exhaust gas cleanup methods such as catalytic oxidation, and front-end methods such as combustion control wherein CO formation is suppressed within the combustors.

A search of EPA's RBLC follows. It was noted that only two BACT determinations relied on an oxidative catalyst, while all others relied on good combustion. Non-feasibility of oxidative catalysts will be discussed later.

Natural Gas Fired Primary Boilers > 250 MMBTUH – Carbon Monoxide

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
FL-0350	Port Dolphin Energy	Florida	12/01/11	Good combustion practices, 0.015 lb/MMBTU CO
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Good combustion practices, 0.0013 lb/MMBTU CO
IA-0106	CF Industries – Port Neal	Iowa	7/12/13	Oxidation catalyst, 0.0013 lb/MMBTU
LA-0231	Lake Charles Gasification	Louisiana	6/22/09	Good design and proper operation, 0.036 lb/MMBTU
LA-0254	Ninemile Point Generating	Louisiana	8/16/2011	Good combustion, natural gas fuel, 0.084 lb/MMBTU
NE-0054	Cargill, Inc.	Nebraska	3/01/13	Good combustion practices
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.037 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Flue gas recirculation, 0.0705 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.0173 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.0172 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.0073 lb/MMBTU

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.0075 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.037 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.848 lb/MMBTU
NV-0049	Harrah's Operating Co.	Nevada	8/20/09	Operation within mfg specs, 0.074 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.0184 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.0214 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.0362 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.037 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.038 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.0148 lb/MMBTU
NV-0050	MGM Mirage	Nevada	11/30/09	Good combustion practices, gas fuel, 0.035 lb/MMBTU
SC-0091	Columbia Energy	South Carolina	7/00/03	Good combustion, clean fuel, 0.06 lb/MMBTU

Step 1. Identify Available Control Technologies

The application identified two control technologies:

- Good combustion practices
- Catalytic oxidation

While secondary non-catalytic oxidation could have been included in the listing, it would have been eliminated at the step of technical feasibility. The two listed options illustrate CO control adequately, either by preventing formation (good combustion practices) or by removal (catalytic oxidation). Catalytic oxidation normally requires a temperature in the range of 500 to 700°F to function properly with maximum catalyst lifespan.

Step 2. Eliminate Technically Infeasible Options

The discharge temperature of exhausts from the boiler and reformer heaters is typically less than 400°F, below the range required for catalytic oxidation to function. Increasing temperatures would require either additional fuel consumption or lowering of heat recovery, items which are at odds with GHG BACT. A review of RBLC shows that only two of the recently-permitted gas-fired boilers or primary reformers have required oxidative catalysts. Oxidative catalysts must be eliminated from the list of potentially-feasible controls due to the temperature issues, leaving only good combustion practices.

Step 3. Rank Remaining Control Technologies by Control Effectiveness

Good combustion controls is the only CO control option left to rank.

Step 4. Evaluate Most Effective Controls Based on Energy, Environmental, and Economic Impacts

Good combustion controls are the only CO control option remaining.

Step 5. Select BACT and Document the Selection as BACT

Good combustion is accepted as BACT for CO emissions from the proposed No. 2 Urea Plant boiler at 0.037 lb/MMBTU (3-hour average) and the modified ammonia plant reformer heaters at 0.084 lb/MMBTU (3-hour average).

C. Particulate Matter (PM₁₀ / PM_{2.5}) BACT Review

The new or modified emissions units subject to a BACT analysis are the modified reformer heaters, No. 2 Urea Plant boiler, urea granulator, new No. 2 Urea Plant cooling tower, new and modified synthesis vents, haul roads, and materials handling/storage and truck/railcar loading. The BACT analysis will address these as categories of combustion units, process units, cooling towers, materials handling, and roads. Since the controls for both PM₁₀ and PM_{2.5} are nearly identical, the two pollutants will be analyzed as a single category.

i. Urea Granulators

Step 1 - Identify All Control Technologies

The following add-on controls were identified as technologies available to control PM emissions from solid nitrogen fertilizer production facilities.

- Wet scrubbers
- Fabric filters (baghouses)
- Mechanical collectors (cyclones)
- Electrostatic precipitators (dry and wet)

A search of EPA's RBLC showed the following results. The RBLC database showed the emissions limits but did not include the types of technologies being used to achieve those results.

Urea Granulators – Particulate Matter

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	0.1 kg/metric tonne total PM and PM ₁₀ , 0.025 kg/metric tonne PM _{2.5}
IA-0106	CF Industries Port Neal	Iowa	7/12/13	0.11 lb/ton
OK-0124	Koch Industries Enid Plant	Oklahoma	5/01/08	0.31 lb/ton
OK-0135	Pryor Chemical	Oklahoma	2/23/09	0.042 lb/ton

Wet Scrubbers

Wet scrubbers are widely used in the solid urea manufacturing industry and are preferred over other controls for a variety of reasons, not the least of which is the ability to recycle urea back to the process. Three types of wet scrubbers were analyzed: spray-tower scrubbers, impingement-type scrubbers, and venturi scrubbers. All of these scrubbers work by capturing small solids in a larger water droplet which is then captured in a mist eliminator or equivalent.

Fabric Filter Baghouse

A fabric filter baghouse (FF) removes solids from the flue gas by drawing dust-laden flue gas through a bank of filter tubes. A filter cake, composed of the removed particles, builds up on the dirty side of the bag. Periodically, the cake is removed through physical mechanisms such as a blast of air from the clean side of the bag, or mechanical shaking of the bags, which causes the cake to fall. The dust is then collected in a hopper and removed. Fabric filters include reverse gas fabric filters (RGFF) or pulse jet fabric filters (PJFF). In a PJFF, the solids are collected on the outside of the bags. A PJFF can operate at higher air-to-cloth ratios than a reverse gas system. Consequently, a PJFF is smaller and will usually have lower capital costs than a RGFF. The bags in a RGFF, however, can be expected to have a longer service life. Consequently, an RGFF will typically have lower operating costs than a PJFF. For the purposes of this BACT analysis, a distinction is not made between RGFF and PJFF.

Mechanical Collectors followed by Particulate Scrubbers

Other technologies available are mechanical collectors such as centrifugal separators (cyclones). However, these technologies do not achieve the removal efficiency of wet scrubbers.

Electrostatic Precipitator (ESP)

An electrostatic precipitator (ESP) removes dust or other fine particles from the flue gas by charging the particles inductively with an electric field and then attracting the particles to highly charged collector plates, from which they are removed. An ESP consists of a hopper-bottomed box containing rows of plates forming passages through which the flue gas flows. Centrally located in each passage are emitting electrodes energized with a high-voltage, negative polarity direct current. The voltage applied is high enough to ionize the gas molecules close to the electrodes, resulting in a corona current of gas ions from the emitting electrodes across the gas passages to the grounded collecting plates. When passing through the flue gas, the charged ions collide with, and attach themselves to, particles suspended in the gas. The electric field forces the charged particles out of the gas stream towards the grounded plates, and there they are collected in a layer. The plates are periodically cleaned by a mechanical rapping system to release the PM layer into hoppers as an agglomerated mass. Factors affecting the efficiency of the ESP include flue gas flow rate, resistivity of the PM, plate area, voltage, number of sections, and overall power consumption.

Wet ESP

A wet ESP operates in the same three-step process as a dry ESP: charging, collection, and removal. However, the removal of particles from the collecting electrodes is accomplished by washing of the collection plate surface using liquid, rather than mechanical rapping of the plates. A wet ESP is more widely used in applications where the gas stream has high moisture content, is below the dew point, or includes sticky particles.

Step 2-Eliminate Technically Infeasible Options

The urea to be handled is an organic material and quite sticky as well as hygroscopic (absorbs water from surrounding gases). Both properties result in urea PM sticking to fabric filters, “blinding” them, and not being recoverable.

The stickiness also creates similar problems in dry ESPs, where the dust collected from an exhaust stream cannot be readily recovered, resulting in accumulation in the ESP. Although cyclones are somewhat less efficient than wet scrubbers, they appear to be equally vulnerable to plugging.

Theoretically, wet ESPs could collect sticky material, but the RBLC database does not show any applications. Wet ESPs, therefore, are not demonstrated technology for this application.

Step 3-Rank Remaining Control Technologies by Control Effectiveness

The highest-efficiency feasible control technology is wet scrubbing; several different wet scrubber designs are feasible. The applicant proposes a limit of 0.1 lb/ton PM. This proposed limitation is more stringent than any other BACT determination except for Pryor Chemical, which has not yet demonstrated compliance with their proposed limit.

Step 4-Evaluate Most Effective Controls for Energy, Environmental, and Economic Impacts

The applicant has selected wet scrubbing as the control technology for control of PM emissions, which is considered the best technology available.

Step 5-Select BACT and Document the Selection as BACT

The high-efficiency wet scrubbers are acceptable as BACT for the new urea granulator. A PM limit of 0.1 lb/ton will be established in the permit.

ii. Solids Handling And Loading

Step 1 - Identify All Control Technologies

The BACT analysis identified the following control options:

- Fabric filters
- Mechanical collectors
- Full or partial enclosures
- Telescoping Chutes
- Wet suppression
- Conditioning agents

It should be noted that some operations, especially the loading operations, will have long periods of inactivity interspersed with near-maximum short-term operations. These load swings complicate the control technology analysis.

Fabric Filter Baghouse

A fabric filter baghouse (FF) removes solids from the flue gas by drawing dust-laden flue gas through a bank of filter tubes. Since this analysis is essentially identical to the analysis for the urea granulators, that text will not be repeated.

Mechanical Collectors

This discussion is also identical to the discussion for the urea granulators.

Enclosures

Enclosures prevent entrainment of particulates by isolation from wind or other disturbances. They have the advantage of being compatible with most process equipment and can enhance product quality.

Telescoping Chutes

Telescoping chutes are used in intermittently-used operations such as load-out. They are lowered into railcars to minimize disturbance of materials during loading operations.

Conditioning Agents

A conditioning agent in the solids handled can reduce brittleness, thus reduce the tendency to fracture into small particles which are susceptible to becoming airborne. It may also enhance the tendency of small particles to stick to each other, forming larger particles which are more prone to settle out gravimetrically.

Wet Suppression

Wet suppression is often used in loading and handling solids, minimizing dust losses. However, since urea is hydrophilic and hygroscopic, any water applied would be readily absorbed into the solids and would create a cake of granulated solids.

Step 2-Eliminate Technically Infeasible Options

A review of the RBLC indicates that, for all of the solid urea plants permitted in the United States during the previous 10 years, conditioning agents, and enclosures have all been accepted in the solid fertilizer industry. Most more-involved systems cannot follow load swings for intermittent operations.

BACT Determinations: Urea Handling & Loading – Particulate Matter

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0106	CF Industries Port Neal	Iowa	7/12/13	Bin Vent Filter, 0.0011 lb/ton
OK-0124	Koch Industries Enid Plant	Oklahoma	5/01/08	Enclosure, telescopic chutes, conditioning agent

Mechanical collectors such as cyclones are not demonstrated technology given the tendency of urea to stick to the cyclone interiors. Similarly, fabric filters would be impractical due to the stickiness of the urea.

Step 3-Rank Remaining Control Technologies by Control Effectiveness

Enclosures provide approximately 85% control. Product conditioning is expected to achieve 90% control, while telescopic chutes should provide approximately 75% control. Used in tandem, the three measures achieve 99.6% control of PM.

The facility adds a conditioning agent as a matter of course.

Step 4-Evaluate Most Effective Controls for Energy, Environmental, and Economic Impacts

The applicant has selected enclosures (full or partial, depending on the operation) as the control technology for control of PM emissions from handling and storage. These units prevent emissions to the atmosphere while maintaining product quality. There is a minimum of waste created by these options.

Telescoping chutes and enclosures will be used for loading operations.

Step 5-Select BACT and Document the Selection as BACT

Enclosures of handling and storage facilities, use of conditioning agents in the urea production, and telescoping chutes on loading operations, are acceptable as BACT.

iii. Cooling Towers

Particulate emissions occur from the cooling tower as a result of the total solids (suspended and dissolved metals and minerals) in the water being entrained in the air stream. Mist eliminators prevent most of the water from escaping out the top of the tower; however, some water droplets (with dissolved and suspended particulate) do escape the cooling tower and are referred to as “drift”. For this analysis, as a simplifying conservative assumption, all of the particulate resulting from the drift is considered to be PM₁₀.

Step 1-Identify All Control Technologies

There are several ways to reduce drift (and resulting PM and PM₁₀) emissions from cooling towers. Process modifications could be considered, including elimination of a cooling tower by using an available water source such as a stream or nearby water reservoir or lake to provide enough water to use “once through” cooling. A standard cooling tower is similar to a once through system except the water is recycled in the tower. Another alternative is the use of air fin cooling. A third alternative is to use a hybrid system that combines some aspects of a wet and a dry system. A fourth option is the installation of modern high efficiency drift eliminators on the cooling tower.

A search of EPA’s RBLC showed that cooling tower PM emissions were controlled almost exclusively by drift eliminators. Three determinations also limited the total dissolved solids content of the cooling waters (two in Nevada and one in Virginia), both of which allowed a much higher drift than 0.0005%

Cooling Towers – Particulate Matter

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
FL-0316	Levy Nuclear Plant	Florida	2/20/09	Drift eliminators, 0.0005% drift
FL-0317	FPL Turkey Point Nuclear Plant	Florida	5/30/09	Drift eliminators, 0.0005% drift
FL-0322	Sweet Sorghum-to-Ethanol	Florida	12/23/10	Not stated
GA-0141	Warren County Biomass Energy	Georgia	12/17/10	Drift eliminators, 0.0005% drift
GA-0142	Osceola Steel	Georgia	12/29/10	Drift eliminators, 0.0005% drift
IA-0106	CF Industries	Iowa	7/12/13	Drift eliminators, 0.0005% drift
ID-0017	Power County Advanced Energy	Idaho	2/10/09	Drift eliminators, 0.0005% drift
ID-0018	Langley Gulch Power Plant	Idaho	6/25/10	Drift eliminators
LA-0204	Plaquemine PVC	Louisiana	2/27/09	Good design, maintenance, drift eliminators, 0.057 lb/MMGal
LA-0213	St. Charles Refinery	Louisiana	11/17/09	Drift eliminators
LA-0264	Norco Hydrogen	Louisiana	9/14/12	Drift eliminators
MI-0400	Wolverine Power	Michigan	6/29/11	Drift eliminators
MI-0401	Midland Power Station	Michigan	12/21/11	Drift eliminators, 0.0005% drift
MN-0078	Sappi Cloquet	Minnesota	10/28/09	Drift eliminators
NV-0049	Harrah's Operating	Nevada	8/20/09	Drift eliminators, 0.005% drift, TDS below 2,520 ppm
NV-0049	Harrah's Operating	Nevada	8/20/09	Drift eliminators, 0.005% drift, TDS below 3,000 ppm
NV-0050	MGM Mirage	Nevada	11/30/09	Drift eliminators, 0.001% drift, TDS below 3,600 ppm
TX-0551	Panda Sherman Power Station	Texas	2/03/10	Drift eliminators, 0.0005% drift
TX-0552	Wolf Hollow Power Plant No. 2	Texas	3/03/10	Drift eliminators, 0.0005% drift
TX-0553	Lindale Renewable Energy	Texas	1/08/10	Drift eliminators, 0.0005% drift

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
VA-0319	Gateway Cogeneration Smart Water Project	Virginia	8/27/12	Drift eliminators, 0.001% drift, TDS below 1,200 ppm
WY-0072	Granger Facility	Wyoming	6/12/13	Drift eliminators, 0.0005% drift

Step 2-Eliminate Technically Infeasible Options

“Once through” cooling is not a feasible option in this location. Several studies have shown that both the dry cooling system (air fins) and the wet/dry hybrid system have an impact on system performance (i.e., reduce the available power output) during the hottest parts of the year. The only feasible option at this location is a wet cooling tower with high efficiency drift eliminators. Since only one control option is feasible, Steps 3 and 4 are not necessary.

Step 5-Select BACT and Document the Selection as BACT

The applicant proposed that high efficiency drift eliminators, with the capability to reduce the potential drift to a maximum of 0.0005% of the circulating water flow rate, is BACT for PM₁₀ and PM_{2.5} control at the cooling tower. The proposed control technology is acceptable as BACT. Compliance will be demonstrated by vendor guarantees, and the facility will be required to show TDS contents periodically.

iv. Combustion Units

Step 1 - Identify All Control Technologies

The following add-on controls were identified as technologies available to control PM emissions from solid nitrogen fertilizer production facilities.

- Wet scrubbers
- Fabric filters (baghouses)
- Mechanical collectors (cyclones)
- Electrostatic precipitators (dry and wet)
- Fuel selection / good combustion practices

A search of EPA’s RBLC showed the following results.

Natural Gas Fired Primary Reformers – Particulate Matter

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Good combustion practices, 0.0024 lb/MMBTU TPM
LA-0211	Garyville Refinery	Louisiana	12/27/06	Proper design and operation, 0.0075 lb/MMBTU
LA-0264	Norco Hydrogen	Louisiana	9/04/12	Proper equipment design, good combustion practices, gas fuel
OK-0134	Pryor Chemical	Oklahoma	2/23/09	Not stated
OK-0135	Pryor Chemical	Oklahoma	2/23/09	Not stated
PA-0231	United Refinery	Pennsylvania	10/09/03	Good combustion
TX-0526	Air Products	Texas	8/18/06	Not stated

Natural Gas Fired Primary Boilers – Particulate Matter

RBLC ID	Facility	State	Permit Issuance Date	BACT Limit
IA-0105	Iowa Fertilizer	Iowa	10/26/12	Good combustion practices, 0.0024 lb/MMBTU TPM
IA-0106	CF Industries	Iowa	7/12/13	Good combustion practices, gas fuel, 0.0024 lb/MMBTU TPM
LA-0231	Lake Charles Gas	Louisiana	6/22/09	Good design and proper operation
LA-0254	Ninemile Point	Louisiana	8/16/11	Good combustion, natural gas fuel
MN-0078	Sappi Cloquet	Minnesota	10/28/09	0.007 lb/MMBTU
NE-0054	Cargill, Inc.	Nebraska	3/01/13	Good combustion practices
SC-0091	Columbia Energy	South Carolina	7/03/03	Good combustion practices, 0.005 lb/MMBTU

It is noted that the Iowa determinations for PM from gas-fired units are approximately 1/3 of the values in AP-42, Section 1.4, and without any add-on controls.

Wet Scrubbers

Wet scrubbers are widely used. All of these scrubbers work by capturing small solids in a larger water droplet which is then captured in a mist eliminator or equivalent. There would be the added benefit of cooling exhaust streams, condensing condensable PM. However, their effectiveness is limited for small-diameter particles.

Fabric Filter Baghouse

A fabric filter baghouse (FF) removes solids from the flue gas by drawing dust-laden flue gas through a bank of filter tubes. A filter cake, composed of the removed particles, builds up on the dirty side of the bag. Periodically, the cake is removed through physical mechanisms such as a blast of air from the clean side of the bag, or mechanical shaking of the bags, which causes the cake to fall. The dust is then collected in a hopper and removed. However, the effectiveness of baghouses is limited for submicron particles and negligible for condensable PM; the gas stream would have to be cooled adequately to condense condensable PM for the baghouses to have any beneficial effect.

Mechanical Collectors followed by Particulate Scrubbers

Other technologies available are mechanical collectors such as centrifugal separators (cyclones). However, these technologies do not achieve the removal efficiency of wet scrubbers. Mechanical collectors are rarely used for PM smaller than 5 microns, and most PM from natural gas combustion is expected to be PM_{2.5}.

Electrostatic Precipitator (ESP)

An electrostatic precipitator (ESP) removes dust or other fine particles from the flue gas by charging the particles inductively with an electric field and then attracting the particles to highly charged collector plates, from which they are removed. Factors affecting the efficiency of the ESP include flue gas flow rate, resistivity of the ash, plate area, voltage, number of sections, and overall power consumption. Similarly to other potential controls, the gas stream must be cooled first to condense condensable PM. The condensable PM is largely soot, salts, and condensed organic vapors, all of which have inadequate resistivity to hold a surface charge.

Wet ESP

A wet ESP operates in the same three-step process as a dry ESP: charging, collection, and removal. However, the removal of particles from the collecting electrodes is accomplished by washing of the collection plate surface using liquid, rather than mechanical rapping of the plates. A wet ESP is more widely used in applications where the gas stream has high moisture content, is below the dew point, or includes sticky particles.

Step 2-Eliminate Technically Infeasible Options

A search of RBLs shows no add-on controls being used for gas-fired units. The only practical control technology is use of gas fuel, which is low-emitting fuel.

Step 3-Rank Remaining Control Technologies by Control Effectiveness

The only remaining control technology is natural gas fuel.

Step 4-Evaluate Most Effective Controls for Energy, Environmental, and Economic Impacts

The only remaining control technology is natural gas fuel.

Step 5-Select BACT and Document the Selection as BACT

The use of natural gas fuel is acceptable as BACT for the new boiler and modified reformer heaters. A PM, PM₁₀, and PM_{2.5} limit based on 0.0076 lb/MMBTU will be established in the permit.

SECTION VIII. EVALUATION OF EXISTING AIR QUALITY AND DETERMINATION OF MONITORING REQUIREMENTS

Model Selection and Description

Consistent with the available modeling applications provided for by Appendix W to Part 51 Guideline on Air Quality Models, the AERMOD (Version 15181) air dispersion model is used to predict maximum ground-level concentrations associated with the proposed project's emissions. AERMOD is a refined, multi-source Gaussian plume model. The modeling analysis was performed using regulatory default options including stack-tip downwash and missing data processing.

Terrain Considerations

Per AQD guidance, modeling with elevated terrain was conducted. AERMAP (version 11103), a preprocessor that takes digital elevation data from the US Geologic Survey (USGS), was used to assign elevations to stack, buildings, receptors, and hills. The base elevation of the facility is approximately 1,204 feet above mean sea level.

USEPA guidance supports the use of AERSURFACE to process land cover data to determine the surface characteristics (i.e., surface roughness, Bowen ratio, and albedo) for the meteorological measurement site that is used to represent meteorological site conditions. Chapter 2.3.4 of ODEQ's *Air Dispersion Modeling Guidelines for Oklahoma Air Quality Permits* also indicates that surface characteristics using AERSURFACE can be used for air permit applications. The GeoTIFF file for Oklahoma containing the land cover data is used as input for AERSURFACE. ODEQ's modeling guidance document also recommends the following input conditions for running AERSURFACE:

- Center the land cover analysis on the meteorological measurement site.
- Analyze surface roughness within 1 km of measurement site.
- Utilize one sector determining the surface roughness length.
- Temporal resolution of the surface characteristics should be determined on a monthly basis.
- The region does not experience continuous snow cover for most of the winter.
- The Mesonet site is not considered an airport.
- The region is not considered an arid region.
- Utilize the default season assignment (winter=Dec, Jan, Feb; Spring=Mar, Apr, May; Summer=Jun, Jul, Aug; Fall=Sep, Oct, Nov).

Background Concentrations

Regional monitoring data from Monitoring Site ID 401091037, located in Oklahoma City, is considered representative of the background concentrations in the affected area of the KOCH Enid facility for purposes of the Class II modeling and within 50 km of the KOCH Enid facility for purposes of the Class I modeling. Accordingly, site-specific pre-construction monitoring will not be required.

Good Engineering Practice and Building Downwash Evaluation

The dispersion of a plume can be affected by nearby structures when the stack is short enough to allow the plume to be significantly influenced by surrounding building turbulence. This phenomenon, known as structure-induced downwash, generally results in higher model-predicted ground-level concentrations in the vicinity of the influencing structure. Sources included in a PSD permit application are subject to Good Engineering Practice (GEP) stack height requirements outlined in OAC 252:100-8-1.5. GEP stack height is defined as the greater of 65 meters or a height established by applying the formula $H_g = H + 1.5L$, where:

H_g = GEP stack height,

H = height of nearby structures, and

L = lesser dimension (height or projected width) of nearby structures,

or by a height demonstrated by a fluid model or a field study that ensures that emissions from a stack do not result in excessive concentrations of any pollutant as a result of atmospheric downwash, wakes, or eddy effects created by the source itself, nearby structures, or nearby terrain features.

The model utilizes the EPA Building Profile Input Parameters (BPIP) program with the plume rise model enhancements (PRM). BPIP-PRIME determines the effect of building downwash on each plume in calculation of maximum impacts.

Meteorology and Surface Characteristics

Five years (2006, 2007, 2008, 2009, and 2010) of processed Oklahoma Mesonet data from Breckenridge, Oklahoma and Enid, Oklahoma (Woodring Regional Airport) were combined with data from the National Center for Environmental Information (NCEI) and Norman Max Westheimer Airport Upper Air (UA) rawinsonde observation (RAOB) data from the Forecast System Laboratories (FSL). Oklahoma Mesonet data was provided to the AQD courtesy of the Oklahoma Mesonet, a cooperative venture between Oklahoma State University (OSU) and the University of Oklahoma (OU) and supported by the taxpayers of Oklahoma.

When using AERMET to prepare the meteorological data for AERMOD, the surface characteristics (Albedo, Bowen Ratio, and Surface Roughness Length) for the primary (MESONET) and secondary (NCDC-ISD) meteorological sites were determined using AERSURFACE.

Receptor Grid

The AERMOD model allows the user to have the model calculate impacts at user defined discrete and/or flagpole receptors. Discrete receptors are those that are placed at precise locations that may be of interest due to their sensitive nature. Flagpole receptors are receptors that are located above ground level. The ODEQ Air Dispersion Modeling Guidelines does not mention the application of any discrete or flagpole receptors; therefore, no discrete or flagpole receptors are used in the modeling analysis.

Six Cartesian grids for the modeling analyses were defined as follows:

1. A Fence Line Grid containing receptors spaced at 50 meter intervals along the facility fence line.
2. A Fine Grid containing receptors spaced at 100 meter intervals extending approximately 1.0 km from the fence line, exclusive of the Fence Line Grid.
3. A 250-meter grid containing receptors spaced at 250 meter intervals extending approximately 2.5 km beyond the Fine Grid.
4. A 500-meter grid containing receptors spaced at 500 meter intervals extending approximately 5.0 km beyond the 250-meter grid.
5. A 750-meter grid containing receptors spaced at 750 meter intervals extending approximately 7.5 km beyond the 500-meter grid.
6. A 1,000-meter grid containing receptors spaced at 1,000 meter intervals extending approximately 50.0 km beyond the 750-meter grid.

Secondary PM_{2.5} Formation Modeling

On March 4, 2013, EPA published “Draft Guidance for PM_{2.5} Permit Modeling.” According to the draft guidance, since the proposed project will have an emission increase greater than 10 TPY of PM_{2.5} but less than 40 TPY apiece of NO_x and SO₂, only primary PM_{2.5} emissions have to be considered.

Source Input Parameters

The modeled stack point source parameters and emission rates for the Enid facility are shown following.

Source	Height	Temp	Velocity	Diameter	Elevation	PM_{2.5}	PM₁₀	CO
	feet	°F	ft/sec	inches	feet	lb/hr	lb/hr	lb/hr
New boiler	201	300	49.6	84	1203	3.35	3.35	16.67
New granulator	224	117	106.9	99	1200	6.04	6.04	0.00
New cooling tower 1	39	78	36.4	216	1203	<0.01	0.05	0.00
New cooling tower 2	39	78	36.4	216	1205	<0.01	0.05	0.00
New cooling tower 3	39	78	36.4	216	1207	<0.01	0.05	0.00
New cooling tower 4	39	78	36.4	216	1209	<0.01	0.05	0.00
Existing A2 Cooling Tower 1	67	78	77.9	240	1209	<0.01	0.01	0.00
Existing A2 Cooling Tower 2	67	78	77.9	240	1209	<0.01	0.01	0.00
Existing A2 Cooling Tower 3	67	78	77.9	240	1208	<0.01	0.01	0.00
Existing A2 Cooling Tower 4	67	78	77.9	240	1208	<0.01	0.01	0.00
New No. 2 Ammonia cooling tower cell	47	78	36.4	216	1209	<0.01	0.05	0.00
No. 1 Reformer	105	570	67.5	126	1200	0.72	0.72	88.89
No. 2 Reformer	120	350	35.8	156	1208	2.69	2.69	111.11
No. 1 Urea synthesis vent	217	206	3.6	26	1206	0.90	0.90	1.85
No. 2 Urea synthesis vent	180	92	11.6	16	1201	0.05	0.05	3.08
No. 1 Urea boiler 403A	50	323	50.6	38	1203	0.34	0.34	0.00
No. 1 Urea boiler 403B	50	323	50.6	38	1204	0.34	0.34	0.00

Urban/Rural Classification

Section 8.2.3 of the GAQM provides the basis for determining the urban/rural status of a source. For most applications, the land use procedure described in Section 8.2.3(c) is sufficient for determining the urban/rural status. However, there may be sources located within an urban area, but located close enough to a body of water to result in a predominantly rural classification. In those cases, the population density procedure may be more appropriate. Because the Enid facility is not located within an urban area near a body of water, only the following land use procedure is used to assess the urban/rural status of the source.

- Classify the land use within the total area, A_o , circumscribed by a 3-km radius circle about the source using the meteorological land use typing scheme proposed by Auer.
- If land use Types I1 (heavy industrial), I2 (light-moderate industrial), C1 (commercial), R2 (single-family compact residential), and R3 (multifamily compact residential) account for 50 percent or more of A_o , use urban dispersion coefficients; otherwise, use appropriate rural dispersion coefficients.

Based on visual inspection of the USGS 7.5-minute topographic map of the project site location, it was conservatively concluded that over 50 percent of the area surrounding the project may be classified as rural. Accordingly, the rural dispersion modeling option is used in the AERMOD PRIME model.

Significance Analysis

Dispersion modeling analysis usually involves two distinct phases; a preliminary analysis and a full impact analysis. The preliminary analysis models only the significant increase in potential emissions of a pollutant from a proposed new source, or the significant net emissions increase of a pollutant from a proposed modification. The results of this preliminary analysis determine whether the applicant must perform a full impact analysis, involving the estimation of background pollutant concentrations resulting from existing sources and growth associated with the proposed project. Specifically, the preliminary analysis:

- determines whether the applicant can forego further air quality analyses for a particular pollutant;
- may allow the applicant to be exempted from the ambient monitoring data requirements; and
- is used to define the impact area within which a full impact analysis must be carried out.

In general, the full impact analysis is used to project ambient pollutant concentrations against which the applicable NAAQS and PSD increments are compared, and to assess the ambient impact of non-criteria pollutants. The full impact analysis is not required for a particular pollutant when emissions of that pollutant would not increase ambient concentrations by more than the applicable significant impact level (SIL).

Using EPA's March 2013 "Draft Guidance for $PM_{2.5}$ Permit Modeling," a full impact analysis for $PM_{2.5}$ is not required if: (1) the difference between the $PM_{2.5}$ background concentration and the $PM_{2.5}$ NAAQS is greater than the $PM_{2.5}$ significance impact level; and (2) the modeled impacts of $PM_{2.5}$ from the project would not increase ambient concentrations by more than the $PM_{2.5}$ significant impact level (SIL). The same analysis was completed for CO and PM_{10} . As demonstrated by the following table, a full impact analysis is not required for CO, PM_{10} , or $PM_{2.5}$.

Pollutant	Averaging Period	Max Project Impact $\mu\text{g}/\text{m}^3$	SIL $\mu\text{g}/\text{m}^3$	Max Background $\mu\text{g}/\text{m}^3$	Background + SIL $\mu\text{g}/\text{m}^3$	NAAQS $\mu\text{g}/\text{m}^3$	Full Impact Analysis Required?
CO	1-hr	88.3	2,000	1,488	3,488	40,000	No
	8-hr	51.8	500	1,259	1,759	10,000	No
PM ₁₀	24-hr	4.18	5	77	82	150	No
PM _{2.5}	24-hr	1.17	1.2	31	32.2	35	No
	Annual	0.24	0.3	9.7	10.0	12	No

Since the maximum project impacts are less than the PM₁₀ 24-hour, PM_{2.5} 24-hour and PM_{2.5} annual Class II SILs, a full Class II increment analysis is not required.

SECTION IX. OTHER PSD ANALYSES

A. Evaluation of Class I Area Impacts

Federally designated Class I areas are afforded special protection in the air permitting process. Generally, Class I area analyses are conducted only for projects located within 100 km of a Class I area. The Enid facility is approximately 193 km from the closest Class I area, the Wichita Mountains Wildlife Refuge. Another Class I area in proximity to the Enid facility is the Upper Buffalo Wilderness Area located in Arkansas approximately 400 km from the Enid facility.

The first step in the Class I impacts analysis is to model the project's impacts at 50 km to determine if the project's impacts exceed the Class I SILs. If impacts are less than the SILs, no further analysis is necessary; if they exceed the SILs, CALPUFF modeling is used to determine project impacts.

Pollutant	24-hour Average, $\mu\text{g}/\text{m}^3$		Annual Averages, $\mu\text{g}/\text{m}^3$	
	SIL	Project Impacts	SIL	Project Impacts
PM ₁₀	0.3	0.059	0.2	0.004
PM _{2.5}	0.07	0.037	0.06	0.004
CO	NA	NA	NA	NA

For the Class I area impacts analysis, the same approach was taken as for the Class II area impacts analysis. As demonstrated by the data in the following table, which uses the Class I SILs for the relevant pollutants, a full Class I area impact analysis is not required for PM₁₀ or PM_{2.5}:

Pollutant	Averaging Period	Max Impact $\mu\text{g}/\text{m}^3$	Class I SIL $\mu\text{g}/\text{m}^3$	Max Background $\mu\text{g}/\text{m}^3$	Background + SIL $\mu\text{g}/\text{m}^3$	NAAQS $\mu\text{g}/\text{m}^3$	Full Impact Analysis Required?
PM ₁₀	24-hr	0.059	0.3	77	77.3	150	No
	Annual	0.004	0.2	NA	NA	50	No
PM _{2.5}	24-hr	0.037	0.07	31	31.07	35	No
	Annual	0.004	0.06	9.7	9.76	12	No

Since the maximum project impacts are less than the PM₁₀ 24-hour, PM₁₀ annual, PM_{2.5} 24-hour and PM_{2.5} annual Class I SILs, a full Class I increment analysis is not required.

A screening procedure is followed to determine potential impacts on any Air Quality Related Value (AQRV) for any Class I area within 300 km of a new source. The procedure commences with the sum of emissions of SO₂, H₂SO₄, PM₁₀, and NO_x into the value "Q." The Q value is then divided by the distance (D) between the source and the Class I area in question. If the Q/D ratio is less than 10, no further AQRV analysis is required. As shown in the following table, the screening criteria are met for the closest Class I area.

Class I Area	Q, TPY	D, km	Q/D Ratio	AQRV Required?
Wichita Mountains Wildlife Refuge	103.1	193	0.53	No

B. Evaluation of Source-related Impacts on Growth, Soils, Vegetation, and Visibility

Commercial, Residential, and Industrial Growth Analysis

The project is located in Garfield County in an area zoned as industrial. Because the project will create approximately 50 additional full-time employment positions adjacent to a city of 47,000 population, the project will not have a significant effect upon the industrial growth in the immediate area. There will be an increase in the local labor force during the construction phase of the project. It is anticipated that most of the labor force during the construction phase will commute from nearby communities. This labor force increase will be temporary, short-lived, and will not result in permanent commercial and residential growth occurring in the vicinity of the project.

The potential for housing shortages and thus the possibility of housing related growth and secondary air quality impacts have been an issue historically for the construction of large plants in sparsely populated areas. However, smaller projects (modifications) like the proposed project located in or near urban areas typically have no noticeable impacts on the housing market. The reason is that impacts are primarily a function of the size of the construction workforce and the need for the workforce to relocate during construction.

The need to relocate is a function of the available workforce within a reasonable commuting distance of the work site. Research by the Electric Power Research Institute (EPRI) has indicated that the construction workforce for a power plant project can reasonably be expected to commute without relocating during construction from a distance of more than 70 miles, with instances of a commuting distance of more than 100 miles found in each of the construction projects studied. When a 70 mile radius around the Enid facility is considered, areas including Tulsa, Enid, and Ponca City in Oklahoma are within commuting distance to the site.

The area offers a wide variety of temporary lodging. Given the expected population of the commuting workforce, the fact that during the construction period most workers will be onsite for less than the total construction period, and an abundance of hotel and other short-term lodging options in Garfield County, it is unlikely that a substantial number of the construction workforce would choose to relocate during the construction period. Therefore, the anticipated housing growth will be minimal or nonexistent, and is not expected to have a significant impact on the air quality.

Population increase is a secondary growth indicator of potential increases in air quality levels. Changes in air quality due to population increase are related to the amount of vehicle traffic, commercial/institutional facilities, and home fuel use. Since there will be no or only minimal number of new, permanent jobs created by the project, secondary residential, commercial, and industrial growth is not expected to have a significant impact on the air quality.

Finally, because the maximum model-predicted CO concentrations for the proposed project are well below the NSR/PSD significant impact levels, air concentrations in the region are expected to fully comply with the ambient air quality standards when the proposed project becomes operational. Therefore, from an air quality impact standpoint, the proposed project is consistent with the balanced growth demonstrated by the county to date.

Soils & Vegetation Analyses

The NSR Workshop Manual states that the analysis of air pollution impacts on vegetation should be based on an inventory of species found in the impact area, i.e., significant impact area (SIA). Since the emissions from the proposed project did not result in any exceedances of the significant impact levels; thus no SIA exists.

Unlike fauna, CO does not poison vegetation since it is rapidly oxidized to form carbon dioxide which is used for photosynthesis. However, extremely high concentrations can reduce the photosynthetic rate. According to the USEPA document *A Screening Procedure for the Impacts of Air Pollution Sources on Plant, Soils, and Animals*, hereafter referred to as USEPA Screening Document, for the most sensitive vegetation, a CO concentration of 1,800,000 $\mu\text{g}/\text{m}^3$ (1-week averaging period) could potentially reduce the photosynthetic rate. The maximum model-predicted 1-hour CO impact of 82.9 $\mu\text{g}/\text{m}^3$ produced by the proposed project is significantly lower than this screening level (even at a conservative 1-hour averaging period). Consequently, no adverse impacts to vegetation at or near the proposed project are expected from CO emissions.

The potential effects of PM_{10} produced by the proposed expansion on the nearby vegetation and soil were examined. The potential effects of the air emissions to vegetation within the immediate vicinity were compared to scientific research examining the effects of pollution on vegetation. Damage to vegetation often results from acute exposure to pollution, but may also occur after prolonged or chronic exposures. Acute exposures are typically manifested by internal physical damage to leaf tissues, while chronic exposures are more associated with the inhibition of physiological processes such as photosynthesis, carbon allocation, and stomatal functioning.

The most obvious effect of particle deposition on vegetation is a physical smothering of the leaf surface. This will reduce light transmission to the plant, in turn causing a decrease in photosynthesis. Modeling results have shown that PM_{10} increment is still available after construction, and modeled values are almost one half less than the NAAQS level for 24-hour impacts including background. These levels are considered low, so it is highly unlikely that particulate matter emissions will impact vegetation adjacent to the Enid plant. The PM itself is agricultural fertilizer, so there should be beneficial instead of adverse impacts in the vicinity of the Enid plant.

Based upon the results, it is concluded that the construction of the proposed project will not have a significant adverse impact on the surrounding soil and vegetation.

Visibility Impairment Analysis

An additional impacts visibility analysis may be used to determine if the emissions increases associated with a proposed PSD project will have an impact on Class I sensitive areas such as state parks, wilderness areas, or scenic sites and over looks. However, because the proposed project does not result in any increase of a visibility impairing pollutant, and because the Enid facility is not located within 40 km of a sensitive area, an additional impacts visibility impairment analysis is not required for this project. An explanation of these issues is presented in the following paragraphs.

The screening model VISCREEN can be used to perform a visibility analysis for Class II areas. The VISCREEN model uses emissions of primary particulate matter (PM), nitrogen oxides (NO_x), primary nitrogen dioxide (NO_2), soot (elemental carbon), and primary sulfate (SO_4^-) to determine the visibility impacts from the emissions associated with the proposed project. Three screening levels for visibility impacts are recommended by EPA, for the first two of which VISCREEN is used. The first level involves conservative default parameters. If first level screening exceeds the screening levels, the analysis proceeds to a second level where low-probability events are excluded. This resulted in low wind speeds (below 1.0 m/s) and “F” stability events being excluded. The project passed Level 2 analysis.

SECTION X. INSIGNIFICANT ACTIVITIES

The insignificant activities identified in the application submitted July 30, 2004, and listed in OAC 252:100-8, Appendix I, are summarized below. Additionally, the plant may operate sources of trivial emissions that are not required to be listed in the permit or permit application. Appropriate recordkeeping of activities indicated below with an asterisk (“*”) is specified in the Specific Conditions.

1. * Stationary reciprocating engines burning natural gas, gasoline, aircraft fuels, or diesel fuel, which are either used exclusively for emergency power generation or for peaking power service not exceeding 500 hours per year. The plant operates one (1) diesel-fired emergency generator and one (1) diesel-fired water pump, which were previously in this category but which ceased to be on the compliance date for new standards of NESHAP Subpart ZZZZ. The new emergency generator is subject to NSPS Subpart JJJJ; therefore, it does not qualify for “insignificant activity” status.

2. Various space heaters, boilers, process heaters, and emergency flares less than or equal to 5 MMBTUH heat input (commercial natural gas). In addition, the plant operates one (1) glycol dehydrator reboiler rated at 1.5 MMBTUH. Other space heaters, boilers, or process heaters may be used in the future.
3. Emissions from stationary internal combustion engines rated less than 50-hp output.
4. Gasoline and fuel handling facilities, equipment, and storage tanks except those subject to New Source Performance Standards, and standards under 252:100-37-15, 39-30, 39-41, and 39-48. None identified but may be used in the future.
5. Emissions from condensate tanks with a design capacity of 400 gallons or less in ozone attainment areas. None identified but may be used in the future.
6. * Emissions from storage tanks constructed with a capacity less than 39,894 gallons which store VOC with a vapor pressure less than 1.5 psia at maximum storage temperature. The plant operates one (1) 2,961 gallon compressor oil storage tank, one (1) 1,125 gallon diesel storage tank, one (1) 264 gallon diesel fuel tank, and one (1) 576 gallon diesel fuel tank, which are in this category. Other similar tanks may be used in the future.
7. Cold degreasing operations utilizing solvents that are denser than air. There are currently seven (7) parts washers located on-site using solvents that are denser than air, and others may be added in the future.
8. Welding and soldering operations utilizing less than 100 pounds of solder and 53 tons per year of electrode. These activities are conducted as a part of routine maintenance, which are considered trivial activities and records will not be required.
9. Hazardous waste and hazardous materials drum staging areas.
10. Sanitary sewage collection and treatment facilities other than incinerators and Publicly Owned Treatment Works (POTW). Stacks or vents for sanitary sewer plumbing traps are also included (i.e. lift station).
11. Exhaust systems for chemical, paint, and/or solvent storage rooms or cabinets, including hazardous waste satellite (accumulation) areas. The facility has exhaust systems for chemical, paint, and/or solvent storage rooms or cabinets, including hazardous waste satellite (accumulation) areas, and others may be used in the future.
12. Hand wiping and spraying of solvents from containers with less than 1 liter capacity used for spot cleaning and/or degreasing in ozone attainment areas. None identified but may be used in the future.
13. * Activities having the potential to emit no more than 5 TPY (actual) of any criteria pollutant. The plant Insignificant Activities are listed in EUG-17.

SECTION XI. OKLAHOMA AIR POLLUTION CONTROL RULES

OAC 252:100-1 (General Provisions) [Applicable]
Subchapter 1 includes definitions but there are no regulatory requirements.

OAC 252:100-2 (Incorporation by Reference) [Applicable]
This subchapter incorporates by reference applicable provisions of Title 40 of the Code of Federal Regulations. These requirements are addressed in the “Federal Regulations” section.

OAC 252:100-3 (Air Quality Standards and Increments) [Applicable]
Subchapter 3 enumerates the primary and secondary ambient air quality standards and the significant deterioration increments. At this time, all of Oklahoma is in attainment of these standards.

OAC 252:100-5 (Registration, Emission Inventory, and Annual Operating Fees) [Applicable]
The owner or operator of any facility that is a source of air emissions shall submit a complete emission inventory annually on forms obtained from the Air Quality Division. Emission inventories were submitted and fees paid for previous years as required.

OAC 252:100-8 (Permits for Part 70 Sources) [Applicable]
Part 5 includes the general administrative requirements for part 70 permits. Any planned changes in the operation of the facility which result in emissions not authorized in the permit and which exceed the “Insignificant Activities” or “Trivial Activities” thresholds require prior notification to AQD and may require a permit modification. Insignificant activities mean individual emission units that either are on the list in Appendix I (OAC 252:100) or whose actual calendar year emissions do not exceed the following limits:

- 5 TPY of any one criteria pollutant
- 2 TPY of any one hazardous air pollutant (HAP) or 5 TPY of multiple HAPs or 20% of any threshold less than 10 TPY for a HAP that the EPA may establish by rule

Emission limitations for all the sources are taken from the permit application and previous permit.

OAC 252:100-9 (Excess Emissions Reporting Requirements) [Applicable]
Except as provided in OAC 252:100-9-7(a)(1), the owner or operator of a source of excess emissions shall notify the Director as soon as possible but no later than 4:30 p.m. the following working day of the first occurrence of excess emissions in each excess emission event. No later than thirty (30) calendar days after the start of any excess emission event, the owner or operator of an air contaminant source from which excess emissions have occurred shall submit a report for each excess emission event describing the extent of the event and the actions taken by the owner or operator of the facility in response to this event. Request for mitigation, as described in OAC 252:100-9-8, shall be included in the excess emission event report. Additional reporting may be required in the case of ongoing emission events and in the case of excess emissions reporting required by 40 CFR Parts 60, 61, or 63.

OAC 252:100-13 (Open Burning)

[Applicable]

Open burning of refuse and other combustible material is prohibited except as authorized in the specific examples and under the conditions listed in this subchapter. KOCH on occasion conducts fire training for plant personnel. KOCH notifies the local fire department of these activities prior to conducting the training.

OAC 252:100-19 (Particulate Matter)

[Applicable]

Section 19-12 regulates PM emissions from various industrial processes excluding indirect-fired fuel-burning units. Allowable PM emission rates are specified based on process weight rate. The following table compares process weight rate to the applicable allowable rates.

**COMPARISON OF PROCESS PM EMISSIONS TO ALLOWABLE RATES
OF OAC 252:100-19**

Unit	Process Weight Rate, TPH	Allowable PM Emission Rate of OAC 252:100-19, lb/hr	Anticipated PM Emission Rate, lb/hr
No. 1 Urea Granulator 1	21.53	32.06	6.60
No. 1 Urea Granulator 2	21.53	32.06	6.60
No. 1 Urea Granulator 3	21.53	32.06	6.60
No. 1 Urea High Pressure Urea Synthesis Vent	66.67	47.30	1.40
No. 1 Urea Low Pressure Urea Synthesis Vent	66.67	47.30	0.47
No. 2 Urea Synthesis Vent	106	51.9	0.05
No. 2 Urea Granulator	141	54.8	6.04
No. 2 Urea Material Handling	425	67.03	Negligible
No. 2 Urea Material Loading	425	67.03	Negligible
No.2 Urea Plant Loading (annual)	141	54.79	0.04

OAC 252:100-25 (Visible Emissions and Particulates)

[Applicable]

No discharge of greater than 20% opacity is allowed except for short-term occurrences that consist of not more than one six-minute period in any consecutive 60 minutes, not to exceed three such periods in any consecutive 24 hours. In no case shall the average of any six-minute period exceed 60% opacity. Due to the types of fuel burned (natural gas or ammonia plant purge gas) or specific process operations, the following EUGs have little potential to generate opacity (excluding steam, fog, or icy mist from the presence of uncombined water) during normal operations: EUG 2, EUG 3, EUG 4, EUG 5, EUG 7, EUG 10, EUG 13, EUG 15, EUG-17, EUG-21, EUG-22, EUG-23, EUG-25, EUG-26, and EUG-27. Therefore, specific monitoring for these sources is not necessary. Opacity requirements for sources that may have the potential to generate opacity (EUG 6, EUG 12, and EUGs 14/14A) are addressed in the specific conditions of this permit.

OAC 252:100-29 (Fugitive Dust)

[Applicable]

No person shall cause or permit the discharge of any visible fugitive dust emissions beyond the property line on which the emissions originate in such a manner as to damage or to interfere with the use of adjacent properties, or cause air quality standards to be exceeded, or interfere with the maintenance of air quality standards. The handling and loading of granular urea takes place within enclosed, partially-enclosed, or shrouded areas to minimize the potential for the generation of fugitive dust. Open-bodied trucks and railcars, which are used to transport urea, are covered prior to leaving the plant boundaries. Primary plant roadways are speed-controlled, paved, and maintained.

OAC 252:100-31 (Sulfur Compounds)

[Applicable]

Part 5 limits sulfur dioxide emissions from new fuel-burning equipment (constructed after July 1, 1972). For gaseous fuels the limit is 0.2 lb/MMBTU heat input averaged over 3 hours. For fuel gas having a gross calorific value of 1,000 BTU/SCF, this limit corresponds to fuel sulfur content of 1,203 ppmv. The permit requires the use of pipeline natural gas as defined in Part 72 having 0.5 grains TRS/100 scf to ensure compliance with Subchapter 31.

OAC 252:100-33 (Nitrogen Oxides)

[Applicable]

This subchapter limits new gas-fired fuel-burning equipment with rated heat input greater than or equal to 50 MMBTUH to emissions of 0.2 lb of NO_x per MMBTU, three-hour average. New fuel burning equipment is defined as fuel-burning equipment that was not in service on February 14, 1972 or any existing fuel burning equipment that was altered, replaced, or rebuilt after February 14, 1972 with some exceptions. For direct fired processes, new fuel burning equipment is defined as fuel-burning equipment that was not in service on July 1, 1977 or any existing fuel burning equipment that was altered, replaced, or rebuilt after July 1, 1977, resulting in an increase in NO_x emissions. The Ammonia Plant primary reformers were initially constructed in 1973 and 1975, which is in between the applicability dates for indirect fired and direct fired units. With modification and becoming subject to more stringent NO_x limits, those dates are no longer significant. The following table compares NO_x emissions from the plant's fuel-burning equipment, as calculated above, to the limitations of Subchapter 33.

COMPARISON OF NO_x EMISSIONS TO LIMITATIONS OF OAC 252:100-33

Unit	Heat Input Capacity, MMBTUH	NO _x Emission Limitation of OAC 252:100-33, lb/MMBTU	Anticipated NO _x Emission Rate, lb/MMBTU
Ammonia Plant Primary Reformer #1	1,076	0.2	0.2
Ammonia Plant Primary Reformer #2	1,350	0.2	0.2
Ammonia Unit Startup Boiler	144	0.2	0.2
No. 1 Urea Boiler 1	84	0.2	0.2
No. 1 Urea Boiler 2	84	0.2	0.2
No. 2 Urea Plt. Boiler	450	0.2	0.045

OAC 252:100-35 (Carbon Monoxide)

[Not Applicable]

None of the following affected processes are part of this plant: gray iron foundry, blast furnace, basic oxygen furnace, petroleum catalytic reforming unit, or petroleum catalytic cracking unit.

OAC 252:100-37 (Volatile Organic Compounds)

[Applicable]

Part 3 requires storage tanks constructed after December 28, 1974, with a capacity of 400 gallons or more and storing a VOC with a vapor pressure greater than 1.5 psia to be equipped with a permanent submerged fill pipe or with an organic vapor recovery system. This part applies to the 1,128 gallon gasoline storage tank, which is equipped with a permanent submerged fill pipe. The vapor pressure of diesel is less than 1.5 psia; therefore, Part 3 does not apply to the diesel tanks. The conditioning agent storage tanks (EUG 5 and EUG-24) store a VOC with a vapor pressure less than 1.5 psia; therefore, Part 3 does not apply to this unit. Ammonia is inorganic, so ammonia storage is not affected by Part 3.

Part 3 requires loading facilities with a throughput equal to or less than 40,000 gallons per day to be equipped with a system for submerged filling of tank trucks or trailers if the capacity of the vehicle is greater than 200 gallons. This plant fills only vehicle gasoline tanks with capacities less than 200 gallons. Therefore, this requirement is not applicable.

Part 5 limits the VOC content of coatings used in coating lines or operations. This plant will not normally conduct coating or painting operations except for routine maintenance of the plant and equipment, which is exempt.

Part 7 also requires fuel-burning and refuse-burning equipment to be operated to minimize emissions of VOC. The fuel burning equipment at the plant is subject to this requirement.

OAC 252:100-42 (Toxic Air Contaminants (TAC))

[Applicable]

This subchapter regulates toxic air contaminants (TAC) that are emitted into the ambient air in areas of concern (AOC). Any work practice, material substitution, or control equipment required by the Department prior to June 11, 2004, to control a TAC, shall be retained, unless a modification is approved by the Director. Since no AOC has been designated there are no specific requirements for this facility at this time.

OAC 252:100-43 (Testing, Monitoring, and Recordkeeping)

[Applicable]

This subchapter provides general requirements for testing, monitoring and recordkeeping and applies to any testing, monitoring or recordkeeping activity conducted at any stationary source. To determine compliance with emissions limitations or standards, the Air Quality Director may require the owner or operator of any source in the state of Oklahoma to install, maintain and operate monitoring equipment or to conduct tests, including stack tests, of the air contaminant source. All required testing must be conducted by methods approved by the Air Quality Director and under the direction of qualified personnel. A notice-of-intent to test and a testing protocol shall be submitted to Air Quality at least 30 days prior to any EPA Reference Method stack tests. Emissions and other data required to demonstrate compliance with any federal or state emission limit or standard, or any requirement set forth in a valid permit shall be recorded, maintained, and submitted as required by this subchapter, an applicable rule, or permit requirement. Data from any required testing or monitoring not conducted in accordance with the provisions of this subchapter shall be considered invalid. Nothing shall preclude the use, including the exclusive use, of any credible evidence or information relevant to whether a source would have been in compliance with applicable requirements if the appropriate performance or compliance test or procedure had been performed.

The following Oklahoma Air Pollution Control Rules are not applicable to this facility:

OAC 252:100-8 Part 9	Major Sources Affecting Nonattainment Areas	not in area category
OAC 252:100-15	Mobile Sources	not in source category
OAC 252:100-17	Incinerators	not type of emission unit
OAC 252:100-23	Cotton Gins	not type of emission unit
OAC 252:100-24	Grain Elevators	not in source category
OAC 252:100-29-2	Fugitive Dust/Nonattainment Areas	not in area category
OAC 252:100-39	Nonattainment Areas	not in area category
OAC 252:100-47	Landfills	not in source category

SECTION XII. FEDERAL REGULATIONS

PSD, 40 CFR Part 52

[Applicable]

Emissions of several regulated pollutants exceed the major source level of 100 TPY for a listed source. PSD will apply to any future project whose added emissions exceed the significance levels: CO 100 TPY, NO_x 40 TPY, SO₂ 40 TPY, PM 25 TPY, PM₁₀ 15 TPY, VOC 40 TPY, etc.

NSPS, 40 CFR Part 60

[Subparts Db, VVa and JJJJ Applicable]

Subpart D (Steam Generating Units) regulates fossil fuel fired steam-generating units with a rated heat input above 250 MMBTUH. The auxiliary burner sections, which are used to generate steam, of the Primary Reformers (EU-101B1 and EU-101B2) are physically constrained to be less than 250 MMBTUH due to plant draft limitations. Therefore, NSPS Subpart D does not apply to EU-101B1 or EU-101B2.

Subpart Db (Steam Generating Units) regulates steam-generating units rated between 100 and 250 MMBTUH that commenced construction, reconstruction, or modification after June 19, 1984. The auxiliary burner section of the Primary Reformers (EU-101B1 and EU-101B2) and the Ammonia Unit Startup Boiler (EU-2202UB) are rated at a heat input capacity greater than 100 MMBTUH. However, these units were constructed prior to the effective date of this subpart and no reconstruction has occurred, nor have any emissions increases occurred as a result of a modification. Therefore, NSPS Subpart Db is not applicable except to the new No. 2 Urea Plant boiler. Since the No. 2 Urea Plant Boiler does not burn coal or No. 2 fuel oil, it is only subject to Sections 60.44b, 60.46b, 60.48b, and 60.49b of this subpart (standards of Subpart Db for SO₂ and PM do not apply to gas-fueled boilers). Requirements include:

- Compliance testing for particulate matter and nitrogen oxides (40 CFR 60.46b). The emission standard for oxides of nitrogen is 0.2 lb/MMBTU per §60.44b(a), including periods of start-up, shutdown and malfunction (§60.44b(h). Compliance with the NO_x standard is to be demonstrated on a rolling 30-day basis, except that the initial performance test shall demonstrate compliance on a 24-hour basis and any subsequent performance tests shall demonstrate compliance on a 3-hour basis (§60.44b(i, j)).
- Emissions monitoring for nitrogen oxides (40 CFR 60.48b). The applicant will install a continuous emission monitor (CEM) to monitor NO_x on the No. 2 Urea Plant boiler.
- Reporting and recordkeeping (40 CFR 60.49b). KOCH will record natural gas usage and CEMs data.

Subpart Dc (Steam Generating Units) regulates steam-generating units rated between 10 and 100 MMBTUH that commenced construction, reconstruction, or modification after June 9, 1989. The Urea Boilers (EU-403A and EU-403B) are rated at a heat input capacity between 10 and 100 MMBTUH. However, these units were constructed prior to the effective date of this subpart and no reconstruction has occurred, nor have any emissions increases occurred as a result of a modification. Therefore, NSPS Subpart Dc is not applicable.

Subpart G (Nitric Acid Plants) regulates nitric acid plants that commenced construction, reconstruction, or modification after August 17, 1971, but before October 14, 2011. The nitric acid plant was originally constructed in 1968 and was relocated to the current site from Kennewick, Washington in 1990. 40 CFR 60.14(e) specifically excludes a relocation or change in ownership from the definition of modification. The nitric acid plant has not been reconstructed or modified since it was originally constructed in 1968. Therefore, NSPS Subpart G does not apply.

Subpart Ga (Nitric Acid Plants) regulates nitric acid plants that commenced construction, reconstruction, or modification after October 14, 2011. The nitric acid plant was originally constructed in 1968 and was relocated to the current site from Kennewick, Washington in 1990. The nitric acid plant has not been reconstructed or modified since it was originally constructed in 1968. Therefore, NSPS Subpart Ga does not apply.

Subpart Kb (Volatile Organic Liquids Storage Vessels) regulates volatile organic materials storage tanks with a capacity above 19,183 gallons, which commenced construction, reconstruction, or modification after July 23, 1984. The 54,319-gallon No. 1 Urea conditioning agent storage tank (EU-D202) is above this de minimis level. However, the tank was constructed prior to 1984 and has not been reconstructed or modified since July 23, 1984. NSPS Subpart Kb applies to volatile organic materials with a vapor pressure less than 3.5 kPa (0.5 psi). The conditioning agent has a vapor pressure of approximately 2.2 kPa at the anticipated maximum monthly average temperature of 90 degrees F. Therefore, NSPS Subpart Kb does not apply.

Subpart VVa (Synthetic Organic Chemical Manufacturing) is applicable. Subpart VVa affects synthetic organic chemical manufacturing operations, which commenced construction, reconstruction, or modification after November 7, 2006. Urea is a listed chemical in 40 CFR Part 60.489a. However, per 60.480a(d)(3), if a facility produces only heavy liquid chemicals from heavy liquid feed or raw materials, it is not subject to 60.482 (LDAR). The No. 1 and No. 2 Urea units will be subject only to recordkeeping and reporting requirements under 60.486a(i) and 60.487a.

Subpart IIII (Stationary Compression Ignition Internal Combustion Engines) affects stationary compression ignition (CI) internal combustion engines (ICE) based on power and displacement ratings, depending on date of construction, beginning with those constructed after July 11, 2005. For the purposes of this subpart, the date that construction commences is the date the engine is ordered by the owner or operator. The existing emergency engines at this facility pre-date Subpart IIII. The emergency generator (EUG-18) is not a compression ignition engine subject to this subpart.

Subpart JJJJ, Stationary Spark Ignition Internal Combustion Engines (SI-ICE), promulgates emission standards for all new SI engines ordered after June 12, 2006, and all SI engines modified or reconstructed after June 12, 2006, regardless of size. The specific emission standards (either in g/hp-hr or as a concentration limit) vary based on engine class, engine power rating, lean-burn or rich-burn, fuel type, duty (emergency or non-emergency), and numerous manufacture dates. Engine manufacturers are required to certify certain engines to meet the emission standards and may voluntarily certify other engines. An initial notification is required only for owners and operators of engines greater than 500 HP that are non-certified. Emergency engines will be required to be equipped with a non-resettable hour meter and are limited to 100 hours per year of

operation excluding use in an emergency (the length of operation and the reason the engine was in operation must be recorded). The emergency generators in EUG-18 are subject to the applicable emission standards and all applicable testing, monitoring, recordkeeping, and reporting requirements.

NESHAP, 40 CFR Part 61

[Subparts M and FF Applicable]

Subpart M (Asbestos) regulates asbestos from demolition and renovation activities. Prior to a demolition or renovation activity, owners or operators are required to inspect the affected facility or part of the facility where the renovation and demolition activity will occur for the presence of asbestos, including Category I and Category II non-friable ACM. For demolition or renovation activities subject to this subpart, owners and operators are required to comply with the standards, including notification requirements, under §61.145.

Subpart FF (Benzene Waste Operations) regulates benzene contaminated wastewater at chemical manufacturing plants. The facility is not subject to control requirements of 40 CFR 61 Subpart FF because the total annual benzene quantity from facility wastewater streams is less than 1 Mg/yr. The plant is required to repeat the determination of total annual benzene quantity whenever there is a change in the process generating the waste that could cause the total annual benzene quantity to increase to 1 Mg/yr or more. The plant is also subject to recordkeeping requirements under §61.356 and reporting requirements under §61.357.

NESHAP, 40 CFR Part 63

[Subparts ZZZZ, CCCCCC, and VVVVVV Applicable]

Subparts F, G, H and I (Hazardous Organic NESHAP) affect major sources of HAPs. This plant is an area source rather than a major source.

Subpart FFFF (Miscellaneous Organic Chemicals) affects facilities which produce the listed organic chemicals. Ammonia, nitric acid, urea, and UAN are not among the listed chemicals.

Subpart ZZZZ, Reciprocating Internal Combustion Engines (RICE). This subpart previously only affected RICE with a site-rating greater than 500 brake horsepower that are located at a major source of HAP emissions. The EPA published a final rule that promulgates standards for new and reconstructed engines (after June 12, 2006) with a site rating of less than or equal to 500 HP located at major sources, and for new and reconstructed engines (after June 12, 2006) located at area sources. Owners and operators of new engines and reconstructed engines at area sources and of new or reconstructed engines with a site rating of equal to or less than 500 HP located at a major source (except new or reconstructed 4-stroke lean burn engines with a site rating of greater than or equal to 250 HP and less than or equal to 500 HP located at a major source) must meet the requirements of either 40 CFR Part 60 Subpart IIII (for CI engines) or 40 CFR Part 60 Subpart JJJJ (for SI engines). Owners and operators of new or reconstructed 4SLB engines with a site rating of greater than or equal to 250 HP and less than or equal to 500 HP located at a major source are subject to the same MACT standards previously established for 4SLB engines above 500 HP at a major source, and must also meet the requirements of 40 CFR Part 60 Subpart JJJJ, except for the emissions standards for CO.

On March 3, 2010, EPA finalized additional requirements for stationary CI RICE located at area sources. A summary of these requirements for the emergency generator engine and fire pump engine located at this facility are shown below.

Engine Category	Normal Operation @ 15% O ₂
Existing Emergency CI & Black Start CI	Change oil and filter every 500 hours of operation or annually, whichever one comes first; Inspect air cleaner every 1,000 hours of operation or annually, whichever one comes first; and Inspect all hoses and belts every 500 hours of operation or annually, whichever one comes first and replace as necessary.

Sources have the option to utilize an oil analysis program in order to extend the specified oil change requirements of this subpart. Initial compliance demonstrations must be conducted within 180 days after the compliance date. Owners and operators of a non-operational engine can conduct the performance test when the engine is started up again.

Other applicable requirements include:

- 1) The owner/operator must operate and maintain the stationary RICE and after-treatment control device (if any) according to the manufacturer's emission-related written instructions or develop their own maintenance plan which must provide to the extent practicable for the maintenance and operation of the engine in a manner consistent with good air pollution control practice for minimizing emissions.
- 2) Existing emergency stationary RICE located at an area source of HAP emissions must install a non-resettable hour meter if one is not already installed.

Existing stationary CI RICE (EUG-19) located at an area source of HAP emissions must comply with the applicable emission limitations and operating limitations no later than May 3, 2013. The permit will require the facility to comply with all applicable requirements.

Subpart DDDDD, National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial and Institutional Boilers and Process Heaters at major sources of HAPs. This facility is an "area" source of HAPs.

Subpart CCCCC, Gasoline Dispensing Facilities. This subpart establishes emission limitations and management practices for HAP emitted from the loading of gasoline storage tanks at gasoline dispensing facilities (GDF) located at an area source. GDF means any stationary facility which dispenses gasoline into the fuel tank of a motor vehicle. The affected source includes each gasoline cargo tank during the delivery of product to a GDF and also includes each storage tank. This regulation applies to EUG 20.

If a GDF has a monthly throughput of less than 10,000 gallons of gasoline, the operator must not allow gasoline to be handled in a manner that would result in vapor releases to the atmosphere for extended periods of time. Measures to be taken include, but are not limited to, the following:

- 1) Minimize gasoline spills;
- 2) Clean up spills as expeditiously as practicable;
- 3) Cover all open gasoline containers and all gasoline storage tank fill-pipes with a gasketed seal when not in use;
- 4) Minimize gasoline sent to open waste collection systems that collect and transport gasoline to reclamation and recycling devices, such as oil/water separators.

Subpart JJJJJJ, Industrial, Commercial, and Institutional Boilers. This subpart affects new and existing boilers located at area sources of HAP, except for gas-fired boilers. Gas fired boilers are defined as any boiler that burns gaseous fuel not combined with any solid fuels, liquid fuel only during periods of gas curtailment, gas supply emergencies, or periodic testing on liquid fuel. The boilers and auxiliary boilers at this facility meet the definition of gas fired boilers and are not subject to this subpart. Process heaters such as the Ammonia Reformers are not regulated by Subpart JJJJJJ. Therefore, this regulation does not apply to the Enid site.

Subpart VVVVVV, Chemical Manufacturing Area Sources. This subpart affects each chemical manufacturing process unit that uses as feedstocks or generates as products or byproducts any of the listed organic or metal HAPs. The compliance date for Subpart VVVVVV is October 29, 2012. The facility does not produce any organic HAP in Table 1 of Subpart VVVVVV, but does have nickel and chromium as components of catalysts. Therefore, Subpart VVVVVV does apply to the site.

Compliance Assurance Monitoring, 40 CFR Part 64

[Applicable]

Compliance Assurance Monitoring, as published in the Federal Register on October 22, 1997, applies to any pollutant specific emission unit at a major source that is required to obtain a Title V permit. 40 CFR 64.5(b) requires the owner or operator to submit a CAM plan (if applicable) as part of the application for the renewal for a Part 70 permit. The Nitric Acid Plant stack is subject to emission limitations in this permit and is equipped with a non-selective catalytic reduction system, which reduces emissions of nitrogen oxides (NO_x). KOCH is required by this permit to operate a continuous emissions monitoring system (CEMS) to record emissions of NO_x from the Nitric Acid Plant stack on a continuous basis. In accordance with 40 CFR 64.2(b)(vi), CAM requirements do not apply to units equipped with a permit-required CEMS. CAM for the urea granulators will be required for permit renewal.

Chemical Accident Prevention Provisions, 40 CFR Part 68

[Applicable]

The plant has substances regulated under 40 CFR Part 68 present in quantities greater than the threshold quantities; therefore, 40 CFR Part 68 is applicable. A Risk Management Plan was submitted on June 16, 1999, and determined to be complete by EPA. KOCH has prepared the plant's updated RMP and it was submitted by the June 21, 2004 deadline. KOCH is in compliance with requirements of this part, including registration and submission of an RMP. More information on this federal program is available on the web page: www.epa.gov/rmp.

Stratospheric Ozone Protection, 40 CFR Part 82

[Subpart A and F Applicable]

These standards require phase out of Class I & II substances, reductions of emissions of Class I & II substances to the lowest achievable level in all use sectors, and banning use of nonessential products containing ozone-depleting substances (Subparts A & C); control servicing of motor vehicle air conditioners (Subpart B); require Federal agencies to adopt procurement regulations which meet phase out requirements and which maximize the substitution of safe alternatives to Class I and Class II substances (Subpart D); require warning labels on products made with or containing Class I or II substances (Subpart E); maximize the use of recycling and recovery upon disposal (Subpart F); require producers to identify substitutes for ozone-depleting compounds under the Significant New Alternatives Program (Subpart G); and reduce the emissions of halons (Subpart H).

Subpart A identifies ozone-depleting substances and divides them into two classes. Class I controlled substances are divided into seven groups; the chemicals typically used by the manufacturing industry include carbon tetrachloride (Class I, Group IV) and methyl chloroform (Class I, Group V). A complete phase-out of production of Class I substances is required by January 1, 2000 (January 1, 2002, for methyl chloroform). Class II chemicals, which are hydrochlorofluorocarbons (HCFCs), are generally seen as interim substitutes for Class I CFCs. Class II substances consist of 33 HCFCs. A complete phase-out of Class II substances, scheduled in phases starting by 2002, is required by January 1, 2030. This facility does not utilize any Class I & II substances.

SECTION XII. COMPLIANCE

Tier Classification and Public Review

This application has been determined to be a Tier I because it is a minor modification to a PSD construction permit.

The applicant has submitted an affidavit that they are not seeking a permit for land use or for any operation upon land owned by others without their knowledge. The affidavit certifies that the applicant owns the property or has provided appropriate notification.

Information on all permit actions is available for review by the public in the Air Quality section of the DEQ Web page: <http://www.deq.state.ok.us/>.

The “proposed” permit was submitted to EPA for a 45-day review period. No comments were received from Region VI.

Fees Paid

Construction permit modification fees of \$5,000.

SECTION XIII. SUMMARY

The facility has demonstrated the ability to comply with the requirements of the several air pollution control rules and regulations. Ambient air quality standards are not threatened at this site. Issuance of the permit is recommended.

**PERMIT TO CONSTRUCT
AIR POLLUTION CONTROL FACILITY
SPECIFIC CONDITIONS**

**Koch Fertilizer Enid LLC
Enid Nitrogen Plant**

Permit No. 2016-1295-C (M-5)(PSD)

The permittee is authorized to construct in conformity with the specifications submitted to Air Quality on February 13, 2019. The Evaluation Memorandum dated May 13, 2019, explains the derivation of applicable permit requirements and estimates of emissions; however, it does not contain limitations or permit requirements. Commencing construction or continuing operations under this permit constitutes acceptance of, and consent to the conditions contained herein.

1. Point of emissions and applicable emissions limitations. [OAC 252:100-8-6(a)(1)]

EUG 1 Plant-wide Emissions Cap

- A. The permittee shall limit actual annual emissions of methanol from the plant to 9.9 TPY (calculated on a 12-month rolling total). Actual annual plant-wide methanol emissions shall be calculated each month and the 12-month rolling total shall be determined. Relevant records specified in Specific Condition 5 will be used in the methanol emission calculations, as applicable.
- B. The permittee shall tabulate monthly methanol emissions using the methods outlined below or based on equivalent methods as accepted by ODEQ.
1. Emissions from methanol-containing conditioning agent(s) shall be calculated on a mass balance basis from the weight of conditioning agent(s) added to urea from each urea plant times the weight percent of methanol in the conditioning agent(s). The average weight percent of methanol in the conditioning agent(s) shall be based on a 12-month rolling average calculated for each granular urea plant.
 2. Emissions from diverting process condensate from the process condensate stripper to the zero discharge pond or emergency venting from the process condensate stripper stack to the atmosphere, shall be calculated based on the methanol concentrations in the condensate times the volume of condensate diverted to the ponds and/or the methanol concentrations exhausted to the atmosphere.
 3. Methanol emissions during plant startup, shutdown, and/or malfunction events from each of the CO₂ strippers (PIC-30 vents) shall be calculated as 0.476 lb methanol per ton CO₂ or based on factors derived for each PIC-30 vent from the most recent ODEQ-approved stack test.
- C. Facility-wide process CO₂ emissions shall not exceed 1,260,000 tons per year, 12-month rolling average.

1. Facility-wide process CO₂e emissions shall not exceed 1,260,000 tons per year, 12month rolling average. Compliance with this limit will be demonstrated using 40 CFR 98, Subpart G to calculate the amount of process CO₂ produced plant-wide, then subtracting the amount of CO₂ sold or consumed plant-wide using a mass balance approach. Relevant records specified in Specific Condition 5 will be used in the CO₂ emission calculations, as applicable.
2. Plant-wide process CO₂ emissions shall not exceed a rate of 1.26 tons CO₂e emitted per ton ammonia produced on 12-month rolling average. Compliance with this limit will be demonstrated using the procedure in paragraph C.1 to calculate plant-wide CO₂e emissions and site production records to calculate the amount of ammonia produced plant-wide.

D. The permittee shall limit combustion CO₂e as follows:

1. Total combustion CO₂e emissions from the emission unit groups EUG 2, EUG 3 (except this limit does not apply to 2202UB), and EUG 23, shall not exceed 1,318,669 tons per year on a 12-month rolling average. Compliance with this limit will be demonstrated using 40 CFR 98, Subpart C to calculate combustion CO₂ from these emission unit groups.
2. Combustion CO₂ emissions from the emission unit groups: EUG 2, EUG 3 (except this limit does not apply to 2202UB), and EUG 23, shall not exceed 117 lb/MMBtu. Compliance with this limit will be demonstrated using records of fuel consumed.
3. Compliance Demonstration: Use of pipeline-quality natural gas as the only fuel demonstrates compliance with combustion CO₂e emissions limitations for EUG 2, EUG 3, and EUG 23. Compliance can be shown by the following methods: for pipeline grade natural gas, a current gas company bill. Compliance shall be demonstrated at least once annually.

EUG 2 Ammonia Plant Primary Reformers

Location	EU ID	Heat Input*
Ammonia Plant #1	101B1	965 MMBTUH
Ammonia Plant #2	101B2	990 MMBTUH

*Heat input limitation is for a 12-month rolling averaging period, and includes arch burners, tunnel burners, superheat burners, and auxiliary boiler burners.

Point ID	Emission Unit	PM₁₀ / PM_{2.5}		SO₂		NO_x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
2-9095 (No. 1 Reformer)	101B1	8.02	31.49	0.95	3.73	215.20	500.86	8.70	28.49	88.61	348.08
2-9097 (No. 2 Reformer)	101B2	10.06	32.31	1.19	3.83	270.00	173.45	9.10	29.23	111.18	357.10

- A. The above fuel-burning equipment shall be fueled by pipeline quality natural gas and ammonia and HRU plant purge gas as primary fuels.

- B. Emissions of NO_x from the No. 1 and No. 2 Reformers shall not exceed 0.20 lb/MMBTU, 3-hour average. [OAC 252:100-33]
- C. The permittee shall operate and maintain continuous emissions monitoring systems (CEMS) for measuring emissions of NO_x and CO from each reformer. The CEMS shall be certified and quality-assured using the methods and procedures of 40 CFR 60, Appendices B and F.
- D. Within 180 days following completion of physical modifications to the each reformer's heaters, performance testing shall be conducted and a written report of results submitted to AQD. The following USEPA methods shall be used for testing of emissions, unless otherwise approved by Air Quality:
- Method 1: Sample and Velocity Traverses for Stationary Sources.
Method 2: Determination of Stack Gas Velocity and Volumetric Flow Rate.
Method 3: Gas Analysis for Carbon Dioxide, Excess Air, and Dry Molecular Weight.
Method 4: Moisture in Stack Gases.
Method 7E: NO_x Emissions from Stationary Sources
Method 10: Carbon Monoxide Emissions from Stationary Sources
- E. A copy of the test plan shall be provided to AQD at least 30 days prior to each test date.
- F. Performance testing shall be conducted while the units are operating within 10% of the rates at which operating permit authorization will be sought.
- G. At least 30 days prior to the testing, a notification of the test date and testing protocol shall be submitted to AQD. Deficiencies in the protocol shall be resolved prior to commencement of testing.
- H. Combustion CO_{2e} emissions shall not exceed 117 lb CO_{2e} / MMBTU heat input (30 day rolling average). [OAC 252:100-8-34(b)]
- I. Prior to commencement of operations of the new boiler in EUG-23, the No. 2 Reformer shall include a selective catalytic reduction system which achieves NO_x emissions of 0.04 lb/MMBTU or less. [OAC 252:100-8-5]
- J. The following requirements demonstrate compliance with the heat input restrictions for EUG 2. [OAC 252:100-43]
1. The permittee shall measure natural gas and ammonia plant purge gas flow to the primary reformers. Flow instrumentation shall be calibrated semi-annually.

2. The permittee shall calculate the total fuel energy usage in each plant by adding the total natural gas energy for fuel to the purge gas energy usage for fuel for each plant.
 3. The permittee shall calculate the average hourly heat input for each plant by dividing the total plant fuel energy usage by the number of hours the plant operated during the month. Monthly calculations shall be used to determine the heat input on a 12-month rolling average.
- K. Emissions of NO_x and CO from the reformers shall be determined on an hourly basis by multiplying the heat input (MMBTUH) by the emission rates (lb/MMBTU obtained from CEMS data). Compliance with the lb/hr emission limitations for NO_x and CO shall be based upon a 3-hour averaging period using the arithmetic average from three contiguous 1-hour periods. Hourly emissions of VOC, SO₂, and PM shall be determined monthly based on multiplying AP-42 factors by the monthly total heat input and dividing by the monthly total hours of operations.
- L. 12-month rolling emissions shall be calculated as follows: emissions of NO_x and CO from the reformers shall be determined on a monthly basis by totaling the hourly emissions. Emissions of VOC, SO₂, and PM shall be determined monthly based on AP-42 factors and the monthly total heat input rates. Compliance with the annual emission limitations shall be based upon a 12-month rolling total and the first 12-month rolling period shall begin on start-up following modification.

EUG 3 Heaters/Boilers > 50 MMBTUH

Location	EU ID	EU Name/Model
Ammonia Plant #1	2202UB	Ammonia Unit Startup Boiler
No. 1 Urea Plant	403A	No. 1 Urea Boiler No. 1
No. 1 Urea Plant	403B	No. 1 Urea Boiler No. 2

Point ID	Emission Unit	PM ₁₀		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
3-9099	2202UB	1.6	3.5	0.1	0.2	28.8	63.0	1.2	2.6	17.8	39.0
3-9100	403A	0.94	4.11	0.07	0.32	16.80	73.58	0.68	2.98	10.38	45.45
3-9101	403B	0.94	4.11	0.07	0.32	16.80	73.58	0.68	2.98	10.38	45.45

All emissions limits on a TPY basis are on a 12-month rolling basis.

- A. The fuel-burning equipment shall be fired with pipeline grade natural gas.
- B. Emissions of nitrogen oxides from the fuel burning equipment shall not exceed 0.2 lb/MMBTU, three hour average. [OAC 252:100-33-2(a)]
- C. Operation of EU 2202UB is limited to 4,380 hours per year annual operation.
- D. Compliance Demonstration: Use of pipeline-quality natural gas as the only fuel and having hours of operation less than or equal to 4,380 hours per year (12-month rolling total) for EU 2202UB demonstrates compliance with the lb/hr and TPY emissions limitations for EUG 3. Compliance can be shown by the following methods: for

pipeline grade natural gas, a current gas company bill. Compliance shall be demonstrated at least once annually.

EUG 4 Heaters/Boilers < 50 MMBTUH

Location	EU ID	EU Name/Model
Ammonia Plant #1	102B1	Ammonia Unit Startup Heater No. 1
Ammonia Plant #2	102B2	Ammonia Unit Startup Heater No. 2

Point ID	Emission Unit	PM₁₀		SO₂		NO_x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
4-9102	102B1	0.4	1.6	0.03	0.1	4.9	21.3	0.3	1.2	4.1	17.9
4-9103	102B2	0.4	1.6	0.03	0.1	4.9	21.3	0.3	1.2	4.1	17.9

- A. The fuel-burning equipment shall be fired with pipeline grade natural gas.
- B. Compliance Demonstration: Use of pipeline-quality natural gas as the only fuel demonstrates compliance with emissions limitations for EUG 4. Compliance can be shown by the following methods: for pipeline grade natural gas, a current gas company bill. Compliance shall be demonstrated at least once annually.

EUG 5 No. 1 Urea Plant Conditioning Agent Storage Tank: The equipment item listed below is considered insignificant.

Location	EU ID	EU Name
No. 1 Urea Plant	D202	Conditioning Agent Tank

- A. Methanol emission limitations and compliance demonstration for this source are addressed in Item A for EUG 1.

EUG 6 No. 1 Urea Plant Granulators

Point ID	Emission Unit	PM₁₀	
		lb/hr	TPY
6-9104	Granulator 1	6.60	28.92
6-9105	Granulator 2	6.60	28.92
6-9106	Granulator 3	6.60	28.92

- A. Compliance Demonstration: Visible emissions observations shall be performed at least monthly during normal plant operations by conducting a plant walkthrough for sources categorized under EUG 6. A record shall be maintained indicating if any opacity or visible emissions (excluding steam, fog, or icy mist from the presence of uncombined water) were observed during the monthly observations. If visible emissions are detected during normal operations, corrective action shall be taken as soon as possible and/or a six-minute opacity reading in accordance with EPA Reference Method #9 (RM 9) will be conducted within three (3) working days. [OAC 252:100-25-3(b)]

- B. All discharges from each urea granulation operation shall be processed by a high-efficiency spray tower wet scrubber or equivalent device for PM emissions control.
[OAC 252:100-8-34(b)(1)]
- C. Each scrubber shall be operated with a pressure differential of at least 7 inches WC when processing discharges from each urea plant granulator stack. The pressure differential from each scrubber shall be monitored and recorded at least once daily when operating. If the pressure differential is found to be less than 7 inches WC, corrective action shall be taken within four (4) hours and another reading taken. If two (2) consecutive readings are found to be out of range, a possible deviation may have occurred and the permittee shall include such event in the Title V Semi-Annual Monitoring and Deviation Report.
[OAC 252:100-43]
- D. The permittee is subject to following requirements under 40 CFR 60, Subpart VVa for the urea plant, as applicable:
- i. 60.486a: Recordkeeping requirements
 - ii. 60.487a. Reporting requirements

EUG 7 No. 1 Urea Plant Synthesis Vents

Point ID	Emission Unit	CO		PM ₁₀	
		lb/hr	TPY	lb/hr	TPY
7-9111	No. 1 Urea High Pressure Vent	3.86	16.40	1.87	7.92
7-9110	No. 1 Urea Low Pressure Vent				

- A. Compliance Demonstration: Compliance with these limits is demonstrated by Urea production of 1,550 TPD (monthly average) or less.

EUG 9: No. 2 Ammonia Plant Cooling Tower

Point ID	Emission Unit	PM ₁₀		PM _{2.5}		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
9-9159	No. 2 Ammonia Plant Cooling Tower	0.46	2.02	0.002	0.009	--	--	--	--	--	--

- A. Compliance Demonstrations: the following records shall be kept for the No. 2 Ammonia Plant Cooling Tower:
[OAC 252:100-43]
- i. Records of vendor certification of maximum circulation rate
 - ii. Records of design and construction showing 0.0005% or better drift, on the added cell.
 - iii. Records of TDS content of cooling water, tested within 180 days of start-up.

EUG 10 CO₂ Stripping Towers:

Point ID	Emission Unit	CO	
		lb/hr	TPY
10-9120	CO ₂ Stripping Tower 1	5.8	25.4
10-9121	CO ₂ Stripping Tower 2	5.8	25.4

All emissions limits on a TPY basis are on a 12-month rolling basis.

- A. The permittee shall maintain logs of the duration (hours) of venting to the atmosphere.
[OAC 252:100-43]
- B. Excess emissions resulting from unanticipated events, such as malfunctions, shall be reported consistent with 252:100-5 and 252:100-9.

EUG 11 Nitric Acid Plant:

Point ID	Emission Unit	NO _x		
		ppm*	lb/hr	TPY
12-9115	Nitric Acid Plant – Normal Operation	79	5.0	21.9
	Nitric Acid Plant – Start-up and Shutdown	750	47.5	3.6

*based upon a 3-hour averaging period using the arithmetic average from three contiguous 1-hour periods. All emissions limits on a TPY basis are on a 12-month rolling basis.

- A. Air emissions from the nitric acid plant shall be processed by an abatement system that reduces NO_x emissions to 79 ppm_{dv} or less, based on a 3-hour averaging period using the arithmetic average from three contiguous one-hour periods. The permittee shall maintain compliance with the NO_x limits at all times, except as specified in Condition F below.
- B. The permittee shall operate and maintain a continuous emission monitoring system (CEMS) for measuring nitrogen oxides. Except for periods of system breakdowns, repairs, calibration checks, and zero and span adjustments not to exceed a total of 2.5% of the operating hours in a calendar quarter, the CEMS shall be in continuous operation.
[OAC 252:100-43]
- C. A record shall be maintained of emissions resulting from start-up, shutdown, and malfunction events and the duration of each occurrence. Emissions resulting from start-up, shutdown and malfunction events shall be quantified for this source and reported in the facility's annual emissions inventory.
- D. When monitoring shows concentrations in excess of the ppm limit for either normal operations (79 ppm) or for start-ups and shutdowns (750 ppm), the owner or operator shall comply with reporting provisions of OAC 252:100-9-3 for excess emissions. Requirements for periods of other excess emissions (during normal operations) include prompt notification to Air Quality and prompt commencement of repairs to correct the condition of excess emissions.
[OAC 252:100-9]

- E. Compliance Demonstration: the permittee shall maintain a continuous emission monitoring system (CEMS) for measuring nitrogen oxides. Compliance with the ppm limit will be determined on the basis of a 3-hour averaging period using the arithmetic average from three contiguous one-hour periods. Compliance with NO_x emissions rates on a lb/hr basis may be calculated as 0.0181 lb/ton/ppm NO_x and annual basis using monthly nitric acid production on 100 percent basis on a 12-month rolling period. Except for periods of malfunction, repairs, calibration checks, and zero and span adjustments, the CEM shall be in continuous operation. [OAC 252:100-43]
- F. During periods of start-up and shutdown of the nitric acid plant, NO_x emissions (3-hour average using the arithmetic average from three contiguous 1-hour periods) shall not exceed 750 ppm. A shutdown event is defined as the cessation of nitric acid plant operations for any reason and begins at the time when ammonia feed stops and ends three hours later. A start-up event is defined as the process of initiating nitric acid production operations and begins 1 hour prior to the initiation of ammonia feed and ends no more than 5 hours after initiating ammonia feed. The maximum number of start-up or shutdown events shall not exceed 50 events per calendar year.

EUG 12 Urea Ammonium Nitrate (UAN) Plant:

Point ID	Emission Unit	PM ₁₀		CO	
		lb/hr	TPY	lb/hr	TPY
12-9116	UAN Plant	2.6	11.0	0.1	0.5

- A. Compliance Demonstration: Visible observations shall be performed at least monthly during normal plant operations by conducting a plant walkthrough for sources categorized under EUG 12. A record shall be maintained indicating if any opacity or visible emissions (excluding steam, fog, or icy mist from the presence of uncombined water) were observed during the monthly observations. If visible emissions are detected during normal operations, corrective action shall be taken as soon as possible and/or a six-minute opacity reading in accordance with EPA Reference Method #9 (RM 9) will be conducted within three (3) working days. [OAC 252:100-25-3(b)]

EUG 13 Flare

Location	EU ID	EU Name
Ammonia Plant	222OU	Flare

EU ID	NO _x TPY
222OU	15.8

- A. Compliance with the NO_x emission limitation from the flare is based on a 12-month rolling total.

- B. The flare shall be fueled with pipeline quality natural gas and/or ammonia plant purge gas as fuel to maintain the pilot, maintain pressure to the flare during idling, and as enrichment fuel if needed. The flare is authorized to flare ammonia and process off-gases.
- C. The flare system shall be operated with the following equipment:
1. Thermocouple or any other equivalent device to detect the presence of a flame.
 2. Steam heated vaporizer for vaporization of any liquids from railcar depressurizing or other sources as needed.
- D. Compliance Demonstration: Compliance with the NO_x emission limit will be demonstrated based on maintaining throughput records for material (fuel and flared streams) sent to the flare and estimating NO_x emissions (12-month rolling total). Compliance with the equipment standards set forth in Permit Condition C for EUG 13 will be demonstrated through annual verification with Plant personnel that the equipment exists as stated.

EUG 14 Fugitives

Location	EU ID	Point ID	EU Name
No. 1 Urea Plant	UMH	14-9120	No. 1 Urea Plant Material Handling/Loading Fugitives

- A. Except for truck and railcar loading, urea handling operations shall take place within completely-enclosed buildings, etc., without direct exposure to winds. Railcar and truck loading may take place in partially-enclosed operations which provide some shelter from winds.
[OAC 252:100-29]

EUG 14A No. 1 Urea Plant Fugitives

EU ID	Point ID	EU Name
UMS	UMS	No. 1 Urea Materials Storage
UMH	UMH	No. 1 Urea Materials Handling
UML	UML	No. 1 Urea Materials Loading

- A. Except for truck and railcar loading, urea handling drop operations shall take place within completely-enclosed buildings, etc.. The conveyor leading from the No. 1 Urea storage warehouse to the No. 1 Urea storage dome shall be at least partially-enclosed. Railcar and truck loading may take place in partially-enclosed operations which provide some shelter from winds.
[OAC 252:100-29]

EUG 15 Start-up/Shutdown Vents: The methanol limit and compliance demonstration are addressed in EUG 1, (plant-wide emission cap)

Point ID	Emission Unit	CO	
		lb/hr	TPY
15-9151	Ammonia Plant 1 SU/SD Vent No.1 (PV-102 & PV-5)	10,962.8	345.3
15-9154	Ammonia Plant 2 SU/SD Vent No.1 (PV-102 & PV-5)	10,962.8	345.3
15-9109	Ammonia Plant #2 Process Condensate Stripper (308E)	--	--

Starting on January 1, 2014, CO emissions shall be calculated and reported on a 12-month rolling total basis, using emissions from the previous eleven months and the current month. Starting on January 1, 2014 all emissions limits on a TPY basis shall be calculated on a 12-month rolling basis.

- A. The permittee shall maintain records of the duration (hours) and amount of venting to the atmosphere (12-month rolling total).
- B. Compliance Demonstration: records contained in the log specified in Item A for EUG 15 shall demonstrate compliance.
- C. Excess emissions resulting from unanticipated events, such as malfunctions, shall be reported consistent with 252:100-5 and 252:100-9.

EUG 16 No. 1 Urea Plant Cooling Tower

EU ID	Point ID	EU Name
22014E	22014E	No. 1 Urea Plant Cooling Tower No. 2

- A. The No. 1 Urea Plant cooling tower No. 2 shall be maintained with drift eliminators that achieve a drift efficiency of 0.002 percent.

EUG 17 Insignificant Activities

The equipment items listed below are considered insignificant. Although emission limits are not specified, the facility will keep records demonstrating the continued insignificance of these items. Other insignificant emission sources may exist at the facility for which recordkeeping is not required. Recordkeeping shall be maintained for insignificant activities as required by Specific Condition No. 6.

Unit ID	Description
R-2401	Glycol dehydration reboiler (1.5 MMBTUH)
APP-IC	475-hp Portable mixer engine *
APP-Portable Unit	APP Portable 10-34-0 processing unit*
Diesel	Diesel storage tanks (3)
UAN TANKS	UAN tanks (2)
LIME	Lime silos (2)
#1 Plant 108-D Vent	No. 1 Ammonia Plant TV-50 vent
#1 PIC-14 Vent	No. 1 Ammonia Plant PIC-14 fuel vent
#1 PIC-33 Vent	No. 1 Ammonia Plant PIC-33 fuel vent
#1 Catalyst Warm-ups	No. 1 Ammonia Plant catalyst warm-up vent (SP-73)
#1 Low Shift Vent	No. 1 Ammonia Plant Low-Shift Reductions vent (SP-73)
#1 LTS Catalyst Cooling	No. 1 Ammonia Plant LTS Catalyst Cooling vent (SP-73)
#1 HTS Catalyst Cooling	No. 1 Ammonia Plant HTS Catalyst Cooling vent (SP-73)
#1 Methanator Unit Catalyst Cooling	No. 1 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)
#2 Plant 108-D Vent	No. 2 Ammonia Plant TV-50 vent
#2 PIC-14 Vent	No. 2 Ammonia Plant PIC-14 fuel vent
#2 PIC-33 Vent	No. 2 Ammonia Plant PIC-33 fuel vent
#2 Catalyst Warm-ups	No. 2 Ammonia Plant catalyst warm-up vent (SP-73)
#2 Low Shift Vent	No. 2 Ammonia Plant Low-Shift Reductions vent (SP-73)
#2 LTS Catalyst Cooling	No. 2 Ammonia Plant LTS Catalyst Cooling vent (SP-73)
#2 HTS Catalyst Cooling	No. 2 Ammonia Plant HTS Catalyst Cooling vent (SP-73)
#2 Methanator Unit Catalyst Cooling	No. 2 Ammonia Plant Methanator Catalyst Cooling vent (SP-73)
Laboratory Vents	Laboratory fume hoods and vents
UR2FBATK	No. 2 Urea Plant Conditioning Agent Tank

* Equipment owned, operated, and maintained by a contractor.

- A. Compliance Demonstration: Relevant records specified in Specific Condition 6 will be used annually, as applicable, to demonstrate continued insignificant status. Compliance with the equipment standards set forth will be demonstrated through annual verification with plant personnel annually that the equipment exists as stated.

EUG 18. Emergency Engines Subject to NSPS Subpart JJJJ

Point ID#	Capacity (hp)	Make/Model	Installed Date
GEN2	147	Generac 6.8GN	2010
GEN3	40	Olympian G25LTA	2011

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
GEN2	Generac 6.8GN	0.02	0.01	0.01	0.01	0.65	0.16	0.32	0.08	1.30	0.32
GEN3	Olympian G25LTA	0.01	0.01	0.01	0.01	0.88	0.04	0.01	0.01	34.13	1.71

- A. The emergency generator engines listed above are subject to 40 CFR Part 60, Subpart JJJJ, and shall comply with all applicable standards for owners or operators of stationary spark ignition internal combustion engines:
1. 60.4230: Am I subject to this subpart?
 2. 60.4231: What emission standards must I meet if I am a manufacturer of stationary SI internal combustion engines?
 3. 60.4232: How long must my engines meet the emissions standards if I am a manufacturer of stationary SI internal combustion engines?
 4. 60.4233: What emission standards must I meet if I am an owner or operator of a stationary SI internal combustion engine?
 5. 60.4234: How long must I meet the emissions standards if I am an owner or operator of a stationary SI internal combustion engine?
 6. 60.4235: What fuel requirements must I meet if I am an owner or operator of a stationary SI internal combustion engine?
 7. 60.4236: What is the deadline for importing or installing stationary SI ICE produced in the previous model year?
 8. 60.4237: What are the monitoring requirements if I am an owner or operator of a stationary SI internal combustion engine?
 9. 60.4238: What are my compliance requirements if I am a manufacturer of stationary SI internal combustion engines \leq 19 KW (25 HP).
 10. 60.4239: What are my compliance requirements if I am a manufacturer of stationary SI internal combustion engines \geq 19 KW (25 HP) that use gasoline?
 11. 60.4240: What are my compliance requirements if I am a manufacturer of stationary SI internal combustion engines \geq 19 KW (25 HP) that use LPG?
 12. 60.4241: What are my compliance requirements if I am a manufacturer of stationary SI internal combustion engines participating in the voluntary certification program?
 13. 60.4242: What other requirement must I meet if I am a manufacturer of stationary SI internal combustion engines?
 14. 60.4243: What are my compliance requirements if I am an owner or operator of a stationary SI internal combustion engine?
 15. 60.4244: What test methods and other procedures must I use if I am an owner or operator of a stationary SI internal combustion engine?
 16. 60.4245: What are my notification, reporting, and recordkeeping requirements if I am an owner or operator of a stationary SI internal combustion engine?
 17. 60.4246: What parts of the General Provisions apply to me?
 18. 60.4247: What parts of the mobile source provisions apply to me if I am a manufacturer of stationary SI internal combustion engines?
 19. 60.4248: What definitions apply to this subpart?

EUG 19. Diesel Engines Subject to NESHAP Subpart ZZZZ

Point ID#	Capacity (hp)	Make/Model	Serial Number	Installed Date
GEN	460	Cummins KT-1150-G	100P1432	1976
PUMP	145	Clarke VMFPT6HT	91B-02093	2002

- A. Upon the compliance date of NESHAPS Subpart ZZZZ, the owner/operator shall comply with all applicable requirements of the NESHAP: Reciprocating Internal Combustion Engines, Subpart ZZZZ, for each affected facility including but not limited to:

[40 CFR 63.6580 through 63.6675]

What This Subpart Covers

1. § 63.6580 What is the purpose of subpart ZZZZ?
2. § 63.6585 Am I subject to this subpart?
3. § 63.6590 What parts of my plant does this subpart cover?
4. § 63.6595 When do I have to comply with this subpart?

Emission and Operating Limitations

5. § 63.6603 What emission limitations and operating limitations must I meet if I own or operate an existing stationary RICE located at an area source of HAP emissions?

General Compliance Requirements

6. § 63.6605 What are my general requirements for complying with this subpart?

Testing and Initial Compliance Requirements

7. § 63.6625 What are my monitoring, installation, operation, and maintenance requirements?
8. § 63.6630 How do I demonstrate initial compliance with the emission limitations and operating limitations?

Continuous Compliance Requirements

9. § 63.6640 How do I demonstrate continuous compliance with the emission limitations and operating limitations?

Notifications, Reports, and Records

10. § 63.6650 What reports must I submit and when?
11. § 63.6655 What records must I keep?
12. § 63.6660 In what form and how long must I keep my records?

Other Requirements and Information

13. § 63.6665 What parts of the General Provisions apply to me?
14. § 63.6670 Who implements and enforces this subpart?
15. § 63.6675 What definitions apply to this subpart?

EUG 20. Gasoline Tank

Unit ID	Point	EU Description	Capacity	Construction Date
Gasoline	Gasoline	Vehicle gasoline tank	1,128 gal	Pre-2003

- A. The gasoline storage tank shall be equipped and operated with a permanent submerged fill pipe.
[OAC 252:100-37-15(b)]
- B. The owner/operator shall comply with all applicable requirements of the NESHAP Subpart CCCCCC, for each affected facility including but not limited to:
[40 CFR 63.11110 through 63.11132]
1. Minimize gasoline spills;
 2. Clean up spills as expeditiously as practicable;
 3. Cover all open gasoline containers and all gasoline storage tank fill-pipes with a gasketed seal when not in use;
 4. Minimize gasoline sent to open waste collection systems that collect and transport gasoline to reclamation and recycling devices, such as oil/water separators.

EUG 21: No. 2 Urea Plant Synthesis Vent

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
21-9163	No. 2 Urea Plant Vent	0.05	0.20	--	--	--	--	--	--	3.08	12.83

- A. Compliance Demonstration: Compliance with these limits is demonstrated by Urea production of 2,900 TPD (monthly average) or less.
- B. Within 180 days following commencement of operations of the new urea granulator, the permittee shall conduct performance testing as follows and furnish a written report to Air Quality.
[OAC 252:100-43]
- C. The following USEPA methods shall be used for testing of emissions, unless otherwise approved by Air Quality:
- Method 1: Sample and Velocity Traverses for Stationary Sources.
 - Method 2: Determination of Stack Gas Velocity and Volumetric Flow Rate.
 - Method 3: Gas Analysis for Carbon Dioxide, Excess Air, and Dry Molecular Weight.
 - Method 4: Moisture in Stack Gases.
 - Method 5: PM Emissions from Stationary Sources
 - Method 202: Condensable PM Emissions from Stationary Sources
- D. A copy of the test plan shall be provided to AQD at least 30 days prior to each test date.

- E. Performance testing shall be conducted while the units are operating within 10% of the rates at which operating permit authorization will be sought.
- F. At least 30 days prior to the testing, a notification of the test date and testing protocol shall be submitted to AQD. Deficiencies in the protocol shall be resolved prior to commencement of testing.

EUG 22: No. 2 Urea Plant Granulator

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
22-9164	No. 2 Urea Plant Granulator	6.04	26.45	--	--	--	--	2.39	8.44	--	--

- A. All discharges from each urea granulation operation shall be processed by a high-efficiency spray tower wet scrubber or equivalent device for PM emissions control. PM emissions shall not exceed 0.1 lb per ton urea product. [OAC 252:100-8-34(b)(1)]
- B. As part of the operating permit application, the permittee shall specify control device operating parameters which achieve the stated limitations. [OAC 252:100-43]
- C. The permittee is subject to following requirements under 40 CFR 60, Subpart VVa for the urea plant, as applicable:
 - i. 60.486a: Recordkeeping requirements
 - ii. 60.487a. Reporting requirements
- D. Within 180 days following commencement of operations of the new urea granulator, the permittee shall conduct performance testing as follows and furnish a written report to Air Quality. [OAC 252:100-43]
- E. The following USEPA methods shall be used for testing of emissions, unless otherwise approved by Air Quality:
 - Method 1: Sample and Velocity Traverses for Stationary Sources.
 - Method 2: Determination of Stack Gas Velocity and Volumetric Flow Rate.
 - Method 3: Gas Analysis for Carbon Dioxide, Excess Air, and Dry Molecular Weight.
 - Method 4: Moisture in Stack Gases.
 - Method 5: PM Emissions from Stationary Sources
 - Method 25A: VOC Emissions from Stationary Sources
 - Method 202: Condensable PM Emissions from Stationary Sources
- F. A copy of the test plan shall be provided to AQD at least 30 days prior to each test date.

- G. Performance testing shall be conducted while the units are operating within 10% of the rates at which operating permit authorization will be sought.
- H. At least 30 days prior to the testing, a notification of the test date and testing protocol shall be submitted to AQD. Deficiencies in the protocol shall be resolved prior to commencement of testing.

EUG 23: No. 2 Urea Plant Boiler

Point ID	Emission Unit	PM ₁₀ / PM _{2.5}		SO ₂		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
23-9165	No. 2 Urea Plant Boiler	3.35	14.69	0.26	1.16	20.25	88.70	2.43	10.63	16.65	72.93

- A. The above fuel burning equipment shall be fueled by pipeline quality natural gas.
- B. The boiler is subject to federal New Source Performance Standards, 40 CFR Part 60, Subpart Db, and shall comply with all applicable requirements, including, but not necessarily limited to those conditions shown following. (NOTE: Permit limitations are more stringent than Db limitations and will result in compliance with Subpart Db.)
[40 CFR 60.40b through 60.49b]
1. The boiler shall not discharge into the atmosphere any gases that contain nitrogen oxides (expressed as nitrogen dioxide) in excess of 0.20 lbs/MMBTU, 3-hour rolling average.
[40 CFR 60.44b(a)(1)(ii)]
 2. § 60.46b Performance test and compliance provisions;
 3. § 60.48b Emission Monitoring, and
 4. § 60.49b Reporting and recordkeeping requirements.
- C. Sulfur oxide emissions (measured as sulfur dioxide) from any new gas-fired fuel-burning equipment shall not exceed 0.2 lbs/MMBtu-heat input (86 ng/J), three hour average.
[OAC 252:100-31-25(a)(1)]
- D. Combustion CO_{2e} emissions shall not exceed 117 lb CO_{2e} / MMBTU heat input (30 day rolling average).
[OAC 252:100-8-34(b)]
- E. Within 180 days following commencement of operations of the boiler, performance testing shall be conducted and a written report of results submitted to AQD. The following USEPA methods shall be used for testing of emissions, unless otherwise approved by Air Quality:
[OAC 252:100-43]
- Method 1: Sample and Velocity Traverses for Stationary Sources.
- Method 2: Determination of Stack Gas Velocity and Volumetric Flow Rate.
- Method 3: Gas Analysis for Carbon Dioxide, Excess Air, and Dry Molecular Weight.
- Method 4: Moisture in Stack Gases.

Method 7E: NO_x Emissions from Stationary Sources
 Method 10: Carbon Monoxide Emissions from Stationary Sources
 Method 25A: VOC Emissions from Stationary Sources

- F. A copy of the test plan shall be provided to AQD at least 30 days prior to each test date.
- G. Performance testing shall be conducted while the boiler is operating within 10% of the rates at which operating permit authorization will be sought.
- H. At least 30 days prior to the testing, a notification of the test date and testing protocol shall be submitted to AQD. Deficiencies in the protocol shall be resolved prior to commencement of testing.

EUG 25: No. 2 Urea Plant Cooling Tower

Point ID	Emission Unit	PM ₁₀		PM _{2.5}		NO _x		VOC		CO	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
25-9167	No. 2 Urea Plant Cooling Tower	0.20	0.86	0.01	0.01	--	--	--	--	--	--

- A. Compliance Demonstrations: the following records shall be kept for the No. 2 Urea Plant Cooling Tower: [OAC 252:100-43]
 - i. Records of vendor certification of maximum circulation rate
 - ii. Records of design and construction showing 0.0005% or better drift.
 - iii. Records of TDS content of cooling water, tested within 180 days of start-up.

EUG 26 No. 2 Urea Plant Fugitive PM

EU ID	Point ID	EU Name
UR2MLD	26-9170	No. 2 Urea Materials Loading
UR2MSTG	26-9168	No. 2 Urea Materials Storage
UR2MTRFR	26-9169	No. 2 Urea Materials Transfer

- A. All conveyors between granulation, storage, and loading shall be equipped with wind shields. [OAC 252:100-8-6(a)]
- B. Loading of product into trucks and railcars shall be conducted inside enclosures on at least two sides using telescoping chutes into the receiving vessels. [OAC 252:100-8-6(a)]
- C. Storage of urea product shall be done in an enclosed building or other vessel shielded from winds. [OAC 252:100-8-6(a)]

EUG 27: New Haul Roads

EU ID	Point ID	EU Name
HAULRD	HAULRD	No. 2 Urea Plant Vehicle Traffic

- A. Haul roads in the No. 2 Urea Plant loading area shall be paved. [OAC 252:100-29]
 - B. The roads shall be watered and swept daily as necessary to control fugitive dust, except when the following conditions occur: [OAC 252:100-29]
 - i. Sweeping and watering need not occur on any day that the haul road is not in use.
 - ii. Sweeping and watering need not occur when a rain gauge located at the facility indicates that at least 0.2 inches of precipitation (water equivalent) has occurred within the preceding 24-hour time period.
 - iii. Sweeping and watering will not be required on calendar days where the daily high temperature is below 35 degrees F.
 - iv. If the facility has applied salt or sand for worker or driver safety the facility is not required to sweep or wash until the road has returned to driving conditions that no longer require the use of salt or sand.
 - C. The permittee shall maintain daily records of road watering and sweeping activities.
 - D. The permittee may use a wet street sweeper to meet the requirements of this condition.
2. The permittee is authorized to operate the facility continuously (24 hours per day, every day of the year). [OAC 252:100-8-6(a)]
 3. The facility is subject to 40 CFR Part 61, Subpart FF, and shall comply with the following standards: [40 CFR Part 61.340]
 - A. 61.342: Standards, General
 - B. 61.355: Test Methods, Procedures, and Compliance Provisions
 - C. 61.356: Recordkeeping Requirements
 - D. 61.357: Reporting Requirements
 4. Upon the compliance date of NESHAPS Subpart VVVVVV, the owner/operator shall comply with all applicable requirements of the NESHAP: Chemical Manufacturing Process Sources, Subpart VVVVVV, for each affected facility including but not limited to: [40 CFR 63.11494 through 63.11501]
 - A. § 63.11494 What are the applicability requirements and compliance dates?
 - B. § 63.11495 What are the management practices and other requirements?
 - C. § 63.11496 What are the standards and compliance requirements for process vents?
 - D. § 63.11497 What are the standards and compliance requirements for storage tanks?
 - E. § 63.11498 What are the standards and compliance requirements for wastewater systems?
 - F. § 63.11499 What are the standards and compliance requirements for heat exchange systems?
 - G. § 63.11500 What compliance options do I have if part of my plant is subject to both this standard and another Federal standard?

- H. § 63.11501 What are the notification, recordkeeping, and reporting requirements?
- I. § 63.11502 What definitions apply to this subpart?
- J. § 63.11503 Who implements and enforces this subpart?

5. The following records shall be maintained on location for inspection by ODEQ regulatory personnel. The required records shall be retained either in printed hard-copy or electronically for a period of at least five (5) years following the dates of recording. [OAC 252:100-43]

- A. Plant-wide 12-month rolling total methanol emissions calculations in EUG 1 (monthly).
- B. Records of conditioning agent usage from each granular urea plant EUG 6 and EUG 22 (monthly).
- C. Records of conditioning agent methanol content from vendor, with actual annual methanol content calculated on a 12-month rolling average basis for each granular urea plant for EUG 6 and EUG 22.
- D. Granular urea production rates for each granular urea plant for EUG 6 and EUG 22 (monthly).
- E. Granular urea truck and railcar loading rates for the two urea materials loading areas, EUG 14 and 26 (monthly).
- F. Monitoring of NO_x concentrations in exhausts from the EUG 11 Nitric Acid plant (continuous when operated).
- G. Nitric acid production rates, expressed as 100% nitric acid for EUG 11 (monthly).
- H. UAN production rates, expressed as 32% nitrogen for EUG 12 (monthly).
- I. Estimated quantities of ammonia, process off-gas sent to the EUG 13 flare (monthly).
- J. Venting episodes from EUG 15, including methods, assumptions, and duration of each event as used in calculating emission rates during venting episodes, and CO emission rates (12-month rolling total).
- K. Visible observations records where required for EUG 6 and EUG 12 (monthly).
- L. Reference Method 9 results as set forth in Item A for EUG 6 and EUG 12 (as needed, if applicable).
- M. Duration (hours) of venting as needed to calculate CO emissions from EUG 10 (monthly), and CO emission rates (monthly and 12-month rolling totals).
- N. Hours of operation of the ammonia unit startup boiler in EUG 3 (monthly and 12-month rolling totals).
- O. Records as required by 40 CFR Part 61, Subpart FF for Specific Condition 3.
- P. Records as required by 40 CFR Part 60, Subpart VVa for No. 1 and No. 2 Urea Plants (per EUG 6 and EUG 22).
- Q. Pressure differentials of each urea granulator wet scrubber (daily when operated), No 1 Urea granulators (EUG 6).
- R. For the fuel(s) burned, the appropriate document(s) as described in Specific Condition No. 1, EUGs 1, 2, 3, 4, 13, and 23.
- S. Records of fuels used in EUG-1, EUG-2, and EUG-11.
- T. Records as required by NSPS Subpart JJJJ and NESHAP Subpart ZZZZ for the emergency generators in EUG-18 and 19.
- U. Records of average hourly heat input for each reformer, monthly, as required by EUG-2.
- V. Records as required by 40 CFR Part 63, Subpart CCCCCC for EUG 20.

- W. Numbers and durations of each start-up and shutdown event for EUG-11, the Nitric Acid Plant.
 - X. Records as required by 40 CFR Part 63, Subpart VVVVVV for Specific Condition 4.
 - Y. Records as required by NSPS Subpart Db for EUG 23, the No. 2 Urea Boiler.
 - Z. Records of TDS testing in the No. 2 Urea Cooling Tower (EUG 25) and No. 2 Ammonia Cooling Tower (EUG 9).
 - AA. Ammonia production records for EUG 1 (monthly).
 - BB. Process CO₂ calculations using 40 CFR 98, Subpart G for EUG 1 (monthly).
 - CC. CO₂ sales and usage records for EUG 1 (monthly).
 - DD. Records of WESP operating parameters developed for No. 2 Urea Granulator WESP and pressure differentials of the urea granulator wet scrubber for EUG 22 (daily when operated).
 - EE. Records of road watering and sweeping activities for EUG 27 (daily).
 - FF. Monitoring of CO and NO_x concentrations from each Primary Reformer (continuously when operated).
6. The following records shall be maintained on-site to verify Insignificant Activities. No recordkeeping is required for those operations that qualify as Trivial Activities.
[OAC 252:100-8-6 (a)(3)(B)]
- A. Hours of operation and the production rates of the portable fertilizer mixing unit and engine.
 - B. Fuel dispensing to facility owned vehicles: annual throughput of diesel.
 - C. Lime silos: inspection and maintenance of the dust collector.
 - D. Diesel storage tanks: records of tank capacities and tank contents.
 - E. UAN storage tanks: records of tank capacities and tank contents.
 - F. For other activities that have the potential emissions less than 5 TPY (actual): type of activity and the amount of emissions from the activity.
7. No later than 30 days after each anniversary of the original Title V operating permit (December 18, 2006), the permittee shall submit to Air Quality Division of DEQ, with a copy to the US EPA, Region 6, a certification of compliance with the terms and conditions of the Title V operating permit.
[OAC 252:100-8-6 (c)(5)(A) & (D)]
8. Deviations from the 40 CFR Part 68 regulations that arise from review of process safety management procedures and programs, including deviations identified in the process safety management audits, will not be considered deviations of this permit.
9. The permittee shall apply for a modified operating permit within 180 days of commencement of operations of any new or physically modified unit.
[OAC 252:100-8-6]
10. The Permit Shield (Standard Conditions, Section VI) is extended to the following requirements that have been determined to be inapplicable to this facility or the listed emission unit groups.
[OAC 252:100-8-6(d)(2)]

A. Facility Wide

Citation	Description	Reason for Non-Applicability
OAC 252:100-7	Minor Sources	not in source category
OAC 252:100-11	Alternative Reduction Plans and Authorizations	not in source category
OAC 252:100-15	Mobile Sources	not in source category
OAC 252:100-17	Incinerators	not type of emission unit
OAC 252:100-23	Cotton Gins	not type of emission unit
OAC 252:100-24	Grain Elevators	not in source category
OAC 252:100-31, Part 2	Sulfur Compounds, Ambient Concentrations	not in source category
OAC 252:100-35	Carbon Monoxide	not in source category
OAC 252:100-39	Nonattainment Areas	not in area category
OAC 252:100-47	Landfills	not in source category
40 CFR 60 Subpart D	Steam Generators	below the specified size
40 CFR 60 Subpart Dc	Steam Generating Units	prior to the effective date
40 CFR 60 Subpart G	Nitric Acid Plants	prior to the effective date
40 CFR 60 Subpart Ga	Nitric Acid Plants	prior to the effective date
40 CFR 60 Subpart Kb	Volatile Organic Liquid Storage	vapor pressure of stored material below applicability threshold
40 CFR 61, all subparts except M and FF	NESHAP	not in source category, not a major source of HAPs
40 CFR 63, all subparts related to Title III major sources	NESHAP	not a major source of HAPs
40 CFR 63, Subpart JJJJJ	Area Source Boiler GACT	not applicable
40 CFR 64	Compliance Assurance Monitoring	not applicable

B. By Emission Unit Grouping

EUG	Citation	Description	Reason for Non-Applicability
EUG 2	40 CFR 60, Subpart D	Steam Generating Units > 250 MMBTUH	below the specified size
EUG 2,3	40 CFR 60, Subpart Db	Steam Generating Units 100-250 MMBTUH	prior to the effective date
EUG 3	40 CFR 60, Subpart Dc	Steam Generating Units 10-100 MMBTUH	prior to the effective date
EUG 11	40 CFR 60, Subpart G and Ga	Nitric Acid Plants	prior to the effective date
EUG 13	40 CFR 60, Subpart A, 60.18	Flare	Not in source category
EUG 5, 17	40 CFR 60, Subpart Kb	Storage Vessels	vapor pressure of stored material below applicability threshold
EUG 2	OAC 252:100-31-25 (c)	Sulfur Compounds, Fuel and Emissions Monitoring	not in source category
EUG 4 and 23	OAC 252:100-33	Control of Emission of Nitrogen Oxides	below the specified size
EUG 5 and 17	OAC 252:100-37	Control of Emission of VOC	below the specified vapor pressure

EUG 6, 7, 9, 12, 13, 14, 14A, 16, 17, 21, 22, 25, 26, 27	OAC 252:100-19-4	PM Emissions from Fuel Burning Units	not in source category
EUG 5-17, 20-22, 24-25	OAC 252:100-31	Control of Emission of Sulfur Compounds	not in source category
EUG 5-17, 20-22, 24-27	OAC 252:100-33	Control of Emissions of Nitrogen Oxide	not in source category
EUG 6-17, 20-22, 25-27	OAC 252:100-37	Control of Emission of VOC	not in source category
EUG 4, 7, 11, 12, 13, 15, 17 - 20	OAC 252:100-8, Part 7	Prevention of Significant Deterioration	No changes have been made to trigger this requirements for these sources

11. Permit No. 2016-1295-C (M-5)(PSD) replaces and supersedes Permit No. 2011-441-C (M-9) (PSD).



PART 70 PERMIT

AIR QUALITY DIVISION
STATE OF OKLAHOMA
DEPARTMENT OF ENVIRONMENTAL QUALITY
707 N. ROBINSON, SUITE 4100
P.O. BOX 1677
OKLAHOMA CITY, OKLAHOMA 73101-1677

Permit No. 2016-1295-C (M-5)(PSD)

Koch Fertilizer Enid LLC,

having complied with the requirements of the law, is hereby granted permission to construct modifications to the Enid Nitrogen Plant located at 1619 South 78th, Enid, Garfield County, Oklahoma, subject to standard conditions dated June 21, 2016, and specific conditions, both attached.

In the absence of commencement of construction, this permit shall expire 18 months from the date below, except as authorized under Section VIII of the Standard Conditions.

Permits & Engineering Group Manager
Air Quality Division

Date

Koch Fertilizer Enid LLC
Attn: Ms. Lacy Mills
1619 S. 78th Street
Enid, OK 73701

Re: Permit Application No. 2016-1295-C (M-5)(PSD)
Enid Nitrogen Plant
Enid, Garfield County, Oklahoma

Dear Ms. Mills:

Enclosed is the permit authorizing construction of the referenced facility. Please note that this permit is issued subject to standard and specific conditions, which are attached. These conditions must be carefully followed since they define the limits of the permit and will be confirmed by periodic inspections.

Also note that you are required to annually submit an emissions inventory for this facility. An emissions inventory must be completed on approved AQD forms and submitted (hardcopy or electronically) by April 1st of every year. Any questions concerning the form or submittal process should be referred to the Emissions Inventory Staff at (405) 702-4100.

Thank you for your cooperation in this matter. If we may be of further service, please contact our office at (405)702-4100.

Sincerely,

David S. Schutz, P.E.
AIR QUALITY DIVISION

Enclosure

**MAJOR SOURCE AIR QUALITY PERMIT
STANDARD CONDITIONS
(June 21, 2016)**

SECTION I. DUTY TO COMPLY

A. This is a permit to operate / construct this specific facility in accordance with the federal Clean Air Act (42 U.S.C. 7401, et al.) and under the authority of the Oklahoma Clean Air Act and the rules promulgated there under. [Oklahoma Clean Air Act, 27A O.S. § 2-5-112]

B. The issuing Authority for the permit is the Air Quality Division (AQD) of the Oklahoma Department of Environmental Quality (DEQ). The permit does not relieve the holder of the obligation to comply with other applicable federal, state, or local statutes, regulations, rules, or ordinances. [Oklahoma Clean Air Act, 27A O.S. § 2-5-112]

C. The permittee shall comply with all conditions of this permit. Any permit noncompliance shall constitute a violation of the Oklahoma Clean Air Act and shall be grounds for enforcement action, permit termination, revocation and reissuance, or modification, or for denial of a permit renewal application. All terms and conditions are enforceable by the DEQ, by the Environmental Protection Agency (EPA), and by citizens under section 304 of the Federal Clean Air Act (excluding state-only requirements). This permit is valid for operations only at the specific location listed.

[40 C.F.R. §70.6(b), OAC 252:100-8-1.3 and OAC 252:100-8-6(a)(7)(A) and (b)(1)]

D. It shall not be a defense for a permittee in an enforcement action that it would have been necessary to halt or reduce the permitted activity in order to maintain compliance with the conditions of the permit. However, nothing in this paragraph shall be construed as precluding consideration of a need to halt or reduce activity as a mitigating factor in assessing penalties for noncompliance if the health, safety, or environmental impacts of halting or reducing operations would be more serious than the impacts of continuing operations. [OAC 252:100-8-6(a)(7)(B)]

SECTION II. REPORTING OF DEVIATIONS FROM PERMIT TERMS

A. Any exceedance resulting from an emergency and/or posing an imminent and substantial danger to public health, safety, or the environment shall be reported in accordance with Section XIV (Emergencies). [OAC 252:100-8-6(a)(3)(C)(iii)(I) & (II)]

B. Deviations that result in emissions exceeding those allowed in this permit shall be reported consistent with the requirements of OAC 252:100-9, Excess Emission Reporting Requirements. [OAC 252:100-8-6(a)(3)(C)(iv)]

C. Every written report submitted under this section shall be certified as required by Section III (Monitoring, Testing, Recordkeeping & Reporting), Paragraph F. [OAC 252:100-8-6(a)(3)(C)(iv)]

SECTION III. MONITORING, TESTING, RECORDKEEPING & REPORTING

A. The permittee shall keep records as specified in this permit. These records, including monitoring data and necessary support information, shall be retained on-site or at a nearby field office for a period of at least five years from the date of the monitoring sample, measurement, report, or application, and shall be made available for inspection by regulatory personnel upon request. Support information includes all original strip-chart recordings for continuous monitoring instrumentation, and copies of all reports required by this permit. Where appropriate, the permit may specify that records may be maintained in computerized form.

[OAC 252:100-8-6 (a)(3)(B)(ii), OAC 252:100-8-6(c)(1), and OAC 252:100-8-6(c)(2)(B)]

B. Records of required monitoring shall include:

- (1) the date, place and time of sampling or measurement;
- (2) the date or dates analyses were performed;
- (3) the company or entity which performed the analyses;
- (4) the analytical techniques or methods used;
- (5) the results of such analyses; and
- (6) the operating conditions existing at the time of sampling or measurement.

[OAC 252:100-8-6(a)(3)(B)(i)]

C. No later than 30 days after each six (6) month period, after the date of the issuance of the original Part 70 operating permit or alternative date as specifically identified in a subsequent Part 70 operating permit, the permittee shall submit to AQD a report of the results of any required monitoring. All instances of deviations from permit requirements since the previous report shall be clearly identified in the report. Submission of these periodic reports will satisfy any reporting requirement of Paragraph E below that is duplicative of the periodic reports, if so noted on the submitted report.

[OAC 252:100-8-6(a)(3)(C)(i) and (ii)]

D. If any testing shows emissions in excess of limitations specified in this permit, the owner or operator shall comply with the provisions of Section II (Reporting Of Deviations From Permit Terms) of these standard conditions.

[OAC 252:100-8-6(a)(3)(C)(iii)]

E. In addition to any monitoring, recordkeeping or reporting requirement specified in this permit, monitoring and reporting may be required under the provisions of OAC 252:100-43, Testing, Monitoring, and Recordkeeping, or as required by any provision of the Federal Clean Air Act or Oklahoma Clean Air Act.

[OAC 252:100-43]

F. Any Annual Certification of Compliance, Semi Annual Monitoring and Deviation Report, Excess Emission Report, and Annual Emission Inventory submitted in accordance with this permit shall be certified by a responsible official. This certification shall be signed by a responsible official, and shall contain the following language: "I certify, based on information and belief formed after reasonable inquiry, the statements and information in the document are true, accurate, and complete."

[OAC 252:100-8-5(f), OAC 252:100-8-6(a)(3)(C)(iv), OAC 252:100-8-6(c)(1), OAC 252:100-9-7(e), and OAC 252:100-5-2.1(f)]

G. Any owner or operator subject to the provisions of New Source Performance Standards ("NSPS") under 40 CFR Part 60 or National Emission Standards for Hazardous Air Pollutants ("NESHAPs") under 40 CFR Parts 61 and 63 shall maintain a file of all measurements and other

information required by the applicable general provisions and subpart(s). These records shall be maintained in a permanent file suitable for inspection, shall be retained for a period of at least five years as required by Paragraph A of this Section, and shall include records of the occurrence and duration of any start-up, shutdown, or malfunction in the operation of an affected facility, any malfunction of the air pollution control equipment; and any periods during which a continuous monitoring system or monitoring device is inoperative.

[40 C.F.R. §§60.7 and 63.10, 40 CFR Parts 61, Subpart A, and OAC 252:100, Appendix Q]

H. The permittee of a facility that is operating subject to a schedule of compliance shall submit to the DEQ a progress report at least semi-annually. The progress reports shall contain dates for achieving the activities, milestones or compliance required in the schedule of compliance and the dates when such activities, milestones or compliance was achieved. The progress reports shall also contain an explanation of why any dates in the schedule of compliance were not or will not be met, and any preventive or corrective measures adopted. [OAC 252:100-8-6(c)(4)]

I. All testing must be conducted under the direction of qualified personnel by methods approved by the Division Director. All tests shall be made and the results calculated in accordance with standard test procedures. The use of alternative test procedures must be approved by EPA. When a portable analyzer is used to measure emissions it shall be setup, calibrated, and operated in accordance with the manufacturer's instructions and in accordance with a protocol meeting the requirements of the "AQD Portable Analyzer Guidance" document or an equivalent method approved by Air Quality.

[OAC 252:100-8-6(a)(3)(A)(iv), and OAC 252:100-43]

J. The reporting of total particulate matter emissions as required in Part 7 of OAC 252:100-8 (Permits for Part 70 Sources), OAC 252:100-19 (Control of Emission of Particulate Matter), and OAC 252:100-5 (Emission Inventory), shall be conducted in accordance with applicable testing or calculation procedures, modified to include back-half condensables, for the concentration of particulate matter less than 10 microns in diameter (PM₁₀). NSPS may allow reporting of only particulate matter emissions caught in the filter (obtained using Reference Method 5).

K. The permittee shall submit to the AQD a copy of all reports submitted to the EPA as required by 40 C.F.R. Part 60, 61, and 63, for all equipment constructed or operated under this permit subject to such standards. [OAC 252:100-8-6(c)(1) and OAC 252:100, Appendix Q]

SECTION IV. COMPLIANCE CERTIFICATIONS

A. No later than 30 days after each anniversary date of the issuance of the original Part 70 operating permit or alternative date as specifically identified in a subsequent Part 70 operating permit, the permittee shall submit to the AQD, with a copy to the US EPA, Region 6, a certification of compliance with the terms and conditions of this permit and of any other applicable requirements which have become effective since the issuance of this permit.

[OAC 252:100-8-6(c)(5)(A), and (D)]

B. The compliance certification shall describe the operating permit term or condition that is the basis of the certification; the current compliance status; whether compliance was continuous or intermittent; the methods used for determining compliance, currently and over the reporting period. The compliance certification shall also include such other facts as the permitting authority may require to determine the compliance status of the source.

[OAC 252:100-8-6(c)(5)(C)(i)-(v)]

C. The compliance certification shall contain a certification by a responsible official as to the results of the required monitoring. This certification shall be signed by a responsible official, and shall contain the following language: "I certify, based on information and belief formed after reasonable inquiry, the statements and information in the document are true, accurate, and complete."

[OAC 252:100-8-5(f) and OAC 252:100-8-6(c)(1)]

D. Any facility reporting noncompliance shall submit a schedule of compliance for emissions units or stationary sources that are not in compliance with all applicable requirements. This schedule shall include a schedule of remedial measures, including an enforceable sequence of actions with milestones, leading to compliance with any applicable requirements for which the emissions unit or stationary source is in noncompliance. This compliance schedule shall resemble and be at least as stringent as that contained in any judicial consent decree or administrative order to which the emissions unit or stationary source is subject. Any such schedule of compliance shall be supplemental to, and shall not sanction noncompliance with, the applicable requirements on which it is based, except that a compliance plan shall not be required for any noncompliance condition which is corrected within 24 hours of discovery.

[OAC 252:100-8-5(e)(8)(B) and OAC 252:100-8-6(c)(3)]

SECTION V. REQUIREMENTS THAT BECOME APPLICABLE DURING THE PERMIT TERM

The permittee shall comply with any additional requirements that become effective during the permit term and that are applicable to the facility. Compliance with all new requirements shall be certified in the next annual certification.

[OAC 252:100-8-6(c)(6)]

SECTION VI. PERMIT SHIELD

A. Compliance with the terms and conditions of this permit (including terms and conditions established for alternate operating scenarios, emissions trading, and emissions averaging, but excluding terms and conditions for which the permit shield is expressly prohibited under OAC 252:100-8) shall be deemed compliance with the applicable requirements identified and included in this permit.

[OAC 252:100-8-6(d)(1)]

B. Those requirements that are applicable are listed in the Standard Conditions and the Specific Conditions of this permit. Those requirements that the applicant requested be determined as not applicable are summarized in the Specific Conditions of this permit.

[OAC 252:100-8-6(d)(2)]

SECTION VII. ANNUAL EMISSIONS INVENTORY & FEE PAYMENT

The permittee shall file with the AQD an annual emission inventory and shall pay annual fees based on emissions inventories. The methods used to calculate emissions for inventory purposes shall be based on the best available information accepted by AQD.

[OAC 252:100-5-2.1, OAC 252:100-5-2.2, and OAC 252:100-8-6(a)(8)]

SECTION VIII. TERM OF PERMIT

A. Unless specified otherwise, the term of an operating permit shall be five years from the date of issuance. [OAC 252:100-8-6(a)(2)(A)]

B. A source's right to operate shall terminate upon the expiration of its permit unless a timely and complete renewal application has been submitted at least 180 days before the date of expiration. [OAC 252:100-8-7.1(d)(1)]

C. A duly issued construction permit or authorization to construct or modify will terminate and become null and void (unless extended as provided in OAC 252:100-8-1.4(b)) if the construction is not commenced within 18 months after the date the permit or authorization was issued, or if work is suspended for more than 18 months after it is commenced. [OAC 252:100-8-1.4(a)]

D. The recipient of a construction permit shall apply for a permit to operate (or modified operating permit) within 180 days following the first day of operation. [OAC 252:100-8-4(b)(5)]

SECTION IX. SEVERABILITY

The provisions of this permit are severable and if any provision of this permit, or the application of any provision of this permit to any circumstance, is held invalid, the application of such provision to other circumstances, and the remainder of this permit, shall not be affected thereby.

[OAC 252:100-8-6 (a)(6)]

SECTION X. PROPERTY RIGHTS

A. This permit does not convey any property rights of any sort, or any exclusive privilege.

[OAC 252:100-8-6(a)(7)(D)]

B. This permit shall not be considered in any manner affecting the title of the premises upon which the equipment is located and does not release the permittee from any liability for damage to persons or property caused by or resulting from the maintenance or operation of the equipment for which the permit is issued. [OAC 252:100-8-6(c)(6)]

SECTION XI. DUTY TO PROVIDE INFORMATION

A. The permittee shall furnish to the DEQ, upon receipt of a written request and within sixty (60) days of the request unless the DEQ specifies another time period, any information that the DEQ may request to determine whether cause exists for modifying, reopening, revoking, reissuing, terminating the permit or to determine compliance with the permit. Upon request, the permittee shall also furnish to the DEQ copies of records required to be kept by the permit.

[OAC 252:100-8-6(a)(7)(E)]

B. The permittee may make a claim of confidentiality for any information or records submitted pursuant to 27A O.S. § 2-5-105(18). Confidential information shall be clearly labeled as such and shall be separable from the main body of the document such as in an attachment.

[OAC 252:100-8-6(a)(7)(E)]

C. Notification to the AQD of the sale or transfer of ownership of this facility is required and shall be made in writing within thirty (30) days after such sale or transfer.

[Oklahoma Clean Air Act, 27A O.S. § 2-5-112(G)]

SECTION XII. REOPENING, MODIFICATION & REVOCATION

A. The permit may be modified, revoked, reopened and reissued, or terminated for cause. Except as provided for minor permit modifications, the filing of a request by the permittee for a permit modification, revocation and reissuance, termination, notification of planned changes, or anticipated noncompliance does not stay any permit condition.

[OAC 252:100-8-6(a)(7)(C) and OAC 252:100-8-7.2(b)]

B. The DEQ will reopen and revise or revoke this permit prior to the expiration date in the following circumstances:

[OAC 252:100-8-7.3 and OAC 252:100-8-7.4(a)(2)]

- (1) Additional requirements under the Clean Air Act become applicable to a major source category three or more years prior to the expiration date of this permit. No such reopening is required if the effective date of the requirement is later than the expiration date of this permit.
- (2) The DEQ or the EPA determines that this permit contains a material mistake or that the permit must be revised or revoked to assure compliance with the applicable requirements.
- (3) The DEQ or the EPA determines that inaccurate information was used in establishing the emission standards, limitations, or other conditions of this permit. The DEQ may revoke and not reissue this permit if it determines that the permittee has submitted false or misleading information to the DEQ.
- (4) DEQ determines that the permit should be amended under the discretionary reopening provisions of OAC 252:100-8-7.3(b).

C. The permit may be reopened for cause by EPA, pursuant to the provisions of OAC 100-8-7.3(d).

[OAC 100-8-7.3(d)]

D. The permittee shall notify AQD before making changes other than those described in Section XVIII (Operational Flexibility), those qualifying for administrative permit amendments, or those defined as an Insignificant Activity (Section XVI) or Trivial Activity (Section XVII). The

notification should include any changes which may alter the status of a "grandfathered source," as defined under AQD rules. Such changes may require a permit modification.

[OAC 252:100-8-7.2(b) and OAC 252:100-5-1.1]

E. Activities that will result in air emissions that exceed the trivial/insignificant levels and that are not specifically approved by this permit are prohibited. [OAC 252:100-8-6(c)(6)]

SECTION XIII. INSPECTION & ENTRY

A. Upon presentation of credentials and other documents as may be required by law, the permittee shall allow authorized regulatory officials to perform the following (subject to the permittee's right to seek confidential treatment pursuant to 27A O.S. Supp. 1998, § 2-5-105(17) for confidential information submitted to or obtained by the DEQ under this section):

- (1) enter upon the permittee's premises during reasonable/normal working hours where a source is located or emissions-related activity is conducted, or where records must be kept under the conditions of the permit;
- (2) have access to and copy, at reasonable times, any records that must be kept under the conditions of the permit;
- (3) inspect, at reasonable times and using reasonable safety practices, any facilities, equipment (including monitoring and air pollution control equipment), practices, or operations regulated or required under the permit; and
- (4) as authorized by the Oklahoma Clean Air Act, sample or monitor at reasonable times substances or parameters for the purpose of assuring compliance with the permit.

[OAC 252:100-8-6(c)(2)]

SECTION XIV. EMERGENCIES

A. Any exceedance resulting from an emergency shall be reported to AQD promptly but no later than 4:30 p.m. on the next working day after the permittee first becomes aware of the exceedance. This notice shall contain a description of the emergency, the probable cause of the exceedance, any steps taken to mitigate emissions, and corrective actions taken.

[OAC 252:100-8-6 (a)(3)(C)(iii)(I) and (IV)]

B. Any exceedance that poses an imminent and substantial danger to public health, safety, or the environment shall be reported to AQD as soon as is practicable; but under no circumstance shall notification be more than 24 hours after the exceedance. [OAC 252:100-8-6(a)(3)(C)(iii)(II)]

C. An "emergency" means any situation arising from sudden and reasonably unforeseeable events beyond the control of the source, including acts of God, which situation requires immediate corrective action to restore normal operation, and that causes the source to exceed a technology-based emission limitation under this permit, due to unavoidable increases in emissions attributable to the emergency. An emergency shall not include noncompliance to the extent caused by improperly designed equipment, lack of preventive maintenance, careless or improper operation, or operator error. [OAC 252:100-8-2]

D. The affirmative defense of emergency shall be demonstrated through properly signed, contemporaneous operating logs or other relevant evidence that: [OAC 252:100-8-6 (e)(2)]

- (1) an emergency occurred and the permittee can identify the cause or causes of the emergency;
- (2) the permitted facility was at the time being properly operated;
- (3) during the period of the emergency the permittee took all reasonable steps to minimize levels of emissions that exceeded the emission standards or other requirements in this permit.

E. In any enforcement proceeding, the permittee seeking to establish the occurrence of an emergency shall have the burden of proof. [OAC 252:100-8-6(e)(3)]

F. Every written report or document submitted under this section shall be certified as required by Section III (Monitoring, Testing, Recordkeeping & Reporting), Paragraph F. [OAC 252:100-8-6(a)(3)(C)(iv)]

SECTION XV. RISK MANAGEMENT PLAN

The permittee, if subject to the provision of Section 112(r) of the Clean Air Act, shall develop and register with the appropriate agency a risk management plan by June 20, 1999, or the applicable effective date. [OAC 252:100-8-6(a)(4)]

SECTION XVI. INSIGNIFICANT ACTIVITIES

Except as otherwise prohibited or limited by this permit, the permittee is hereby authorized to operate individual emissions units that are either on the list in Appendix I to OAC Title 252, Chapter 100, or whose actual calendar year emissions do not exceed any of the limits below. Any activity to which a State or Federal applicable requirement applies is not insignificant even if it meets the criteria below or is included on the insignificant activities list.

- (1) 5 tons per year of any one criteria pollutant.
- (2) 2 tons per year for any one hazardous air pollutant (HAP) or 5 tons per year for an aggregate of two or more HAP's, or 20 percent of any threshold less than 10 tons per year for single HAP that the EPA may establish by rule.

[OAC 252:100-8-2 and OAC 252:100, Appendix I]

SECTION XVII. TRIVIAL ACTIVITIES

Except as otherwise prohibited or limited by this permit, the permittee is hereby authorized to operate any individual or combination of air emissions units that are considered inconsequential and are on the list in Appendix J. Any activity to which a State or Federal applicable requirement applies is not trivial even if included on the trivial activities list.

[OAC 252:100-8-2 and OAC 252:100, Appendix J]

SECTION XVIII. OPERATIONAL FLEXIBILITY

A. A facility may implement any operating scenario allowed for in its Part 70 permit without the need for any permit revision or any notification to the DEQ (unless specified otherwise in the permit). When an operating scenario is changed, the permittee shall record in a log at the facility the scenario under which it is operating. [OAC 252:100-8-6(a)(10) and (f)(1)]

B. The permittee may make changes within the facility that:

- (1) result in no net emissions increases,
- (2) are not modifications under any provision of Title I of the federal Clean Air Act, and
- (3) do not cause any hourly or annual permitted emission rate of any existing emissions unit to be exceeded;

provided that the facility provides the EPA and the DEQ with written notification as required below in advance of the proposed changes, which shall be a minimum of seven (7) days, or twenty four (24) hours for emergencies as defined in OAC 252:100-8-6 (e). The permittee, the DEQ, and the EPA shall attach each such notice to their copy of the permit. For each such change, the written notification required above shall include a brief description of the change within the permitted facility, the date on which the change will occur, any change in emissions, and any permit term or condition that is no longer applicable as a result of the change. The permit shield provided by this permit does not apply to any change made pursuant to this paragraph. [OAC 252:100-8-6(f)(2)]

SECTION XIX. OTHER APPLICABLE & STATE-ONLY REQUIREMENTS

A. The following applicable requirements and state-only requirements apply to the facility unless elsewhere covered by a more restrictive requirement:

- (1) Open burning of refuse and other combustible material is prohibited except as authorized in the specific examples and under the conditions listed in the Open Burning Subchapter.
[OAC 252:100-13]
- (2) No particulate emissions from any fuel-burning equipment with a rated heat input of 10 MMBTUH or less shall exceed 0.6 lb/MMBTU.
[OAC 252:100-19]
- (3) For all emissions units not subject to an opacity limit promulgated under 40 C.F.R., Part 60, NSPS, no discharge of greater than 20% opacity is allowed except for:
[OAC 252:100-25]
 - (a) Short-term occurrences which consist of not more than one six-minute period in any consecutive 60 minutes, not to exceed three such periods in any consecutive 24 hours. In no case shall the average of any six-minute period exceed 60% opacity;
 - (b) Smoke resulting from fires covered by the exceptions outlined in OAC 252:100-13-7;
 - (c) An emission, where the presence of uncombined water is the only reason for failure to meet the requirements of OAC 252:100-25-3(a); or
 - (d) Smoke generated due to a malfunction in a facility, when the source of the fuel producing the smoke is not under the direct and immediate control of the facility and the immediate constriction of the fuel flow at the facility would produce a hazard to life and/or property.
- (4) No visible fugitive dust emissions shall be discharged beyond the property line on which the emissions originate in such a manner as to damage or to interfere with the use of adjacent properties, or cause air quality standards to be exceeded, or interfere with the maintenance of air quality standards.
[OAC 252:100-29]

- (5) No sulfur oxide emissions from new gas-fired fuel-burning equipment shall exceed 0.2 lb/MMBTU. No existing source shall exceed the listed ambient air standards for sulfur dioxide. [OAC 252:100-31]
- (6) Volatile Organic Compound (VOC) storage tanks built after December 28, 1974, and with a capacity of 400 gallons or more storing a liquid with a vapor pressure of 1.5 psia or greater under actual conditions shall be equipped with a permanent submerged fill pipe or with a vapor-recovery system. [OAC 252:100-37-15(b)]
- (7) All fuel-burning equipment shall at all times be properly operated and maintained in a manner that will minimize emissions of VOCs. [OAC 252:100-37-36]

SECTION XX. STRATOSPHERIC OZONE PROTECTION

A. The permittee shall comply with the following standards for production and consumption of ozone-depleting substances: [40 CFR 82, Subpart A]

- (1) Persons producing, importing, or placing an order for production or importation of certain class I and class II substances, HCFC-22, or HCFC-141b shall be subject to the requirements of §82.4;
- (2) Producers, importers, exporters, purchasers, and persons who transform or destroy certain class I and class II substances, HCFC-22, or HCFC-141b are subject to the recordkeeping requirements at §82.13; and
- (3) Class I substances (listed at Appendix A to Subpart A) include certain CFCs, Halons, HBFCs, carbon tetrachloride, trichloroethane (methyl chloroform), and bromomethane (Methyl Bromide). Class II substances (listed at Appendix B to Subpart A) include HCFCs.

B. If the permittee performs a service on motor (fleet) vehicles when this service involves an ozone-depleting substance refrigerant (or regulated substitute substance) in the motor vehicle air conditioner (MVAC), the permittee is subject to all applicable requirements. Note: The term “motor vehicle” as used in Subpart B does not include a vehicle in which final assembly of the vehicle has not been completed. The term “MVAC” as used in Subpart B does not include the air-tight sealed refrigeration system used as refrigerated cargo, or the system used on passenger buses using HCFC-22 refrigerant. [40 CFR 82, Subpart B]

C. The permittee shall comply with the following standards for recycling and emissions reduction except as provided for MVACs in Subpart B: [40 CFR 82, Subpart F]

- (1) Persons opening appliances for maintenance, service, repair, or disposal must comply with the required practices pursuant to § 82.156;
- (2) Equipment used during the maintenance, service, repair, or disposal of appliances must comply with the standards for recycling and recovery equipment pursuant to § 82.158;
- (3) Persons performing maintenance, service, repair, or disposal of appliances must be certified by an approved technician certification program pursuant to § 82.161;
- (4) Persons disposing of small appliances, MVACs, and MVAC-like appliances must comply with record-keeping requirements pursuant to § 82.166;
- (5) Persons owning commercial or industrial process refrigeration equipment must comply with leak repair requirements pursuant to § 82.158; and

- (6) Owners/operators of appliances normally containing 50 or more pounds of refrigerant must keep records of refrigerant purchased and added to such appliances pursuant to § 82.166.

SECTION XXI. TITLE V APPROVAL LANGUAGE

A. DEQ wishes to reduce the time and work associated with permit review and, wherever it is not inconsistent with Federal requirements, to provide for incorporation of requirements established through construction permitting into the Source's Title V permit without causing redundant review. Requirements from construction permits may be incorporated into the Title V permit through the administrative amendment process set forth in OAC 252:100-8-7.2(a) only if the following procedures are followed:

- (1) The construction permit goes out for a 30-day public notice and comment using the procedures set forth in 40 C.F.R. § 70.7(h)(1). This public notice shall include notice to the public that this permit is subject to EPA review, EPA objection, and petition to EPA, as provided by 40 C.F.R. § 70.8; that the requirements of the construction permit will be incorporated into the Title V permit through the administrative amendment process; that the public will not receive another opportunity to provide comments when the requirements are incorporated into the Title V permit; and that EPA review, EPA objection, and petitions to EPA will not be available to the public when requirements from the construction permit are incorporated into the Title V permit.
- (2) A copy of the construction permit application is sent to EPA, as provided by 40 CFR § 70.8(a)(1).
- (3) A copy of the draft construction permit is sent to any affected State, as provided by 40 C.F.R. § 70.8(b).
- (4) A copy of the proposed construction permit is sent to EPA for a 45-day review period as provided by 40 C.F.R. § 70.8(a) and (c).
- (5) The DEQ complies with 40 C.F.R. § 70.8(c) upon the written receipt within the 45-day comment period of any EPA objection to the construction permit. The DEQ shall not issue the permit until EPA's objections are resolved to the satisfaction of EPA.
- (6) The DEQ complies with 40 C.F.R. § 70.8(d).
- (7) A copy of the final construction permit is sent to EPA as provided by 40 CFR § 70.8(a).
- (8) The DEQ shall not issue the proposed construction permit until any affected State and EPA have had an opportunity to review the proposed permit, as provided by these permit conditions.
- (9) Any requirements of the construction permit may be reopened for cause after incorporation into the Title V permit by the administrative amendment process, by DEQ as provided in OAC 252:100-8-7.3(a), (b), and (c), and by EPA as provided in 40 C.F.R. § 70.7(f) and (g).
- (10) The DEQ shall not issue the administrative permit amendment if performance tests fail to demonstrate that the source is operating in substantial compliance with all permit requirements.

B. To the extent that these conditions are not followed, the Title V permit must go through the Title V review process.

SECTION XXII. CREDIBLE EVIDENCE

For the purpose of submitting compliance certifications or establishing whether or not a person has violated or is in violation of any provision of the Oklahoma implementation plan, nothing shall preclude the use, including the exclusive use, of any credible evidence or information, relevant to whether a source would have been in compliance with applicable requirements if the appropriate performance or compliance test or procedure had been performed.

[OAC 252:100-43-6]